



1. Formation Pore Pressure

Contents:

- Introduction
- Methods of Estimating Pore Pressure
- Fracture Gradient

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References:

- Applied Drilling Engineering- Adam T. Bourgoyne Jr. et al Chapter 6
- Well Engineering & Construction: Hussain Rabia, Chapters 1 & 2

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- اگر pore ها interconnected باشند ← pore pressure به h و دانسته سیال محسوب درستی دارد.

- هرچند pore pressure صفر باشد به این معنی است که یا pore ها از ازل حاوی سیال نبوده اند و یا اینکه بعداً سیال مهاجرت کرده است. در این مورد برای حفاری از عوا استفاده می کنیم.



Introduction: Pore Pressure

- اگر وزن گل کم باشد differential striking پیش می آید.
- اگر وزن گل حفاری را افزایش دهیم و تا پایان باید وزن Max حفاری کنیم، ROP پایینی می آید.

The magnitude of the pressure in the pores of a formation, known as the **formation pore pressure** (or simply **formation pressure**), is an important consideration in many aspects of well planning and operations.

Applications:

- Mud weight selection (prevent borehole collapsing and influx)
- Casing depth Selection
- Casing design
- Well control: risk of blowout
- Prevent Hole problems : lost of circulation, stuck pipes, ROP etc

Well Design

- به علت وجود Key set ارتباط صبر و استقامت قطع می شود. تمام نیرو در این حالت بر یک سطح کوچک وارد شده و در نتیجه نیروی لازم برای بالا کشیدن لوله افزایش خواهد یافت. (differential striking)

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- روشی های رفع ۱- وزن گل را افزایش دهیم.

۲- باید سیال مخصوصی برای لوله زنی بپیم و لوله را آزاد کنیم. differential striking

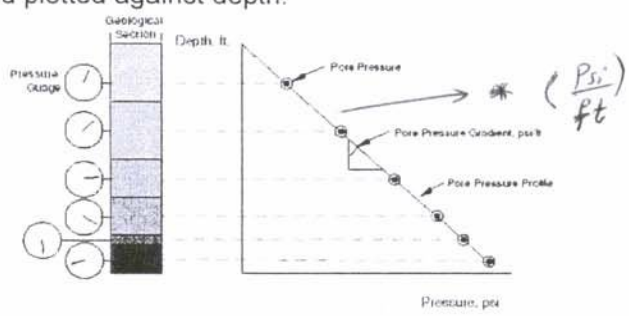
- در هنگام tripping ممکن است به علت تمیز شدن دیواره های چاه، مایه طابری stabilizer جمع شده و با بالابردن بیش بایست گیاه شدن لوله های شود.

- ساختار لوله های وزنی به صورت spiral از differential sticking جلوگیری می کند.



Pressure Gradient

The pressure of the fluid in the pore space (the pore pressure) can be measured and plotted against depth.



The pressure in the formations to be drilled is often expressed in terms of a **pressure gradient**. This gradient is derived from a line passing through a particular formation pore pressure and a datum point at surface and is known as the pore pressure gradient.

5 وقتی سازند متخلخل باشد و این متخلخل عا به هم راه داشته و حاوی سیال باشند، فشار pore عا به هم و سیال موجود در سنگ ها به سگی دارد.
* این خط را pressure gradient می گویند.



Normal Pressure Gradient

Normal pressure gradients correspond to the hydrostatic gradient of a fresh or saline water column

آب خالص $C_w = 62.4 \text{ pcf}$
آب اشباع شده و سیال مذاب $C_{sw} = 72 \text{ pcf}$

Most of the fluids found in the pore space of sedimentary formations contain a proportion of salt and are known as brines. The dissolved salt content may vary from 0 to over 200,000 ppm. Correspondingly, the pore pressure gradient ranges from **0.433 psi/ft** (pure water) to about **0.50 psi/ft**. In most geographical areas the pore pressure gradient is approximately **0.465 psi/ft** (assumes 80,000 ppm salt content) and this pressure gradient has been defined as the normal pressure gradient.

6 - این حالت برای وقتی اسکان تمام pore عا به هم ارتباط دارند و کاملاً از آب اشباع شده باشند.

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Normal Pressure Gradient

Normal Pore Pressure when strata are in direct communication (8.94 ppg) = 66.96 pcf

$$P_o = 0.465 \text{ psi/ft}$$

Abnormal Pore Pressure when adjacent strata are not in direct communication

Note: All abnormal pressures require some means of sealing or trapping the pressure within the rock body. Otherwise hydrostatic equilibrium back to a normal gradient would eventually be restored.

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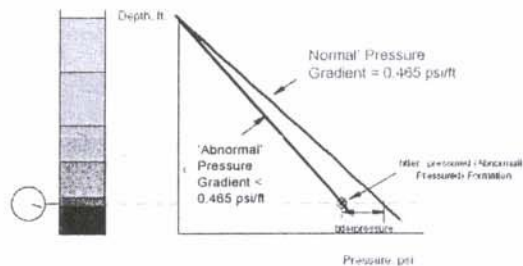
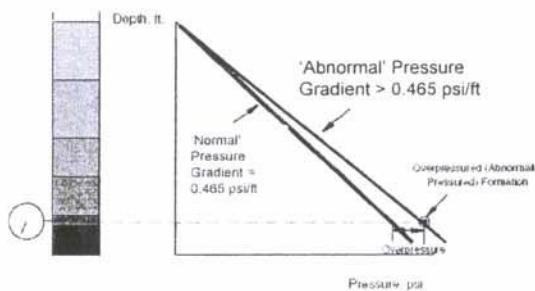


Abnormal Pressure

سازندگی که گرادین فشار آن بیشتر از ۰.۴۶۵ باشد را abnormal می‌گویند

Overpressured

Underpressured (Subnormal pressured)



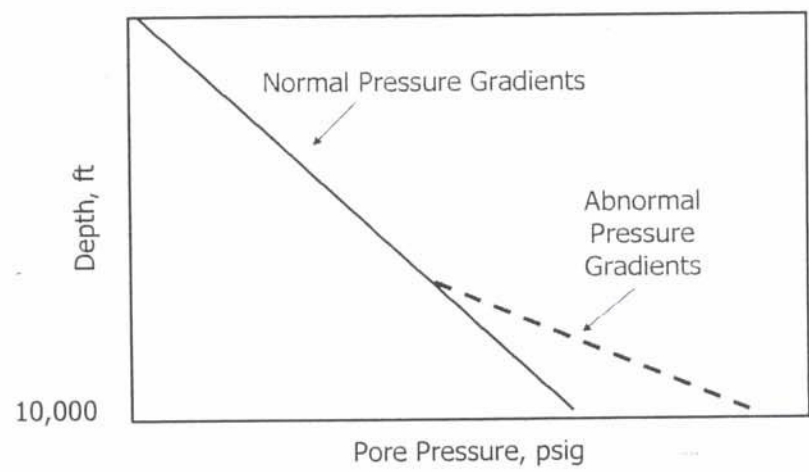
سازندگی که گرادین فشار آن کمتر از ۰.۴۶۵ باشد subnormal یا depletion می‌گویند.

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Abnormal Pressure



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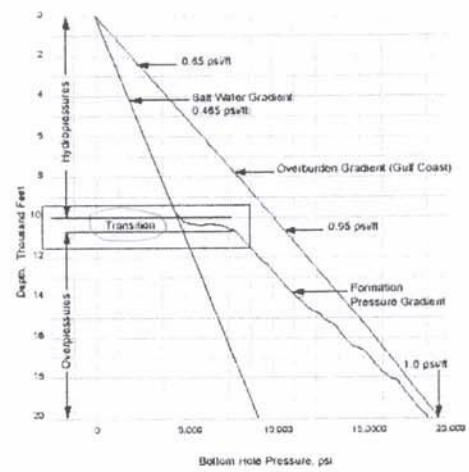


این ناحیه توسط
زنی شناخته می شود

Transition zone

منطقه ای که تغییر فشار gradient به طور
غیر طبیعی تغییر کند و این قسمت برای
نوله گذاری مهم است.

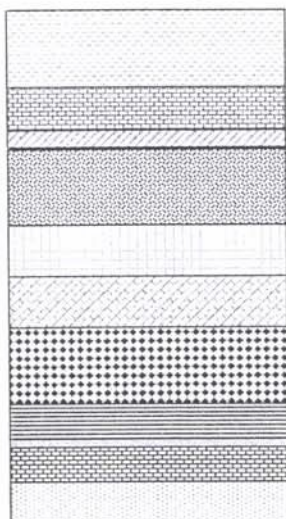
The zone between the normally pressured zone and the overpressured zone is known as the transition zone.



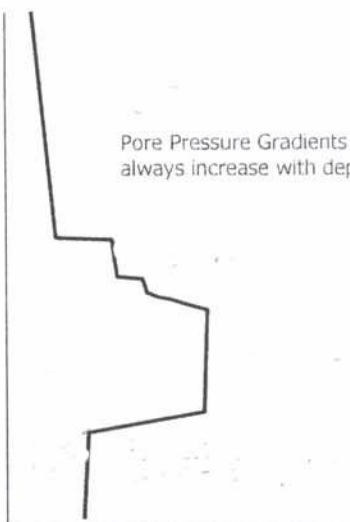
آزاد شود
↑
اگر فشارها
slope کند این
gradient به طور طبیعی خواهد شد

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Abnormal Pressure



Depth



Pore Pressure Gradients do not always increase with depth

Pore Pressure

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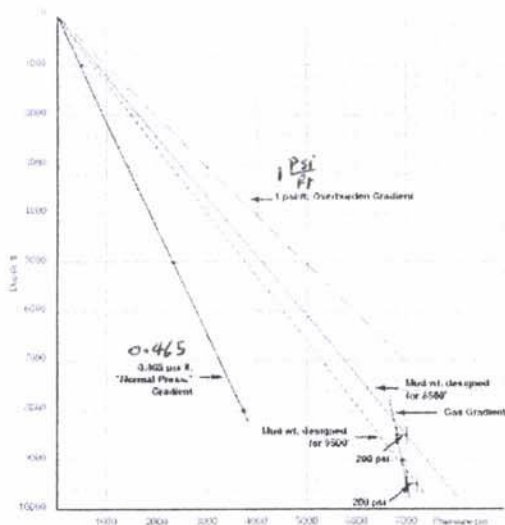
حداقل وزن گلی نه های کانی بسیار کم و مایه های آب و گاز ویل است با وزن ۵۵ پف

Example 6.4 252

Exercise 6.5 295

Example-1 : Pore Pressure Profile

a- The following pore pressure information has been supplied for the well you are about to drill. Plot the following pore pressure/depth information on a P-Z diagram



DEPTH BELOW DRILLFLOOR (ft)	PRESSURE (psi)
0	0
1000	465
5000	2325
8000	3720
8500	6800
9000	6850
9500	6900

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$$HP_{(psi)} = P_h = 0.052 MW_{(ppg)} \times depth_{(ft)} = \frac{MW_{(pcf)} \times depth_{(ft)}}{144}$$

$$HP_{(psi)} = P_h = \frac{MW_{(pcf)} \times depth_{(m)}}{144} \times 3.281$$

(mud) hydrostatic pore
 $P_h > P_p$ با بیش از
 $P_h < P_p$ کمتر از



Example-1 : Pore Pressure Profile

b. Calculate the pore pressure gradients in the formations from surface; to 8000 ft; to 8500 ft; and to 9000 ft. Plot the overburden gradient (1 psi/ft) on the above plot. Determine the mud weight required to drill the hole section: down to 8000ft; down to 8500ft; and down to 9000ft.

Assume that 200 psi overbalance on the formation pore pressure is required

The pore pressure gradients in the formations from surface are:

0 - 8000 ft	$3720/8000 = 0.465$ psi/ft
0 - 8500 ft	$6800/8500 = 0.800$ psi/ft
0 - 9500 ft	$6900/9500 = 0.726$ psi/ft

Required Mudweight:

@ 8000 ft	
$3720 + 200 = 3920$ psi	
$3920/8000 = 0.49$ psi/ft $\Rightarrow 9.42$ ppg	

@ 8500 ft	$6800 + 200 = 7000$ psi
$7000/8500 = 0.82$ psi/ft $= 15.77$ ppg ≈ 118 pcf	

@ 9500 ft	$6900 + 200 = 7100$ psi
$7100/9500 = 0.75$ psi/ft $= 14.42$ ppg	

$$0.433 \frac{psi}{ft} = 1 SG$$

$$1 \frac{psi}{ft} = 144 pcf$$

$$1 ppg = 7.48 pcf$$

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Example-1 : Pore Pressure Profile

c. If the mudweight used to drill down to 8000ft were used to drill into the formation pressures at 8500ft what would be the over/underbalance on the formation pore pressure at this depth?

If the mudweight of were 9.42 ppg were used to drill at 8500 ft the underbalance would be:

$$6800 - (8500 \times 9.42 \times 0.052) = 2636 \text{ psi}$$

Hence the borehole pressure is 2636 psi less than the formation pressure.

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✓



Example-1 : Pore Pressure Profile

- d. Assuming that the correct mudweight is used for drilling at 8500ft but that the fluid level in the annulus dropped to 500 ft below drillfloor, due to inadequate hole fill up during tripping. What would be the effect on bottom hole pressure at 8500ft ?

If, when using 0.82 psi/ft (or 15.77 ppg) mud for the section at 8500ft, the fluid level in the hole dropped to 500ft the bottom hole pressure would fall by:

$$500 \times 0.82 = 210 \text{ psi}$$

Hence the pressure in the borehole would be 210 psi below the formation pressure.



Example-1 : Pore Pressure Profile

- e. What type of fluid is contained in the formations below 8500ft?

The density of the fluid in the formation between 8500 and 9500 ft is:

$$\frac{6900 - 6800}{1000} = 0.1 \text{ psi/ft}$$

The fluid in the formations below 8500 ft is therefore gas.



Sources of Abnormal Pressure

عوامل مختلف که باعث $pressure\ up$ یکسان می شود:

- Tectonics (Faults etc) → مثل: عوامل جابجایی گسل
- Rock diagenesis (Sulfates, clays, etc) → وقتی درگیری اتفاق می افتد و سنگ با مواد دیگر واکنش دهد، گرانید شده و سیال $expand$ می شود و $cap\ rock$ متراکم می آید.
- Surface erosion
- Thermal effects
- External Pressure sources
- etc → کیفیت سیال اطراف لوله جاری کافی نباشد. $loss$ شدن سیال در اطراف لوله جاری که باعث می شود در قسمتی از سازند فشار زیاد شود.

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Methods of Estimating Pore Pressure

Direct measurement of formation pressure is expensive and is possible when the formation has been drilled. (usually are performed to estimate the PI)

Techniques for detecting and estimating abnormal formation pressure often are classified as :

- ① Predictive methods → روشی مای که قبل از حفاری مای پرسی می کشیم
- ② Methods applicable while drilling (Detection Techniques)

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Predictive Methods

Geophysical measurements are generally used to identify geological conditions which might indicate the potential for overpressures such as salt domes which may have associated overpressured zones.

Estimates of formation pressures made before drilling are based primarily:

- ① - Correlation available data from nearby wells (development wells)
- ② - Seismic Surveys (wildcats) توسعه ای

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Predictive Methods

-Non Pay Zones: (indirect measurements)

- Offset well histories may contain information on mud weights used, problems with stuck pipe, lost circulation or kicks.
- Common Sense

- Pay Zones : (Direct Measurements)

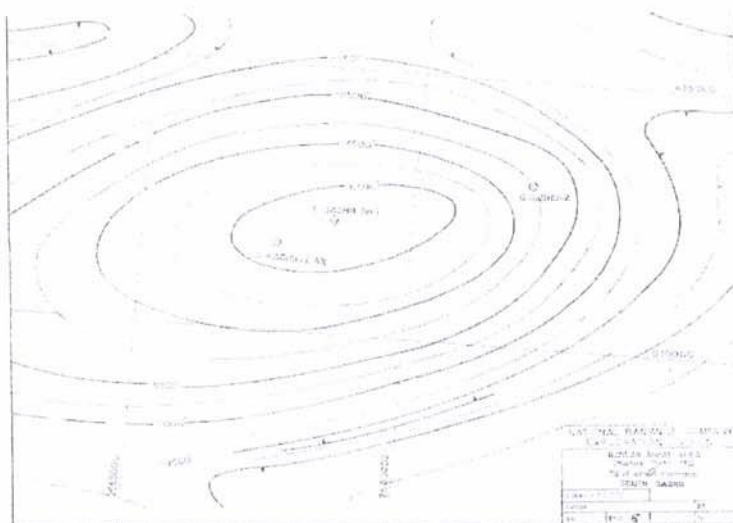
- Known Oil, Gas & Water Pressure at a specific datum depth
- DST, Wire-line Surveying, Production Engineering data base
- $P_o, P_g, P_w, GOC, WOC, \gamma_o, \gamma_g, \gamma_w$

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1.



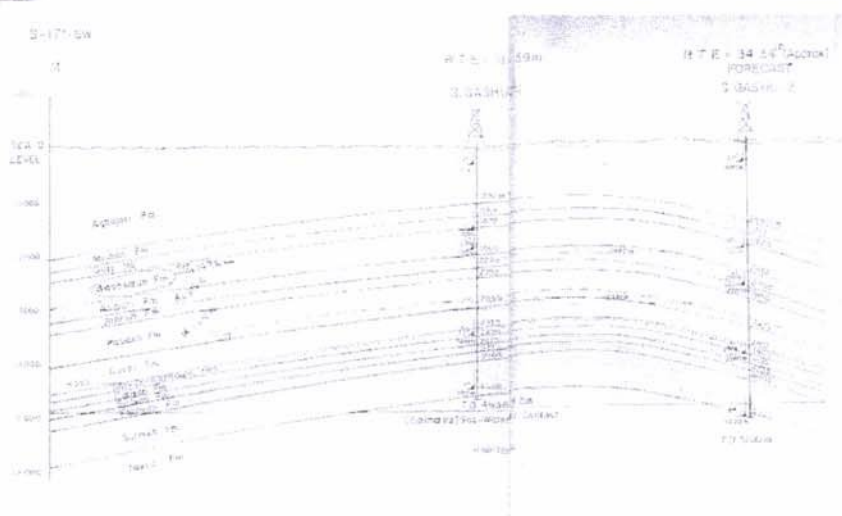
Predictive Methods: Offset Wells



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Predictive Methods: Offset Wells



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Predictive Method: Compaction Theory

Mechanisms which generate the abnormal pore pressures can be quite complex and vary from region to region. However, the most common mechanism for generating overpressures is called **under-compaction**.

Compaction theory:

- ✓ If formation pressures are normal, the porosity-dependent parameter should have an easily recognised trend because of the decreased porosity with increased depth of burial and compaction. *اگر فشار سازندگی روند طبیعی داشته باشد، با افزایش عمق (compaction)، ϕ کاهش می یابد.*
- ✓ A departure from the normal pressure trend signals a probable transition zone. *اگر یک تغییر ناگهانی در فشار normal سازندگی داشته باشیم، منطقه Transitive است.*
- ✓ Detection of the depth at which this departure occurs is critical because casing must be set in the well before excessively pressured permeable zones can be drilled safely. *این منطقه بحرایی که تغییر ناگهانی (departure) داریم مهم است. چون باید casing در اینجا رانده شود.*

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Summary of Compaction Theory of Abnormal Pressure

- ✓ Best fits most naturally occurring abnormal pressures
- ✓ During deposition, sediments are compacted by the overburden load and are subjected to greater temperatures with increasing burial depth.
- ✓ Porosity is reduced as water is forced out.
- ✓ Hydrostatic equilibrium within the compacted layers is retained as long as the expelled water is free to escape
- ✓ If water cannot escape, abnormal pressures occur
- ✓ The average porosity in sediments, generally decreases with increasing depth - due to the increasing overburden. This results in an increasing bulk density with increasing depth, and increasing rock strength

Compaction theory

← **Goal: To Develop a relationship between porosity and bulk density**

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Overburden Pressures

فشار ناشی از
عین طبقات بالای

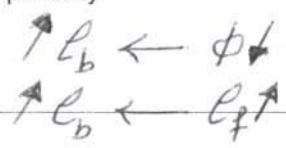
- The vertical pressure at any point in the earth is known as the **overburden pressure** or **geostatic pressure**.
- The overburden pressure at any point is a function of the mass of rock and fluid above the point of interest.

In order to calculate the overburden pressure at any point, the average density of the material (rock and fluids) above the point of interest must be determined. The average density of the rock and fluid in the pore space is known as the **bulk density** of the rock.

$$\rho_b = \rho_g - (\rho_g - \rho_f)\phi$$

دستی دارد به: ۱) دانسیته سنگ
۲) متخلخل
۳) دانسیته سیالی که سنگ را اشباع کرده

ρ_b = bulk density of porous sediment
 ρ_g = density of rock matrix
 ρ_f = density of fluid in pore space
 ϕ = porosity



$\rho_b = \rho_g$ ← اگر صفت غیر متخلخل باشد
مثال: سنگ مرمر

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Overburden Pressures

Since the matrix material (rock type), porosity, and fluid content vary with depth, the bulk density will also vary with depth. The overburden pressure at any point is therefore the integral of the bulk density from surface down to the point of interest

ρ_b با جابجای مجموع ρ_g های
Lithology های مختلف

Typical Densities of Rocks and Fluids

Lithology	Matrix Density (g/cc)
Sandstone	2.65
Limestone	2.71
Dolomite	2.87
Anhydrite	2.98
Halite	2.03
Gypsum	2.35
Clay	~2.7-2.8
Fresh Water	1.0
Salt Water	1.15
Oil	0.80

روش های اندازه گیری ρ_b :
Sources of density data:

1. Density measurements of rock samples using "shale density" techniques. بعد از حفاری ρ_b سنگ را با روشی که در کتاب از طریق cutter های wire اندازه گیری می کنند.
2. Measurements of rock in situ. Using density logs to directly measure the electron density and the bulk density of the rock around the borehole, or from core samples at surface. با استفاده از well log
3. Measurements of Porosity. → Neutron Porosity Logs
• Nuclear Magnetic Resonance studies of cuttings
• Sonic Logs
4. Offset Tables → م و سله های tables



Maximum Overburden Pressure

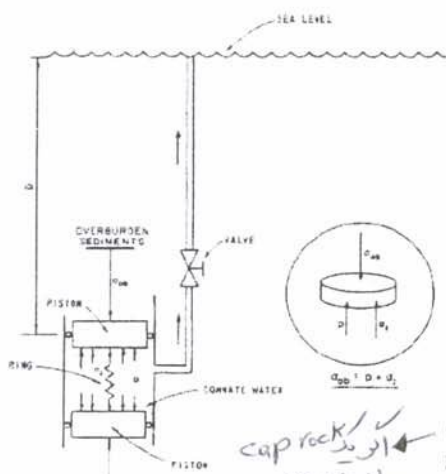
The specific gravity of the rock matrix may vary from 2.1 (sandstone) to 2.4 (limestone). Therefore, using an average of 2.3 and converting to units of psi/ft, it can be seen that the overburden pressure gradient exerted by a typical rock, **with zero porosity** would be:

$$2.3 \times 0.433 \text{ psi/ft} = 0.9959 \approx 1 \text{ psi/ft} \rightarrow \text{حد اکثر فشار} \\ \text{Pressure} \\ \text{مورد انتظار از یک سنگ} \\ \text{در حالتی که تخلخل ندارد}$$

نکته: $1 \text{ SG} = 0.433 \frac{\text{psi}}{\text{ft}}$



Compaction Effects



Pore water expands with increasing burial depth and increased temperature, while the pore space is reduced by increasing geostatic load. Thus, normal formation pressure can be maintained only if a path of sufficient permeability exists to allow formation water to escape readily.

$$\sigma_{ob} = \sigma_z + p$$

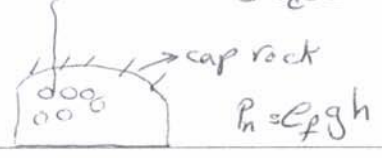
σ_z : matrix Stress \rightarrow مقاومت خود سنگ

p : the pore fluid pressure \rightarrow فشار سیال داخلی سنگ

If the expelled water is not free to escape, abnormal pressures may result.

abnormal pressure \rightarrow فشار غیر طبیعی

cap rock \rightarrow تاج سنگ
escape \rightarrow فرار از سنگ



فشار آن دیگر موجود نیست \rightarrow خطی نیست

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Vertical Overburden Stress

The vertical overburden stress resulting from geostatic load at a sediment depth, D_s , for sediments having an average bulk density, ρ_b , is given by:

$$\sigma_{ob} = \int_0^{D_s} \rho_b g dD,$$

where g is the gravitational constant.

$$\rho_b = \rho_g - (\rho_g - \rho_f)\phi$$

→ برای محاسبه این
رابطه یا ϕ و یا
 E_p را باید به ما بداند.

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Compaction theory

The average porosity in sediments, generally decreases with increasing depth -due to the increasing overburden.

به طور معمول با افزایش عمق که باعث جاذبه و E_p افزایش می یابد.

This results in an increasing bulk density with increasing depth, and increasing rock strength

- 1) Plot ϕ_o Vs. Depth on similog graph.
- 2) Construct a plot of bulk density vs. depth
- 3) Calculate overburden stress vs. depth.

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Bulk Density

In an area of significant drilling activity, the change in bulk density with depth usually is determined by conventional **well logging** methods. The effect of depth on average bulk density for sediments in the Texas and Louisiana gulf coast areas is shown in Fig

The change in bulk density with burial depth is related primarily to the change in sediment porosity with compaction. Grain densities of the common minerals found in sedimentary deposits do not vary greatly and usually can be assumed constant at a representative average value. This is also true for pore fluid density.

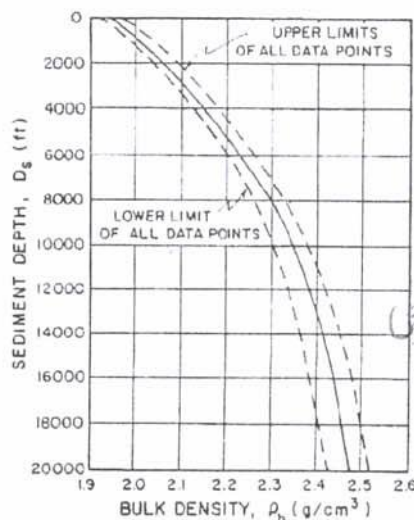


Fig. 6.3—Composite bulk density curve from density log data for the U.S. gulf coast.

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Bulk Density-Porosity Relationship

In many areas, it is convenient to use the **exponential relationship** relating change in average sediment porosity to depth of burial when calculating the overburden stress, σ_{ab} , resulting from geostatic load at a given depth. To use this approach; **the average bulk density data** are expressed first in terms of average porosity.

$$\phi = \frac{\rho_s - \rho_b}{\rho_s - \rho_f} \rightarrow \text{معادله رابطه } \phi \text{ و } \rho_b$$

Handwritten notes: 'Lithology: ρ_s بدست می آید.' (Lithology: ρ_s is obtained.) and 'slide رابطه 29' (slide relationship 29).

This equation allows average bulk density data read from well logs to be expressed easily in terms of average porosity for any assumed grain density and fluid density. If these average porosity values are plotted vs. depth on semi-log paper, a good straight-line trend usually is obtained. The equation of this line is given by:

$$\phi = \phi_0 e^{-KD_s}$$

Handwritten notes: 'overburden pressure' and 'سطح زمین' (ground surface).

where ϕ_0 is the surface porosity, K is the porosity decline constant, and D_s is the depth below the surface of the sediments. The constants ϕ_0 and K can be determined **graphically** or by the **least-square method**.

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Example-2

example 6-2

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Determine values for surface porosity, ϕ_0 and porosity decline constant, K , for the U.S. gulf coast area. Use the average bulk density data shown in Fig. 6.3, an average grain density of 2.60 g/cm³, and an average pore fluid density of 1.074 g/cm³.

exercise 6.1 295
6.2

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Example-2: Solution

The porosity calculations are summarized in Table 6.2.

The bulk density given in Col. 2 was read from Fig. 6.3 at the depth given in Col. 1. The porosity values given in Col. 3 were computed using an average grain density of 2.60 and a fluid density of 1.074 g/cm³ in Eq. 6.3b

$$\phi = \frac{2.60 - \rho_b}{2.60 - 1.074} = \frac{2.60 - \rho_b}{1.526}$$

The computed porosities are plotted in Fig. 6.4

TABLE 6.2—AVERAGE SEDIMENT POROSITY COMPUTATION FOR U.S. GULF COAST AREA

(1) Sediment Thickness D_s (ft)	(2) Bulk Density ρ_b (g/cm ³)	(3) Average Porosity ϕ (frac.)
0	1.95	0.43
1,000	2.02	0.38
2,000	2.06	0.35
3,000	2.11	0.32
4,000	2.16	0.29
5,000	2.19	0.27
6,000	2.24	0.24
7,000	2.27	0.22
8,000	2.29	0.20
9,000	2.33	0.18
10,000	2.35	0.16
11,000	2.37	0.15
12,000	2.38	0.14
13,000	2.40	0.13
14,000	2.41	0.12
15,000	2.43	0.11
16,000	2.44	0.10
17,000	2.45	0.098
18,000	2.46	0.092
19,000	2.47	0.085
20,000	2.48	0.079

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نکته: اگر جوابی سوال می برای lithology را داده بود،
باید برای بدست آوردن ϕ مختلف در اینجا مختلف،
می مخصوص به آن می را وارد می.



Example-2: Solution- cont

A surface porosity, ϕ_0 of 0.41 is indicated on the trend line at zero depth. A porosity of 0.075 is read from the trend line at a depth of 20,000 ft. Thus, the porosity decline constant is

$$K = \frac{\ln \frac{\phi_0}{\phi}}{D_s} = \frac{\ln \left(\frac{0.41}{0.075} \right)}{20,000} = 0.000085 \text{ ft}^{-1}$$

and the average porosity can be computed using

$$\phi = 0.41 e^{-0.000085 D_s}$$

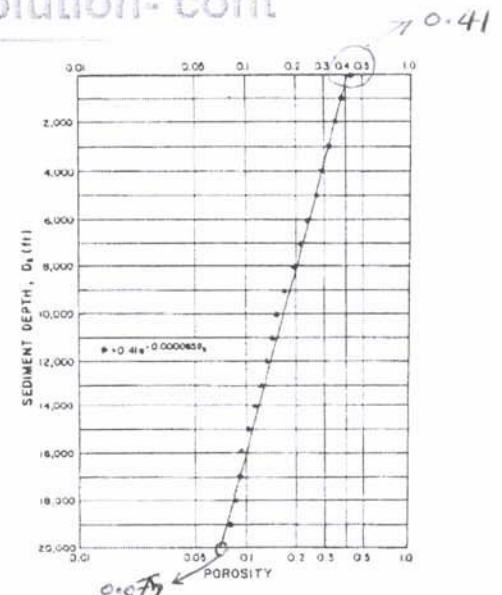


Fig. 6.4—Computed average porosity trend for U.S. gulf coast areas.

mud line. *به خط کف دریا mud line گیند* *sea level*

موتی در خط کف دریا mud line چاهی زده شود، سست mud line را خطب
کود تا بعد از در خاکم ایجاد platform بتوان
از چاه بهره برداری



Vertical Overburden Stress - Offshore

Recalling: For onshore

$$\sigma_{ob} = g \int_0^D [\rho_s (1 - \phi) + \rho_f \phi] dD$$

example 6.3
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In offshore areas, this Eq. must be integrated in two parts. From the surface to the ocean bottom, the seawater density, ρ_{sw} is equal to 8.5 lb_m/gal and the porosity is 1.

$$\sigma_{ob} = g \int_0^{D_w} \rho_{sw} dD + g \int_{D_w}^D [\rho_s - (\rho_s - \rho_f) \phi_0 e^{-KD}] dD$$

exercise 6.4
295

Integration of this equation and substitution of D_s ($D - D_w$), the depth below the surface of the sediments, yields

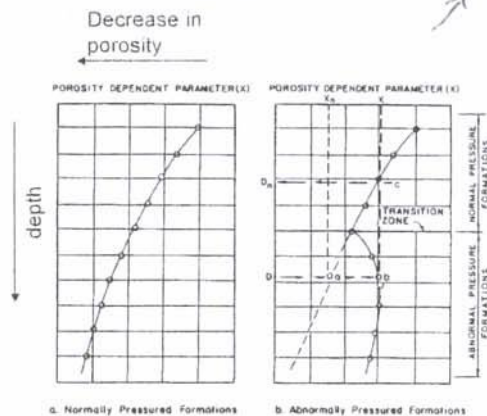
$$\sigma_{ob} = \rho_{sw} g D_w + \rho_s g D_s - \frac{(\rho_s - \rho_f) g \phi_0}{K} (1 - e^{-K D_s})$$



Pore pressure prediction

این نمودار در صورتی که خطی است = semi-log = خطی است

1. Measure the porosity indicator (e.g. density) in normally pressured, clean shales to establish a normal trend line.
2. When the indicator suggests porosity values that are higher than the trend, then abnormal pressures are suspected to be present.
3. The magnitude of the deviation from the normal trend line is used to quantify the abnormal pressure.



تئوری compaction

در این شکل چون

derivation (انحراف) وجود دارد

abnormal pressure وجود دارد

37

① Equ matrix stress

از مقدار انحراف
مقدار فشار را حدسی می زنیم

روشی دیگر: ratio method

از طریق empirical formula

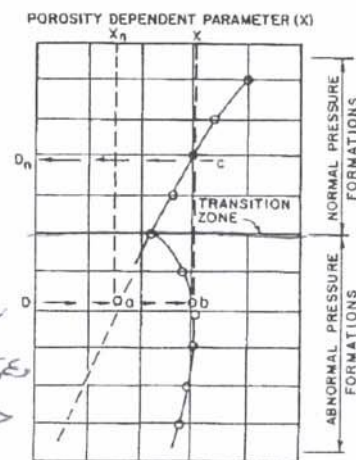
این دوروش بسیار گران قیمت بوده و کار برد ندارد
و در جای هایی مثل مناطق نفت خیز جنوب چون اطلاعات فشاری را داریم، احتیاج به این دوروش نیست



Approach 1: Equivalent matrix stress

This approach is based on the assumption that similar formation having the same value of the porosity-dependent variable are under the same effective matrix stress σ_z .

Thus the matrix stress σ_z of the abnormally pressured formation at depth D is the same as matrix stress state σ_{zn} of a more shallow normally pressured formation at depth D_n which gives the same measured value of the porosity dependent parameter.



$$\sigma_z = \sigma_{zn} = \sigma_{obn} - P_n$$

در نقطه c به با با است. σ_{obn} is evaluated at D_n

در نقطه c به با با است. σ_{obn} is evaluated at D_n

The pore pressure at depth D:

$$P = \sigma_{ob} - \sigma_z$$

مقدار فشاری
مقدار

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Approach 1: Equivalent matrix stress

$$\sigma_z = \sigma_{zn}$$

$$\text{i.e. } \sigma_{ob} - p = \sigma_{obn} - p_n$$

$$p = p_n + (\sigma_{ob} - \sigma_{obn})$$

pore pressure

normal pressure gradient

معمولاً در خاک رس: $0.433 \frac{\text{psi}}{\text{ft}}$

equivalent depth



b. Abnormally Pressured Formations



Example 3

Estimate the pore pressure at 10,200' if the equivalent depth is 9,100'. The normal pore pressure gradient is 0.433 psi/ft. The overburden gradient is 1.0 psi/ft.

این مثال ← از طریق compacted theory

$$\text{At } 9,100', p_n = 0.433 * 9,100 = 3,940 \text{ psig}$$

$$\text{At } 9,100', \sigma_{ob} = 1.00 * 9,100 = 9,100 \text{ psig}$$

$$\text{At } 10,200', \sigma_{ob} = 1.00 * 10,200 = 10,200 \text{ psig}$$

$$p = p_n + (\sigma_{ob} - \sigma_{obn})$$

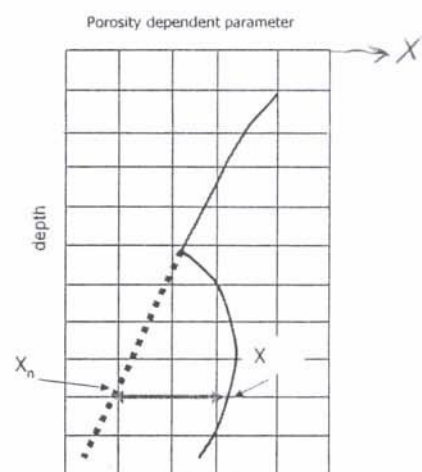
$$= 3,940 + (10,200 - 9,100) = 5040 \text{ psig}$$



Approach 2: Ratio Method

■ Empirical correlations

- More accurate than approach 1
- Need considerable data
- uses (X/X_n) or $(X-X_n)$ to predict the magnitude of the abnormal pressure

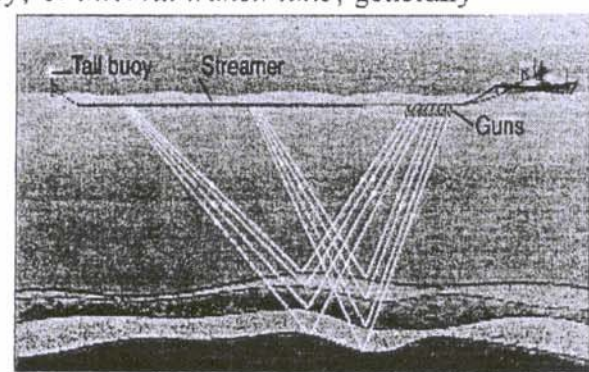


جای این روش به کتاب مراجعه می کنید



Predictive Methods- Seismic data

To estimate formation pore pressure from seismic data, the average acoustic velocity as a function of depth must be determined. A geophysicist who specializes in computer-assisted analysis of seismic data usually performs this for the drilling engineer. For convenience, the reciprocal of velocity, or *interval transit time*, generally is displayed.



٢١



Seismic data

The observed interval transit time t is a porosity dependent parameter that varies with porosity, ϕ according to:

eq 6.7: $t = t_{ma}(1 - \phi) + t_{fl}\phi$

t_{ma} : the interval transit time in the rock matrix
 t_{fl} : the interval transit time in the pore fluid

TABLE 6.3—REPRESENTATIVE INTERVAL TRANSIT TIMES FOR COMMON MATRIX MATERIALS AND PORE FLUIDS

Matrix Material	Matrix Transit Time (10^{-5} s/ft)	
Dolomite	44	
Calcite	46	
Limestone	48	
Anhydrite	50	
Granite	50	
Gypsum	53	
Quartz	56	
Shale	62 to 167	
Salt	67	
Sandstone	53 to 59	
Pore Fluid		
Water (distilled)	218	
100,000 ppm NaCl	208	
200,000 ppm NaCl	189	
Oil	240	
Methane	626*	
Air	910*	

*Valid only near 14.7 psia and 60°F.

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Seismic data

Under normal compaction, density increases with depth. For this reason the interval velocity also increases with depth, so travel time decreases

To find a mathematical model of the normal compaction trend for interval transit time can be developed by substituting the exponential porosity expression defined previously into the above Eq.:

$$\phi = \phi_o e^{-KD_s}$$

$$\ln \left[\frac{t}{\phi_o(t_{fl} - t_{ma})} - \frac{t_{ma}}{\phi_o(t_{fl} - t_{ma})} \right] = -KD$$

exercice 6.3 295

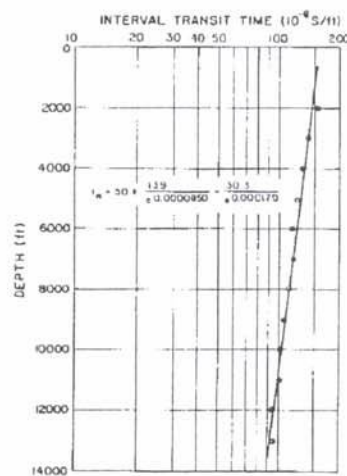


Fig. 6.12—Normal-pressure trend line for interval transit time computed from seismic data in upper Miocene trend of the U.S. gulf coast area

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Example 4

The average interval transit time data shown Table were computed from seismic records of normally pressured sediments occurring in the Upper Miocene trend of the Louisiana gulf coast. These sediments are known to consist mainly of sands and shales. Using these data and the values of K and ϕ_0 computed previously for the U.S. gulf coast area in Example 2, compute apparent average matrix travel times for each depth interval given and curve fit the resulting values as a function of porosity. A water salinity of approximately 90,000 ppm is required to give a pressure gradient of 0.465 psi/ft.

TABLE 6.4—AVERAGE INTERVAL TRANSIT TIME DATA COMPUTED FROM SEISMIC RECORDS OBTAINED IN NORMALLY PRESSURED SEDIMENTS IN UPPER MIOCENE TREND OF GULF COAST AREA¹

Depth Interval (ft)	Average Interval Transit Time (10 ⁻⁴ s/ft)
1,500 to 2,500	153
2,500 to 3,500	140
3,500 to 4,500	132
4,500 to 5,500	126
5,500 to 6,500	118
6,500 to 7,500	120
7,500 to 8,500	112
8,500 to 9,500	106
9,500 to 10,500	102
10,500 to 11,500	103
11,500 to 12,500	93
12,500 to 13,500	96

example 6.5 285.0
 exercise 6.7 295.0
 exercise 6.8 295.0
 exercise 6.14 295.0

exercise 6.9 295.0

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Solution

The values of ϕ_0 and K determined for the U.S. gulf coast area in Example 2 were 0.41 and 0.000085 ft⁻¹, respectively. From Table 6.3, a value of 209 is indicated for interval transit time in 90,000-ppm brine. Inserting these constants in Eqs. 6.4 and 6.7 gives

$$\phi = 0.41e^{-0.000085D} \quad \text{and} \quad t_{mu} = \frac{t - 209\phi}{1 - \phi}$$

For the first data entry in Table 6.4, the mean interval depth is 2,000 ft and the observed travel time is 153 μ s/ft. Using these values for D and t yields

$$\phi = 0.41e^{-0.000085(2,000)} = 0.346 \quad \text{and} \quad t_{mu} = \frac{153 - 209(0.346)}{1 - 0.346} = 122 \mu\text{s/ft.}$$

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Solution cont

TABLE 6.5—EXAMPLE CALCULATION OF APPARENT MATRIX TRANSIT TIME FROM SEISMIC DATA

Average Depth (ft)	Average Porosity (%)	Average Interval Transit Time (10 ⁻³ s/ft)	Apparent Matrix Transit Time (10 ⁻³ s/ft)
2,000	0.346	153	122
3,000	0.318	140	109
4,000	0.292	132	100
5,000	0.268	126	96
6,000	0.246	118	89
7,000	0.226	120	94
8,000	0.208	112	87
9,000	0.191	106	82
10,000	0.175	102	79
11,000	0.161	103	83
12,000	0.148	93	73
13,000	0.136	96	78

A plot of matrix transit time vs. porosity is shown in Fig. 6.11. From this plot, note that for the predominant

shale lithology of the U.S. gulf coast area, the average matrix transit time can be estimated by

$$t_{ma} = 50 + 180\phi$$

Use of this expression for t_{ma} and 209 for t_d in Eq. 6.7 gives

$$t_a = 50 + 339\phi - 180\phi^2$$

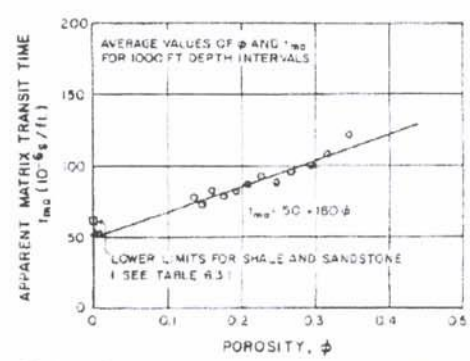


Fig. 6.11—Relationship between matrix transit time and porosity computed for sediments in the upper Miocene trend of the U.S. gulf coast area.

روش های گفته شده، برای بدست آوردن pore pressure قبل از حفاری هستند، معمولاً به صورت تجربی و گرافیکی بوده است.



Detection Techniques

Estimation of Formation pressure while drilling:

- ❖ ROP (correlations)
- ❖ Qualitative measurements:

Hole conditions → اتنا ماتی که در حفاری پیش می آید
 Gas cut mud → گاز وارد گلی می شود، detector حساسی دارد
 Flowline temp. → دمای خروجی گد را اندازه گیری می کنند
 Pit levels (kicks) → حساسی های kick و هوز روی گلی که با مایه دانا
 Direct flow check → pit level را اندازه گرفته و ارتفاع آن را اندازه می گیریم.
 درون چاه نگاه می کنند و می بینند گلی یا سی
 می رود (در حفاری هوز روی) و یا بالایی آید و
 داخل pit tank می ریزد (در حفاری kick) است.

به طور انتظا ردارم، با افزایش عمق ← سرعت حفاری کمتر شود
مگر در موارد خاصی که بیان می شود



ROP → Rate of penetration (سرعت حفاری)

The use of the ROP to detect transition and therefore overpressured zones is a simple concept, but difficult to apply in practice.

The theory behind using drilling parameters to detect over pressured zones is based on the fact that:

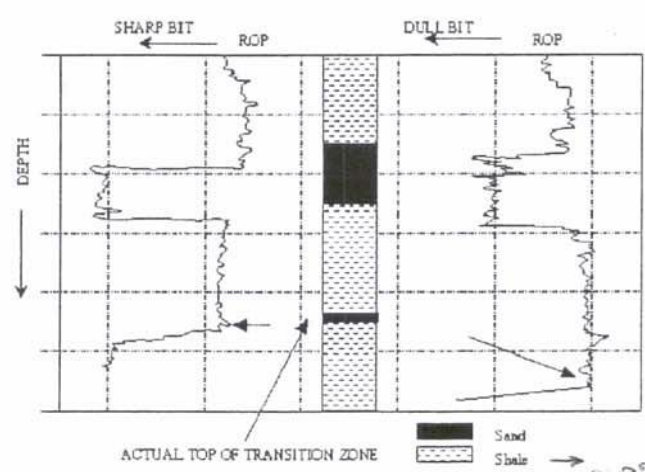
- Compaction of formations increases with depth. ROP will therefore, all other things being constant, decrease with depth
- In the transition zone the rock will be more porous (less compacted) than that in a normally compacted formation and this will result in an increase in ROP. Also, as drilling proceeds, the differential pressure between the mud hydrostatic and formation pore pressure in the transition zone will reduce, resulting in a much greater ROP

در حوضه ناحیه transition نزدیک شوم، اختلاف فشار سازند (pore pressure) و گل با کم تر شده ← ROP بیشتر می شود.



ROP

ROP As An Indicator of Overpressure



shale

ACTUAL TOP OF TRANSITION ZONE

Sand
Shale

در سازند shale چون 50

pore pressure زیاد بود و سیال sealing شده، در نتیجه اجازه خروج مایع را دارد و در نتیجه اختلاف فشار بین سازند و گل بوجود آمده و بهمان طور که در شکل مشخص است، ROP کاهش می یابد.



Limitations of ROP

ROP

The rate of penetration is affected by numerous parameters:

➤ Weight On Bit (WOB)

➔ ROP افزایش می یابد ← با افزایش WOB

➤ RPM

➔ ROP ↑ RPM

➤ bit type

➤ bit wear

➤ hydraulic efficiency

➤ degree of overbalance

➤ drilling fluid properties

➤ hydrostatic pressure

➤ hole size

یعنی کل با اعمال فشار روی سنگ مانع از حفاری می شود

حرف و زن کل شما بیشتر شود ← chip hold-down effect

بیشتری شود (یعنی ROP کمتری شود)

با افزایش وزن کل، ROP کاهش می یابد

حرف و زن کمتری می باشد
باید همه دارای طول دندان کوچکتر
و تعداد دندان بیشتر باشد

حفاری در size کوچکتر دارای ROP بیشتر است

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روشی "d"

"d" exponent

➔ ما چگونه بفهمیم که داریم

normal pressure حفاری می کنیم یا به صورت abnormal

The "d" exponent technique for detection of overpressures is based on a normalised drilling rate equation developed by Bingham (1964):

$$R = aN^e \left(\frac{W}{B} \right)^d$$

R = penetration rate (ft/hr)

N = rotary speed (rpm)

W = WOB (lb)

B = bit diameter (in.)

a = matrix strength constant

d = formation drillability

e = rotary speed exponent

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example 6.7 page 261
exercise 6.20 page 296



Modified "d" exponent

این روش، پارامترهای
روشن قبل را کاهشی می دهد

Removing the variables which are dependent on lithology and rotary speed:

- the rock which was being drilled did not change ($a = 1$)
- the rotary speed exponent (e) was equal to one



the resulting equation can only be applied to one type of lithology and theoretically at a single rotary speed.

$$\frac{R}{N} = \left(\frac{W}{B} \right)^d$$

$$d = \frac{\log\left(\frac{R}{N}\right)}{\log\left(\frac{W}{B}\right)}$$

$$d = \frac{\log\left(\frac{R}{60N}\right)}{\log\left(\frac{12W}{10^3 B}\right)}$$

$\frac{ft}{hr} \rightarrow R$
 $rpm \rightarrow N$
 $K-lbf \rightarrow W$
 $in \rightarrow B$

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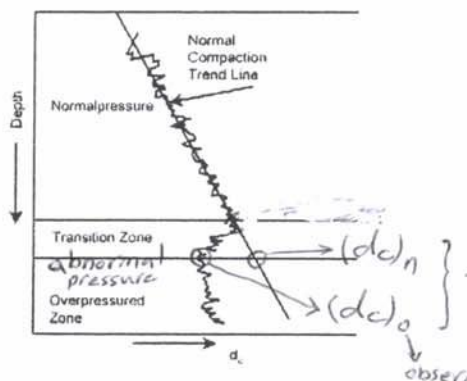
با افزایش عمق d افزایش می یابد.



"d" exponent

- the D exponent attempts to correct the ROP for changes in RPM, weight on bit and hole size.
- The **D exponent** is proportional to **rock strength** and for normally pressured formations, the **D exponent increases linearly with depth**, reflecting increased rock strength with depth.
- For **abnormally pressured shales**, the D exponent deviates from the normal trend and actually decreases with depth.

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روشن قبل را کاهشی می دهد



Eaton Method

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✓ با افزایش د_c hold-down Effect (افزایش یافته) ← ROP کاهش می یابد



"d_c" exponent

the d-exponent equation takes no account of mudweight. Since mudweight determines the pressure on the bottom of the hole the greater the mudweight the greater the chip hold-down effect and therefore the lower the ROP. A modified d-exponent (d_c) which accounts for variations in mudweight has therefore been derived

در معادله d_c صحیحی از MW_n نشده که این پارامتر در معادله می آید.

$$d_c = d \left(\frac{MW_n}{MW_a} \right)$$

MW_n = "normal" mud weight

MW_a = actual mud weight

or

$$d_c = d \left(\frac{NPP}{ECD} \right)$$

d_c = corrected D Exponent (dimensionless)

NPP = normal pore pressure gradient (ppg)

ECD = equivalent circulating density (ppg)

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Pore pressure calculation from d_c exponent - Eaton Method

depth در برابر d_c رسم

1. Record the value of the normal trendline d_c (d_{cn}) and observe d_c (d_{co}) at the depth of interest. NOTE: use only d_{co} values from shales. Do not use any other lithology d_c value.
2. Record the overburden gradient from the overburden plot at the depth of interest. (از این نمودار برداشته می آید)
3. Use the following formula to calculate pore pressure:

$$\frac{PP}{D} = \frac{\sigma_{ov}}{D} - \left(\frac{\sigma_{ov}}{D} - \frac{P_n}{D} \right) \times \left(\frac{d_{co}}{d_{cn}} \right)^{1.2}$$

Pore pressure gradient
psi/ft

Overburden stress gradient
psi/ft

Normal Pore pressure gradient
psi/ft

d_{co} = Observed value of d_c at depth of interest

d_{cn} = Normal trendline value of d_c at depth of interest

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Pore pressure calculation from d_c exponent - Ratio Method

The ratio method is much simpler and does not require values of overburden. To calculate pore pressure, use the following formula

مقدار آن داده می شود. (در یک منطقه خاص)

$$\frac{PP}{D} = \frac{P_n}{D} \times \left(\frac{d_{cn}}{d_{co}} \right)$$

d_{co} = Observed value of d_c at depth of interest

d_{cn} = Normal trendline value of d_c at depth of interest

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Tutorial # 1

- Whilst drilling the 12 1/4" hole section of a well the mudloggers were recording the data as shown in the table below. Plot the d and d_c exponent and determine whether there are any indications of an overpressured zone.
- If an overpressured zone exists, what is the depth of the top of the transition zone.
- Use the Eaton equation to estimate the formation pressure at 8600 ft. Assume a normal formation pressure of 0.465 psi/ft. an overburden gradient of 1.0 psi/ft and a normal mud weight for this area of 9.5 ppg.

DEPTH (ft.)	ROP (ft./hr)	RPM	WOB (,000 lbs)	MUD WEIGHT PPG
7500	125	120	38	9.5
7600	103	120	38	9.5
7700	77	110	38	9.5
7800	66	110	38	9.6
7900	45	110	35	9.6
8000	37	110	37	9.8
8100	40	110	35	9.8
8200	42	110	33	9.9
8300	41	100	33	10.0
8400	44	100	38	10.25
8500	34	100	38	10.25
8600	33	100	40	11
8700	32	110	42	11

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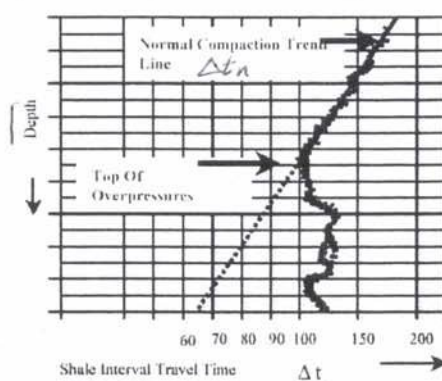
۲۹



Pore pressure calculation- Sonic Log

The sonic log measures the transit time (t) for a compressional sonic wave to travel through the formation from transmitter to receiver. The time to travel through one foot (or one metre) is termed the Interval Transit Time (ITT). In a shale sequence showing a normal compaction profile (and therefore normal pressure); the transit time should decrease with depth due to the decreased porosity and increasing density.

Abnormally pressured shales tend to have higher porosity and lower density than normally pressured shales at the same depth. Hence the ITT values will be higher.



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در ناحیه‌ی shale، ITT افزایش می‌یابد. →



Pore pressure calculation- Sonic

By constructing a logarithmic plot of ITT vs linear depth a normal pressure trendline can be established through clean shales. Abnormally pressured shales will therefore show an increased ITT above the normal trendline value at the depth of interest. Pore pressure can then be calculated at the point of interest using the following Eaton equation:

$$\frac{PP}{D} = \frac{\sigma_{ov}}{D} - \left(\frac{\sigma_{ov}}{D} - \frac{P_n}{D} \right) \times \left(\frac{\Delta t_n}{\Delta t_o} \right)^3$$

PP= Pore Pressure (psi)

σ_{ov} = Overburden (psi)

P_n = Normal pore pressure (psi)

Δt_n = Normal pore pressure trend line t value at depth of interest

Δt_o = Observed t value at the depth of interest.

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Fracture Gradient فشار شکست سازند

When abnormal formation pressure is encountered, the density of the drilling fluid must be increased to maintain the wellbore pressure above the formation pore pressure to prevent the flow of fluids from permeable formations into the well. However, since the wellbore pressure must be maintained below the pressure that will cause fracture in more shallow, relatively weak, exposed formation just below the casing seat, there is a maximum depth into the abnormally pressured zone to which the well can be drilled safely without cementing another casing string in the well.

باید فشار شکست سازند را در نظر گرفت و چگالی مایع حفاری را افزایش داد تا فشار مایع حفاری از فشار پore formation بیشتر باشد. اما چون فشار شکست سازند در عمق کمتری اتفاق می افتد، پس باید چگالی مایع حفاری را به قدری افزایش داد تا فشار مایع حفاری از فشار شکست سازند کمتر باشد. این عمق را Min Fracture grad می گویند. (Min Fracture grad = Minimum Fracture Gradient)



فشار شکست سازند در عمق کمتری اتفاق می افتد. برای جلوگیری از این کار باید چگالی مایع حفاری را به قدری افزایش داد تا فشار مایع حفاری از فشار شکست سازند کمتر باشد. این عمق را Min Fracture grad می گویند. (Min Fracture grad = Minimum Fracture Gradient)

باید مقدار فشار شکست سازند را به وسیله این روش تعیین کرد:



Fracture Gradient

Predictive Methods:

- Empirical Correlations (the pore pressure should be predicted first by one of the correlations)

Verification Methods:

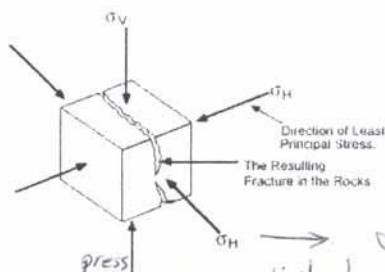
- Experimental methods
 - Leak-off Test
 - Limit Test
 - Formation Breakdown Test

Fracture Gradient

- **Fracture Gradient Test:** A test carried out to the leak off point and beyond until the formation around the wellbore fails. The fracture gradient is equal to the earth minimum horizontal stress.

درجهت مقاومت سنگ ضعیف باشد، در همان جهت شکست می شود.

- In order to avoid lost circulation while drilling it is **important** to know the variation of **fracture gradient** with depth.

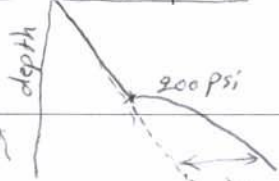


عموماً شکست
سازند در جهه غالب این
صورت می یابد.

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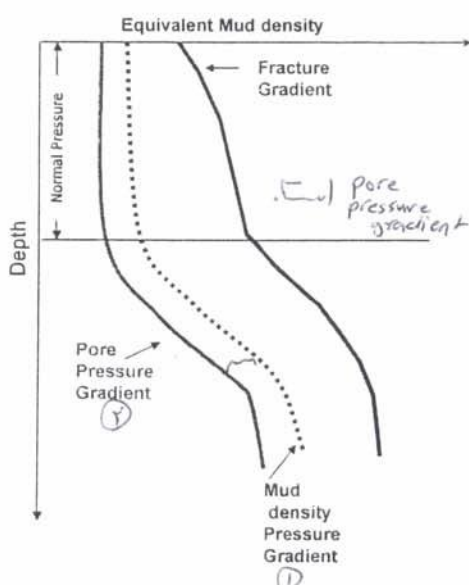
فشار در ردی به عمق
مردم نظر
 $2000 + P = \rho g h$
این فشار برای
ایستادن سازه
بدست می آید
 C_{mud}

σ_v
 $\rho_o d_o \delta_o$
 $\rho_g d_g \delta_g$
 $\rho_w d_w \delta_w$



دلیل ایند جواب افزایش عمق، اختلاف افزایش
می یابد!
چون μ_w که مایه همیشه تراکم سازند

Fracture Gradient



میزان وزن کل به فرجه Fracture gradient و pore pressure gradient است.

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اختلاف ① و ② برابر با overbalance press است.
و درجهت به عمق بیشتر می شود ← اختلاف ② و ③ بیشتر می شود



Hubbert and Willis method

زمانی fracture اتفاق می افتد که فشار تزریق بزرگتر از

The method is based on the premise that fracturing occurs when the applied fluid pressure exceeds the sum of the minimum effective stress and formation pressure. The fracture plane is assumed to be always perpendicular to the minimum principal stress. According to the Hubbert and Willis method, the total injection (or fracturing) pressure required to keep open and extend a fracture is given by:

$$FG = \sigma'_3 + P_f \quad \text{formation pressure}$$

where σ'_3 is the effective minimum principal stress (= minimum principal stress minus pore pressure)

In terms of overburden gradient, Poisson's ratio (ν) and formation pressure, the above equation becomes:

$$\text{Fracture gradient} \leftarrow FG = \left(\frac{\nu}{1-\nu} \right) \left(\frac{\sigma_v - P_f}{D} \right) + \frac{P_f}{D} \quad \text{formation pressure}$$

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Poisson's ratio

Poisson's ratio is a rock property that describes the behaviour of rock stresses (σ_l) in one direction (least principal stress) when pressure (σ_p) is applied in another direction (principal stress).

$$\frac{\sigma_l}{\sigma_p} = \frac{\nu}{1-\nu}$$

Laboratory tests on unconsolidated rock have shown that generally:

$$\frac{\sigma_l}{\sigma_p} = \frac{1}{3}$$

Field tests however show that ν may range from 0.25 to 0.5 at which point the rock becomes plastic (stresses equal in all directions). Poisson's ratio varies with depth and degree of compaction

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این روش برای مراحل عملیاتی آسان است ولی ریسک زیاد دارد و برای یک لایه خاص است و بهای آن پائینی نمی توان تعیین داد.

Experimental methods

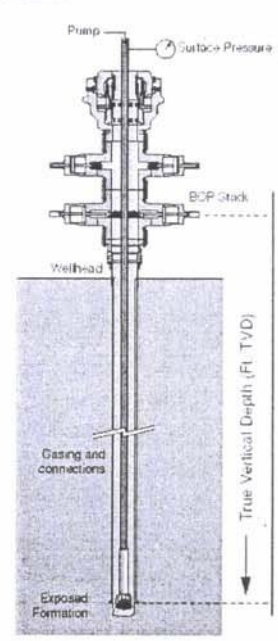


The procedure used to conduct these tests is basically the same in all cases. The test is conducted immediately after a casing has been set and cemented. The only difference between the tests is the point at which the test is stopped.

FLP, shoe Band test = leak-off test =

The procedure is as follows:

1. Run and cement the casing string
2. Run in the drill string and drill bit for the next hole section and drill out of the casing shoe
3. Drill 5 - 10 ft of new formation below the casing shoe
4. Pull the drillbit back into the casing shoe
5. Close the BOPs (generally the pipe ram) at surface



Burst 2000 psi

چاه بسته است
shut-in casing pressure
چون ما فشار casing را در gauge می خوانیم

فشار داخل: فشار بسته ی چاه (SICP)

در اینجا (شکل) ما ۳ safety valve (Kelly check) داریم.

SBT: تستی برای اطمینان از عدم damage بودن casing، قبل از عملیات حفاری casing مراداده و فشار 2000 psi به صورت shut-in casing pressure می کنیم تا ببینیم که casing ما سالم است و یا نه. اعمال شده برای تستی که برآیند سازند.

(الف) - shoe Band Test (این تست معمولاً انجام می شود)



Procedure

6. Apply pressure to the well by pumping a small amount of mud (generally 0.5 bbl ← 1/2 bbl) into the well at surface. Stop pumping and record the pressure in the well. Pump a second, equal amount of mud into the well and record the pressure at surface. Continue this operation, stopping after each increment in volume and recording the corresponding pressure at surface. Plot the volume of mud pumped and the corresponding pressure at each increment in volume.

(Note: the graph shown in Figure represents the pressure all along the wellbore at each increment. This shows that the pressure at the formation at leak off is the sum of the pressure at surface plus the hydrostatic pressure of the mud).

7. When the test is complete, bleed off the pressure at surface, open the BOP rams and drill ahead



Leak-off test

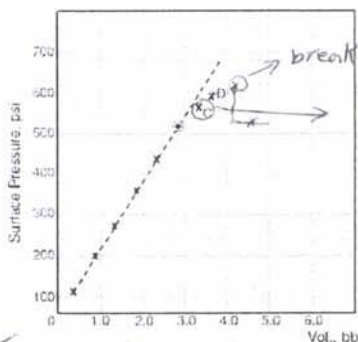
(ب) این تست معمولاً
انجام می شود
چون با این تست می توان
سازندگی را مشخص کرد

The "Leak-off test" is used to determine the pressure at which the rock in the open hole section of the well **just starts to break down** (or "leak off"). In this type of test the operation is terminated when the pressure no longer continues to increase linearly as the mud is pumped into the well

- این نمودار ریسکی دارد

① معیار compressibility سیال

② محوطه چاه (محیط پستی) را می بینیم



(سازندگی می شود)
و ضروری کامل پیدا کنیم
(سازندگی نشده)
و ضروری ناقص است

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تقریباً ۰.۵ bbl اضافه کرد تا وقتی که سازندگی نشود
ای نمودار به صورت خط صاف است

- این تست leak-off در جایی که موقعیت را نمی شناسیم، انجام می گیرد.

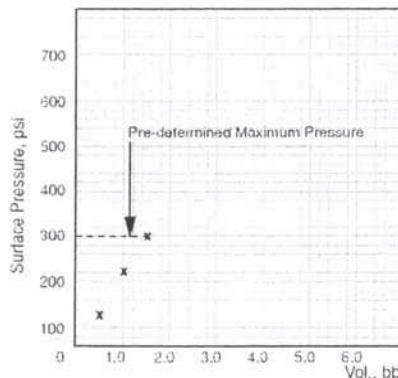


Limit Test (FIT)

The "Limit Test" or "Formation Integrity test, FIT" is used to determine whether the rock in the open hole section of the well will withstand a **specific, predetermined pressure**. This pressure represents the maximum pressure that the formation will be exposed to whilst drilling the next wellbore section. The pressure to volume relationship during this test is shown in Figure below. This test is effectively a limited version of the leak-off test.

- حداکثر وزن کل در حلقه (تجه) مشخص است.

در این تست می خواهیم ببینیم که در منطقه ای
که داریم حفاری می کنیم آیا سازندگی
حداکثر فشار را دارد و یا نه که در صورت
ضرورت وقتی بیشتر که ۱۰۰۰ psi ب درون
چاه داریم، ضروری با افزایش وزن کل
پیدا نکنیم.



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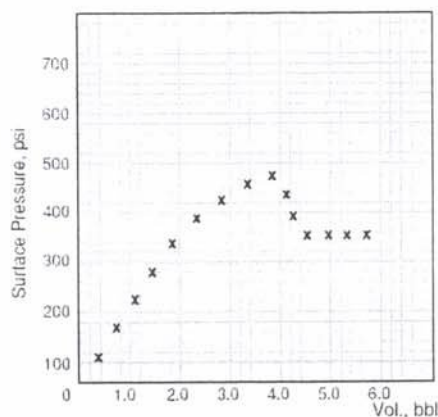
در policy حفاری این تست باید در ضعیف ترین
سازندگی حداکثر فشار را در آن منطقه تست کرده و ببینیم که سازندگی
فشار را تحمل می کند یا خیر

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Formation Breakdown Test

The "Formation Breakdown Test" is used to determine the pressure at which the rock in the open hole section of the well completely breaks down. If fluid is continued to be pumped into the well after leak off and breakdown occurs the pressure in the wellbore will behave as shown in Figure below.



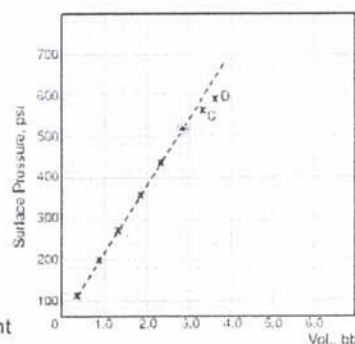
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Leak Off Test Calculations

In a Leak-Off test the formation below the casing shoe is considered to have started to fracture at point C on Figure shown. The surface pressure at point C is known as the leak off pressure and can be used to determine the **maximum allowable pressure** on the formation below the shoe. The maximum allowable pressure at the shoe can subsequently be used to calculate:

- ✓ • The maximum mudweight which can be used in the subsequent open hole section
- ✓ • The Maximum Allowable Annular Surface Pressure (MAASP)



The maximum allowable pressure on the formation just below the casing shoe is generally expressed as an **equivalent mud gradient (EMG)** so that it can be compared with the mud weight to be used in the subsequent hole section.

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Leak Off Test Calculations

Given the pressure at surface when leak off occurs just below the casing shoe, the maximum mudweight that can be used at that depth, and below, can be calculated from :

$$\begin{aligned} & \text{Maximum Mudweight (psi/ft)} \\ &= \frac{\text{Pressure at the shoe when Leak-off occurs}}{\text{True Vertical Depth of the shoe}} - \frac{\text{Pressure at surface and hydrostatic pressure of mud in well}}{\text{True Vertical Depth of the shoe}} \end{aligned}$$

0.5 ppg
 leak-off
 depth shoe
 safety factor

Usually a safety factor of 0.5 ppg (0.026 psi/ft) is subtracted from the allowable mudweight.

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exercise 6-31 298



Example

While performing a leak off test the surface pressure at leak off was 940 psi. The casing shoe was at a true vertical depth of 5010 ft and a mud weight of 10.2 ppg was used to conduct the test.

The Maximum bottom hole pressure during the leakoff test can be calculated from:

$$\begin{aligned} & \text{hydrostatic pressure of column of mud + leak off pressure at surface} \\ &= (0.052 \times 10.2 \times 5010) + 940 \\ &= 3597 \text{ psi} \end{aligned}$$

leak off

the maximum allowable mud weight at this depth is therefore

$$= 3597 / 5010$$

$$= 0.718 \text{ psi/ft} = 13.8 \text{ ppg}$$

✓ Allowing a safety factor of 0.5 ppg.

The maximum allowable mud weight = 13.8 - 0.5 = 13.3 ppg.

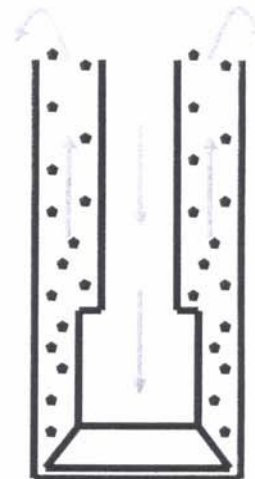
باید حداکثر فشار را در کاسینگ شوی
از این بیشتر نشود و چون می سازند
بیشتر از این می سازند.

حداکثر وزن مایه‌ای که می توانیم بدون مشکلی اعمال می کنیم.
(Max leak off pressure)

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Drilling Hydraulics

A. Hashemi, PhD



مهم پارامتری که در hydraulic بررسی می شود و برای عملیات حفاری مهم است.

WOB (۱)
RPM (۲)
پمپ کردن درون چاه (flow rate) (۳)

تغییر flow rate درون چاه می تواند به وای flow rate چه مقدار افت فشار خواهد داشت.

انواع افت فشار

1) Sacrificial pressure losses: drillstring → برای آغاز عملیات حفاری، کار مفید انجام نمی دهد، باید Minimize شود.

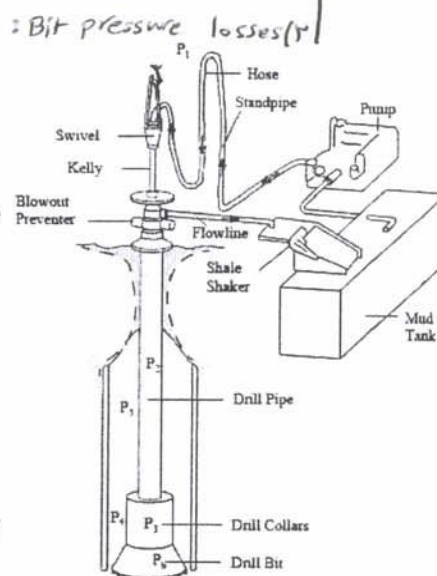
Introduction

• The magnitude of the resistance to flow is dependant on a number of variables

• The resistance is expressed in terms of the amount of pressure required to circulate the fluid around the system: circulating pressure of the system

• Sacrificial Pressure Losses : The pressure required to circulate the fluid through the drillstring and annulus (do not contribute anything to the drilling process but cannot be avoided)

• Bit Pressure Loss: perform a useful function helps to clean the drilled cuttings from the face of the bit



عوامل مختلف در ایجاد افت فشار و انتخاب jet در bit مؤثر است: ① شکل چاه ② size چاه

① Surge وقتی بکسریت زیاد لوله ها را به پایین trip کنیم ، یک فشار مضاعف به سازند اعمال می شود و باعث ایجاد fracture در سازند می شود. عموماً کل سنگی تر باشد، احتمال ایجاد fracture می شود.

در حالت casing راندن ای فشار بیشتر است از وقتی که drill string می رانیم.
② Swab: وقتی که با سرعت زیاد لوله ها را به بالا بکشیم و یک افت فشار در پایین ایجاد شده و ممکن است flow به درون چاه پیدا کنیم.

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Objectives اهداف محاسبه هیدرولیک:

- The pressure along the borehole while circulating (equivalent circulating density – ECD) ← در هنگام گردش کل درون چاه ، فشار را محاسبه می کنیم.
- The pressure along the borehole while moving the drillstring (surge and swab pressures) ← در حالت نامیپ چاه پوش بوده و خارج trip انجام می دهیم ، فشار را محاسبه می کنیم.
- The optimum circulating parameters and bit nozzle sizes
- The cuttings transport capacity of the fluid (hole cleaning) ← ظرفیت حمل cutting های کل حفاری
- The pressure along the borehole during well control operations (kick removal) ← در هنگام Kick فشار را محاسبه می کنیم.
- Surge and swab pressure due to drillstring movement ← در هنگامی که surge و swab اعمال می شود ، فشار را محاسبه می کنیم.

افت فشار در دالینز + فشار هیدرواستاتیکی لوله (ECD (equivalent circulating density
↓
با افزایش flow rate ، افت فشار در دالینز بیشتر خواهد بود.

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Hydraulic Optimization

- Optimize the pressure losses through the Bit: clean the bit face

بهرینه کردن عملیات حفاری
که بهترین جا برای بهینه کردن در حته می باشد.
و کمترین هزینه در حته داشته باشیم.

– Poor cleaning results in:

- Deposit of cutting on well bottom
- Making bridge ← در دالینز افت فشار بیشتر می شود ، باعث هزینه های زیاد می شود.
- Stuck pipes
- Reduction of ROP → متوقف شدن کل شدن و balling up شده و ROP کاهش می یابد.

- Minimize the sacrificial losses in the drillstring and annulus

Hydraulic Power

- The product of the circulating pressure losses and the flowrate through the system is equal to the hydraulic power that the mud pumps will have to generate

hydraulic horse power

$$HHP_t = \frac{P_t \times Q}{1714}$$

P_t = Total pressure (psi)

Q = flow rate (gpm)

$$\Delta P_t = \Delta P_s + \Delta P_{bit} \quad \xrightarrow{\times \frac{Q}{1714}} \quad HHP_t = HHP_s + HHP_{bit}$$

Sacrifice (system) loss

حاصل ضرب $Q \times \Delta P$ ثابت است } $Q \times \Delta P = \text{constant}$

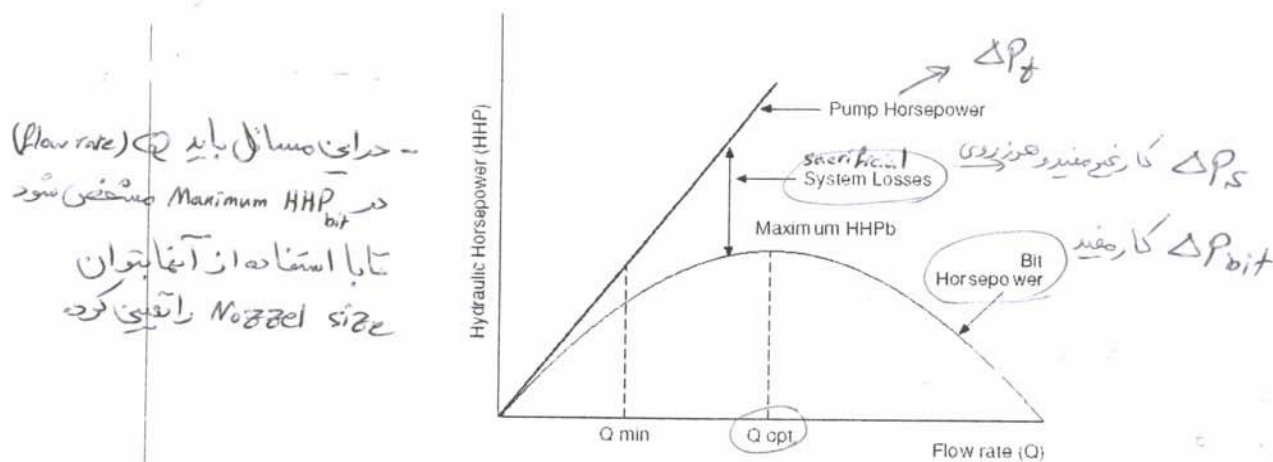
اگر قطر bit زیاد باشد و Q افزایش یابد ΔP کاهش می یابد و چاه را با افزایش Q تمیزی کنیم.

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Hydraulic Optimization

اگر قطر bit کمتر باشد و Q کاهش یابد ΔP افزایش یابد و چاه را با اجمال ΔP تمیزی کنیم.

- There is, for all combinations of drillstring, nozzle size and hole size, an **optimum** flow rate for which the hydraulic power at the bit is maximised



- برای مسائلی باید Q (Flow rate) در $Maximum\ HHP_{bit}$ مشخص شود تا با استفاده از آن بتوان $Nozzle\ size$ را تعیین کرد

چون $turbulence$ (افزایش می یابد) و ΔP افزایش می یابد و Q و توان کاهش می یابد.

Factors for optimization ✓

❶ • The minimum annular velocity

❷ • ^{افت فشار} The pressure losses: in the drillstring,
across the nozzles & in the annulus

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❸ Forces acting in annulus

When mud is rising in the annulus, the cuttings are simultaneously affected by three forces: سه نیروی کنده ها وارد می شود

- **Gravity**: acting downward & tends to fall the cuttings on the bottom of the well.

The velocity of falling down is called **slip velocity, V_s** →

- **Buoyancy force**, every time acting upward

- A force resulting from **Pump Pressure**, this force causes a specific velocity on each part of the stream. (**Annular velocity**)

کنده
- وزن مخصوص
- شکل هندسی کنده
- ویسکوزیته

نیروی ناشی از بالا آمدن
flow rate
دره به وسیله
و به وسیله پمپ ایجاد می شود

Annular velocity

Relative velocity = Annular velocity - slip velocity > 0

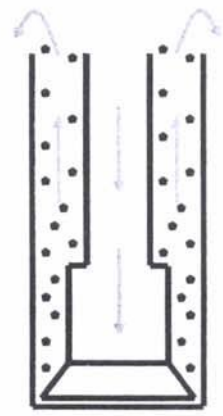
$$V_r = A_v - V_s$$

ANNULAR VELOCITY

$$Av(FPM) = \frac{24.51 \times PumpOutput (GPM)}{D^2 - d^2}$$

- ✓ D: Well diameter or ID of Casing (in)
- ✓ d: OD of DPs or Dcs (in)

A_v is proportional to pump output and reciprocal to well diameter



9.

Optimum annular velocity

← optimum کردن فواید زیر را دارد:

Optimum A_{vs} :

- clean the bit face
- carry the cuttings quickly
- avoid heavy hydrostatic head
- reduce the lost of circulation risk
- reduces the breaking of large cuttings

← optimum را بدست می آوریم تا حداقل GPM را تقویت کنیم

← فواید کل خوبی از flowline با آن ورودی که fresh است موقتاً می کند و فواید کل برآورد وجود solid و کثیفی در کل با آنست (افزایش می شود که با آنست hydraulic fracture و ضروری در جاه خواهیم داشت.

→ برتر شدن cutting ها با آنست افزایش Reology کل شده و ضروری تصفیه کننده های برتر بیشتر است، ما باید کثیفی ها را به صورت درست به سطح بیاوریم.

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Optimum annular velocity

← انتخابی چاه های ایران تعیین شده.



Hole Size (in)	Annular velocity (FPM)
17 1/2	80
12 1/4	90
10 5/8	110
8 3/4	120
7 7/8	130
6	140

hole size \leftarrow گاه های
Annular velocity \leftarrow افزایش

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Optimum annular velocity

Smith recommended:

(light Mw)

گاز های سبک

$$Annular\ velocity = \frac{11800}{Mw \times D_H}$$

$$GPM_{min} = \frac{Annular\ velocity \times (D_H^2 - d^2)}{24.51}$$

Mw= PPG

D_H= Hole diameter (in)

d= OD of DP

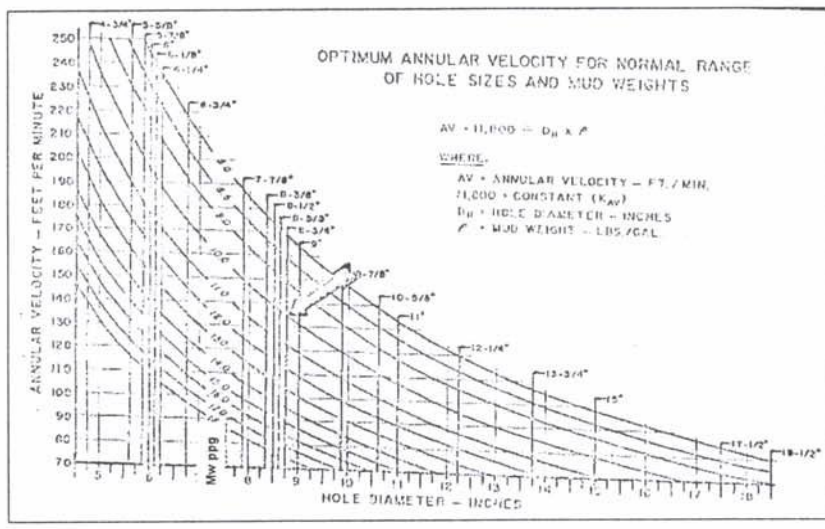
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پیل: برای تمرکز در چاه و بعد از هر سه یا چهار ستافه کل با viscosity بالا که پیل نامیده می شود استفاده می شود.

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Optimum annular velocity



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Min GPM

Hole Size (in)	Min GPM
26	1350
17 1/2	815
12 1/4	490
8 3/4	270
6 1/8	220

مهم: حداقل ۱۰۰۰ GPM می توانیم به وسیله دو پیل استفاده کنیم، برای این hole size ما نمی توانیم ۱۳۵۰ gpm استفاده کنیم. Reology کل

۱) Annular velocity را عوض نمی کنیم (مواد درون کل) بهترین توان کل را سنجی کرده Annular velocity را کاهش می دهیم ۲) سرعت حفاری را کمی کم کنیم ۳) معمولاً hole size های ۲۶" و معمولاً عمق آن ۶۰ تا ۷۰ متر است.

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✓ The magnitude of the pressure losses

بستگی دارد به:

- The **geometry** of circulating system (USUALLY IS FIXED)

- The **flowrate** (limited by the maximum power output by the mudpumps and the maximum pressures which can be tolerated by the pumping system.)

①: limitation: فشار که بیشتر → از یک حدی توان پیدا کرد ②: توانی که پیدا کرد.
 ①: توانی که در دسترس است (توان پمپ)
 ②: که شامل فشار رو پمپ است که نمی تواند از یک حد بیشتر پیدا کنیم

- The **flow regime** in which the fluid is flowing (laminar/turbulent)

- The **rheological** properties of the circulating fluid

خواص علم الکلیا سیال
 ①: خواص سیال PV (plastic viscosity) و ②: YP (Yield point)
 15

که تعیین می کند ما این مدلی را استفاده کنیم (نیوتونی، توانی، بینگهام)

✓ Bernoulli's equation:

“at any point of an ideal steady state incompressible flow system the sum of the specific kinetic energy, the pressure, and the specific potential energy and pressure is constant”

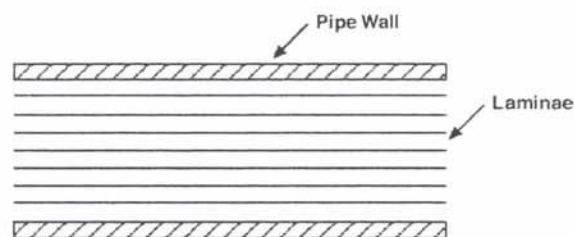
or, in mathematical terms:

$$\frac{1}{2} \rho \bar{v}^2 + p + \rho g h = \text{constant}$$

Flow regimes © A. Hashemi 2008

در جریان دغوی محاسبی \rightarrow فضا متفاوت است

- **Laminar Flow (Streamline or Viscous flow) :**
 - In this type of flow, layers of fluid move in streamlines or laminar. There is no microscopic or macroscopic intermixing of the layers.

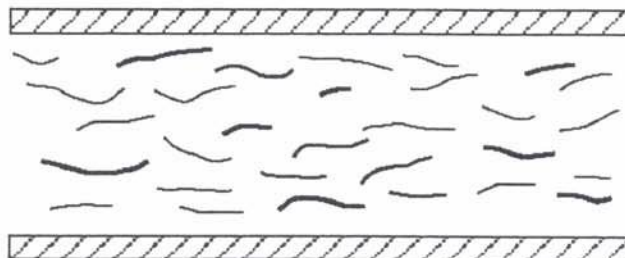


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Flow regimes

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- **Turbulent Flow:**
 - In turbulent flow there is an irregular random movement of fluid in a transverse direction to the main flow. This irregular, fluctuating motion can be regarded as superimposed on the mean motion of the fluid.



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Determination of the laminar/turbulent

- Reynolds showed that when circulating Newtonian fluids through pipes the onset of turbulence was dependant on the following variables:

- Pipe diameter, d ; in
- Density of fluid, ρ ; lbm/gal
- Viscosity of fluid, μ ; cp.
- Average flow velocity, v ; ft/s

$$N_{Re} = \frac{928\rho v d}{\mu}$$

If $Re < 2000$

→ Flow is laminar

If $2000 < Re < 4000$

→ Transition from laminar to turbulent

If $Re > 4000$

→ Flow is turbulent

This is a typical flow inside the drillpipe and drillcollars.

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Rheology of drilling fluids

- Rheology** is derived from the Greek words **rheo**, meaning flow and **logi**, meaning science.

the science of the deformation and/or flow of solids, liquids and gases under applied stress.

تعریف: - دانش بررسی رفتار جامدات، مایعات و گازها وقتی که یک stress بر آن اعمال شود

Relationship between Shear Stress vs. Shear Rate?

- ability to provide accurate predictions of the behaviour of real systems?? Using polymer and invert oil emulsion muds today

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Application of rheological concepts

In the drilling situation the application of rheological concepts for drilling fluids are primarily directed towards:

- a) Suspension → خواص کل چگونه تغییر میکند و چه وضعیتی برای بریدگی cutting
- b) Hydraulic calculations → انتقال می افتد وقتی که میسماها خراب می شود
- c) Hole cleaning and hole erosion → خواص چاه را بهتر کنیم ولی نه به قیمت از دست دادن دیواره چاه و خوردگی و ریزش دیواره چاه
- d) Filtrate migration
- e) Solids Control → در pay zone باعث formation damage می شود و در خارج از pay zone باعث افزایش ضریب نفوذناپذیری می شود و باعث stuck pipe می شود

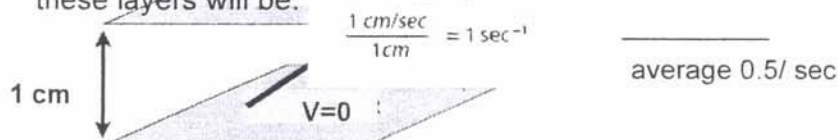
Shear rate

In a moving fluid shear rate can be defined as the rate at which one layer of fluid is moving by another layer divided by the distance between the layers.

$$\dot{\gamma} = \frac{v}{L} = \frac{dv}{dL}$$

It is the velocity gradient i.e. the ratio of velocity to distance between layers.

If a moving layer of fluid has a velocity 1cm/sec relative to a static layer at separation distance of 1cm then the shear rate between these layers will be:

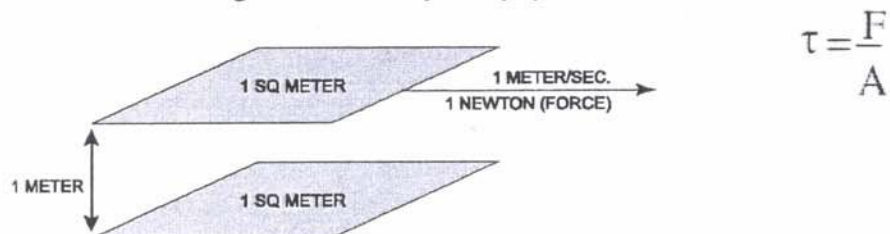


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Shear stress

- Shear Stress is defined as the force required to move a given area of the fluid. In a drilling fluid circulating system this is analogous to the **pump pressure**.



- Units: Newtons/ m² (# Pascal); dynes/cm²; lb_f/in²

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viscosity

Viscosity can be described as the resistance to flow and is defined as the ratio of shear stress to shear rate

$$\text{Viscosity} = \frac{\text{shear stress.dynes/cm}^2}{\text{shear rate sec}^{-1}} = \text{Poise}$$

$$\frac{F}{A} = \mu \frac{V}{L}$$

The higher the viscosity the higher the force required to move the upper plate relative to the lower plate.

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Rheological models

- A mathematical description of the viscous forces present in a fluid is required for the development of equations which describe the pressure losses in the drillstring and annulus.
- These forces are represented by the rheological model of the fluid.

– Models:

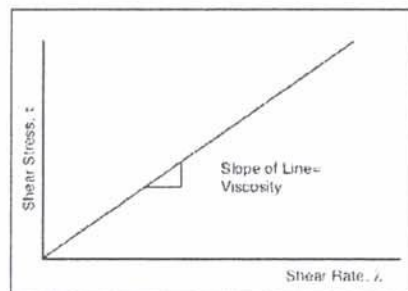
- **Newtonian model**
- **Non-Newtonian models: Bingham plastic; Power-law model.**

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Newtonian models

In these fluids the shear stress is directly proportional to the shear rate.



When the shear rate is doubled the shear stress is doubled i.e. when the circulation rate is doubled the pressure required to pump the fluid is doubled. (at Constant Press & Temp.; in Laminar flow)

Such fluids have a **constant viscosity**.

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Newtonian fluids

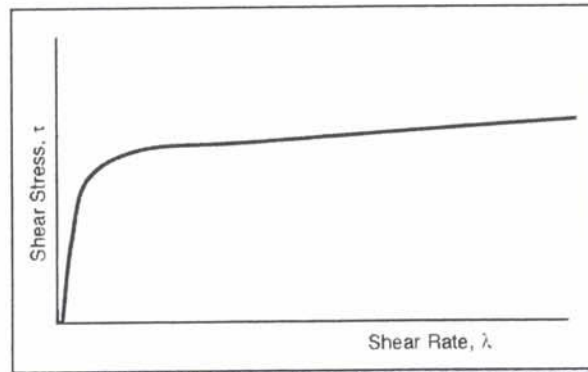
Common Newtonian fluids include:

- Water
- Diesel
- Glycerin
- Clear brines

Non-Newtonian models

- Fluids that do not obey Newton's viscous resistance law are Non-Newtonian
- Non-Newtonian fluids have viscosities that depend on measured shear rates for a given temperature and pressure
- The shear stress to shear rate relationship of these fluids is not linear and cannot therefore be characterised by a single value, such as the coefficient of viscosity
- ✓ Almost all drilling fluid viscosifiers provide rate dependent fluids. تقریباً همه سیالات حفاری «Non-Newtonian»

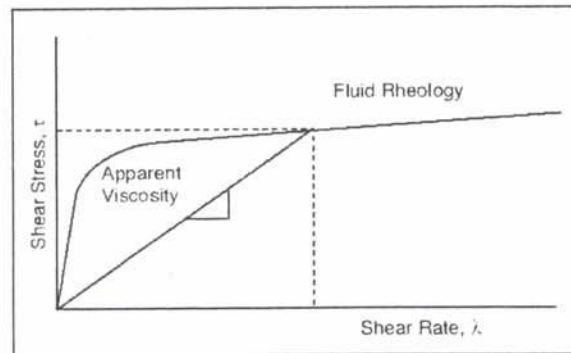
Non-Newtonian models



the shear stress of a non-Newtonian fluid is not directly proportional to shear rate and this is why their relationship cannot be described by a single parameter

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Apparent viscosity



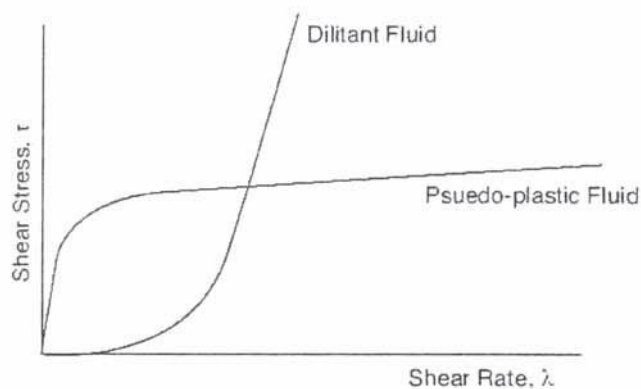
Definition:

the shear stress to shear rate relationship measured at a given shear rate

The apparent viscosity is the slope of the line between the origin and the shear stress and shear rate intercept at any given shear rate.

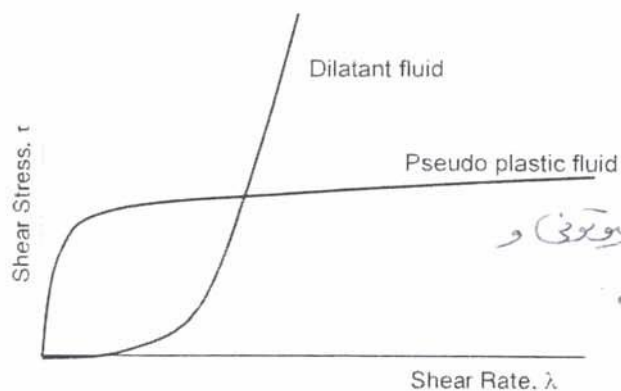
30

Non-Newtonian fluids



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Non-Newtonian fluids



بیشتر سیالات خماری، غیر نیوتونی و
از نوع شبه پلاستیک است.

Non-Newtonian fluids which are shear-rate dependent are called **pseudoplastic** if the apparent viscosity decreases with increasing shear rate.

dilatant if the apparent viscosity increases with increasing shear rate
(suspension of starch or mica in water)

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Rehological models

Non-Newtonian:

- Bingham Plastic
- Power Law

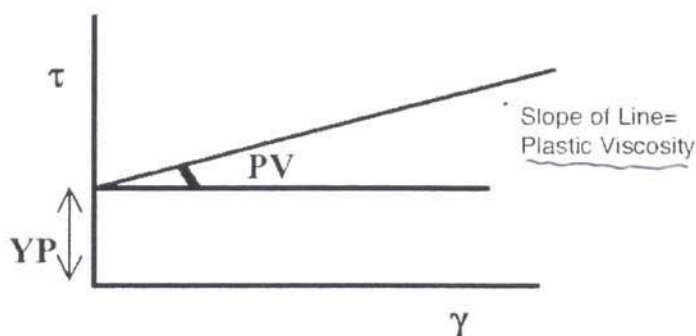
These models are used to approximate the **pseudoplastic behaviour** of drilling fluids and cement slurries.

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Bingham Plastic

- Models which behave according to the Bingham plastic model will not flow until the applied shear stress, exceeds a certain minimum shear stress value known as the yield point, γ



after the yield point has been exceeded, changes in shear stress are directly proportional to changes in shear rate,

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Y_p vs. gel strength

Y_p: مقاومت در مقابل جریان در shear rate های پایینی

- The Y_p defined in the Bingham model is in fact an extrapolation of the linear relationship between stress and shear rate at medium to high shear rates and as such describes **the dynamic yield** of the fluid. (Y_p is time independent)

وقتی گل به یک دوام خاصی برسد به حالت suspend شدن
cutting های سود

- The gel strength represents the shear stress to shear rate behaviour of the fluid at near zero shearing conditions (time dependent) → به زمان وابسته است.

Bingham Plastic

$$\tau = YP + PV \times (\gamma)$$

where

τ = measured shear stress in lb/100 ft²

YP = yield point in lb/100 ft²

PV = plastic viscosity in cP

γ = shear rate in sec⁻¹

$$\mu_a = 300 \frac{cP}{N}$$

$$\mu_p = PV = 0600 - 0300$$

$$\tau_y = YP = 0300 - PV$$

$$YP = (2 \times 0300) - 0600$$

Power law

- The Power Law model assumes that all fluids are pseudoplastic in nature and are defined by the following equation:

$$\tau = K (\gamma)^n$$

where

τ = Shear stress (dynes / cm²)

$$n = 3.32 \log \left(\frac{\theta_{600}}{\theta_{300}} \right)$$

K = Consistency Index

γ = Shear rate (sec-1)

$$K = \frac{\theta_{300}}{(511)^n}$$

n = Power Law Index

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نشان دهنده تغییرات چسبندگی
در طول محدوده برش می باشد

Power law

$$\tau = K (\gamma)^n$$

n: Power Law Index: indicates the degree of non-Newtonian behaviour over a given shear rate range. → *نشان دهنده این از انحراف از غیر نیوتونی شدن سیال است*

$n = 1 \rightarrow$

Newtonian

$n < 1 \rightarrow$

Non-Newtonian: Pseudo plastic fluid :the viscosity will decrease with an increase in shear rate

$n > 1 \rightarrow$

Dilatant Fluid

K: Consistency Index:

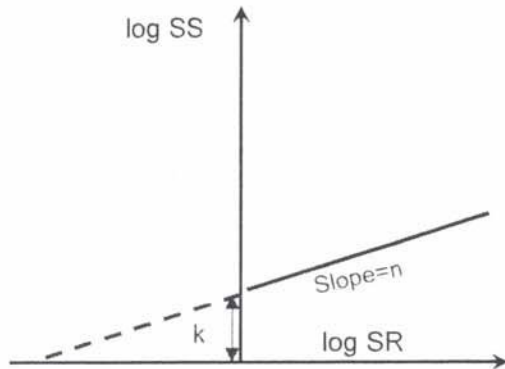
- is defined as the shear stress at a shear rate of one reciprocal second

- increase in the value of 'K' → increase in the overall hole cleaning effectiveness of the fluid.

- $K \rightarrow$ lbs/100ft², dynes-sec or N/cm².

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Power law



$$SS = k(SR)^n$$

$$\log SS = \log k + n \log SR$$

For two values of SR (ω_1, ω_2 in rpm), and two values of SS θ_1, θ_2 :

$$\log \theta_1 = \log k + \log \omega_1$$

$$\log \theta_2 = \log k + \log \omega_2$$

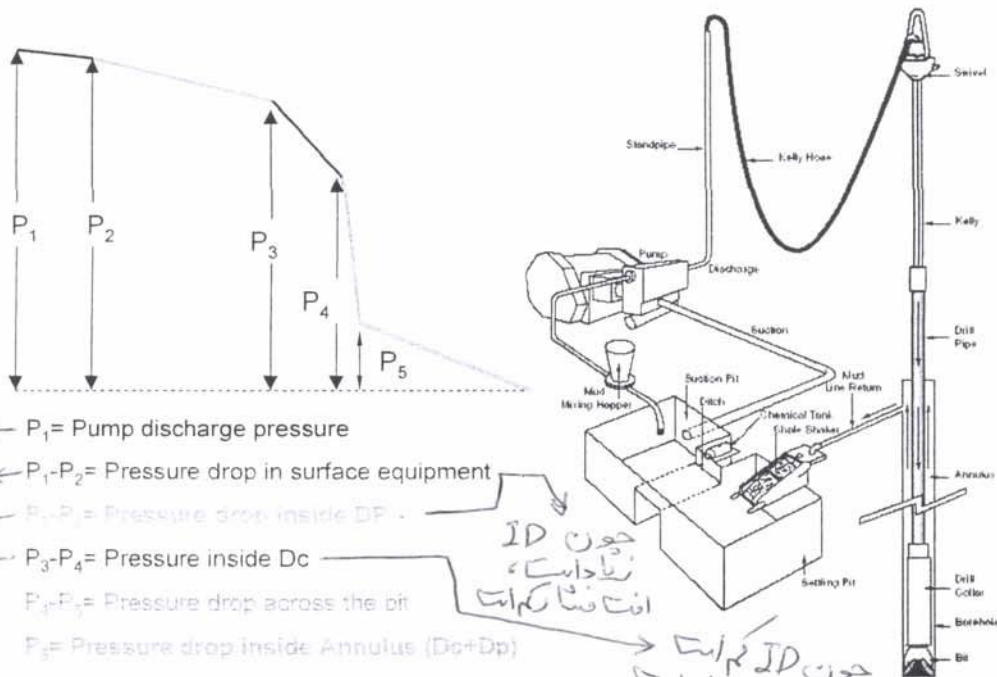
$$n = \frac{\log \frac{\theta_1}{\theta_2}}{\log \frac{\omega_1}{\omega_2}} \quad k = \frac{\theta_1}{\omega_1^n} = \frac{\theta_2}{\omega_2^n}$$

shear rate و rpm
مقتضی می توان اندازه گرفت
معمولاً لازم نیست که در 300 و 600
حساب کنیم

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قدرت افت فشار در مدل بینگهام بیشتر از مقدار واقعی است.
power law کمتر از مقدار واقعی است.
Power law ← مدل بینگهام
بکتر است.

Pressure loss



طابق از مدل
Bingham
صرف نظری کنیم

افت فشار کل سیستم
فشار خروجی از بئری
Drill pipe =
Drill collar =

P_1 = Pump discharge pressure
 $P_1 - P_2$ = Pressure drop in surface equipment
 $P_2 - P_3$ = Pressure drop inside DP
 $P_3 - P_4$ = Pressure inside Dc
 $P_4 - P_5$ = Pressure drop across the bit
 P_5 = Pressure drop inside Annulus (Dc + Dp)

چون ID زیاد است
افت فشار کم است
چون ID کم است
افت فشار زیاد است
تurbulancy
زیاد است و

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Pressure loss calculation matrix

ماتریکس محاسبه ضایعات در جدول را تکمیل کنید

Non-Newtonian

Fluid Type	Laminar Flow		Turbulent Flow	
	Pipe	Annulus	Pipe	Annulus
Newtonian	?	?	?	?
Bingham Plastic	?	?	?	?
Power law	?	?	?	?

Which Equation?

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بعد از این سرعت وارد جریان ملاطم می شود

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Critical velocity inside Dp, Dc

$$V_c = 1.08 \frac{P_v + \sqrt{p_v^2 + 12.34 d^2 (Mw)(Y_p)}}{d(Mw)}$$

V_c = critical velocity, $\frac{ft}{sec}$

P_v = pastic viscosity, cp

Y_p = yield point, lb_f/100 ft²

Mw = mud weight PPG

d = ID of pipe, in

$$V = 0.4085 \frac{\overbrace{q}^{Pump\ output\ (GPM)}}{d^2}$$

V = fluid velocity inside D_p , D_c , ft/sec

$V < V_c$: Laminar flow ✓

$V > V_c$: Turbulent flow ✓

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ΔΛ

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Critical velocity inside annulus

$$V_c = 1.08 \frac{P_v + \sqrt{p_v^2 + 9.256(D-d)^2(M_w)(Y_p)}}{(D-d)(M_w)}$$

V_c = critical velocity inside annulus, $\frac{ft}{sec}$

P_v = plastic viscosity, cp

Y_p = yield point, lb_f/100 ft²

M_w = mud weight PPG

d = OD of pipe, in

$$V = 0.4085 \frac{Q}{D^2 - d^2}$$

$\frac{ft}{sec}$

$V < V_c$: Laminar flow ✓

$V > V_c$: Turbulent flow ✓

$\frac{ft}{sec}$ ← V = fluid velocity inside annulus, ft/sec

D = hole size, in
(bit diameter)

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Laminar flow

R_e ?

Is R_e Constant?

Assumptions for ΔP calculations:

- The drillstring is placed concentrically in the casing or open hole
- The drillstring is not being rotated → فرض چپای چوبی نیست
- Sections of open hole are circular in shape and of known diameter
- The drilling fluid is incompressible
- The flow is isothermal

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این روابط در امتحان داده می شود و احتیاج به حفظ کردن نیست.
(در امتحان جواب نهایی را خود می کشد اگر غلط بود سوال غلط است.)
جواب

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Laminar flow

	In Pipes	In Annulus
Newtonian	$\frac{dP}{dL} = \frac{\mu \bar{v}}{1,500d^2}$	$\frac{dP}{dL} = 1500 \left[\frac{\mu \bar{v}}{d_2^2 + d_1^2 - \frac{d_2^2 - d_1^2}{\ln \frac{d_2}{d_1}}} \right]$
Bingham plastics	$\frac{dP}{dL} = \frac{\mu_p \bar{v}}{1,500d^2} + \frac{\tau_y}{225d}$	$\frac{dP}{dL} = \frac{\mu_p \bar{v}}{1000(d_2 - d_1)^2} + \frac{\tau_y}{200(d_2 - d_1)}$
Power law	$\frac{dP}{dL} = \frac{k \bar{v}}{144,000d^{(1+n)}} \left(\frac{3+1/n}{0.0416} \right)^n$	$\frac{dP}{dL} = \frac{k \bar{v}}{144,000d(d_2 - d_1)^{(1+n)}} \left(\frac{2+1/n}{0.0208} \right)^n$

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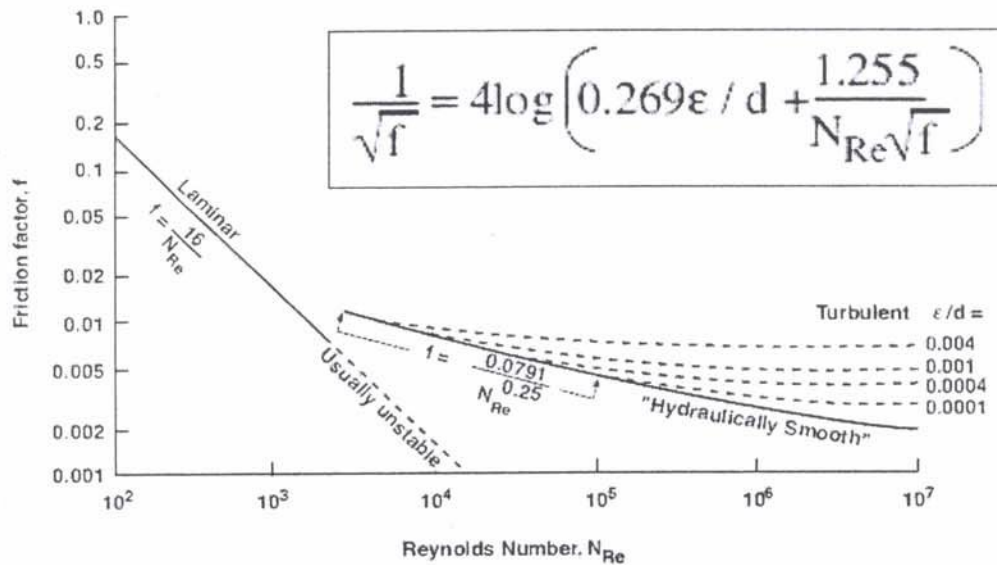
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Turbulent flow:

	In Pipes	In Annulus
Newtonian	$\Delta p = \frac{4 f L v^2 (Mw)}{2d}$	$\Delta p = \frac{4 f L v^2 (Mw)}{2(D - d)}$
Bingham plastics	$\Delta p = \frac{f L v^2 (Mw)}{25.8d}$	$\Delta p = \frac{f L v^2 (Mw)}{25.8(D - d)}$

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Stanton chart; fanning friction factor



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Pressure drop: power law

1. Determine n and K from:

$$n = 3.322 \log \left(\frac{\theta_{600}}{\theta_{300}} \right)$$

or

$$n = \frac{\log \left(\frac{\theta_{N_2}}{\theta_{N_1}} \right)}{\log \left(\frac{N_2}{N_1} \right)}$$

$$K = \frac{510 \theta_{300}}{(511)^n}$$

or

$$K = \frac{510 \theta_N}{(1.703 N)^n}$$

2. Calculate the annular velocity in FPM in annulus

$$v = \frac{24.51 \times \overset{\text{pump output}}{PO(GPM)}}{D^2 - d^2} \quad \frac{ft}{min}$$

3. Calculate SR in rpm for each velocity

$$SR(rpm) = \frac{1.41v(fpm)}{D - d}$$

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Pressure drop: power law

4. Calculate the dial reading for each SR:

$$\theta = k(SR)^n$$

5. Determine the flow regime from R_e :

$$R_e = \frac{v^2 \times Mw}{13.757 \times \theta}$$

6. Calculate Δp for each segment

$\Delta p = \frac{3.75}{1000} \frac{L\theta}{D-d}$ ← If $R_e < 2000$; laminar flow

↙ If $R_e > 2000$; turbulent flow

$\Delta p = 1.4327 \times 10^{-7} \frac{L v^2 Mw}{D-d}$

$$\frac{dp_f}{dL} = \frac{Kv^n \left(\frac{3+1/n}{0.0416} \right)^n}{144,000 (d_2 - d_1)^{1+n}}$$

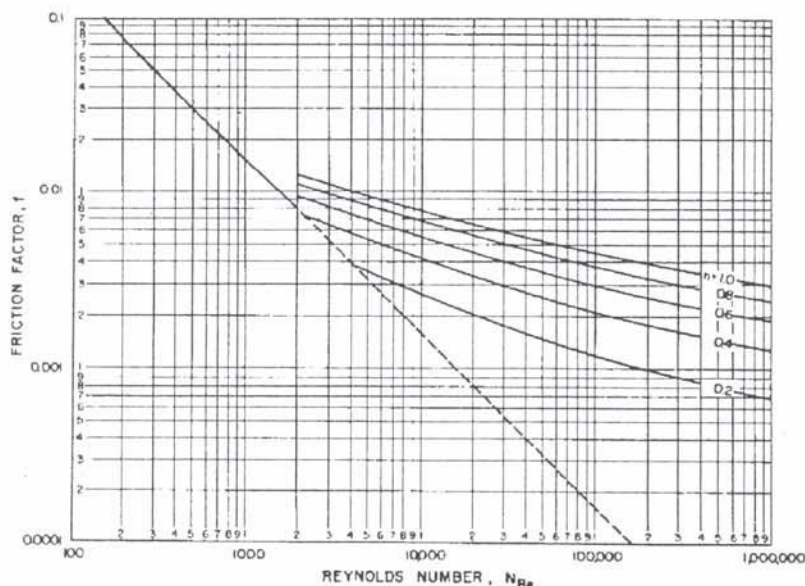
$$\frac{dp_f}{dL} = \frac{f_p v^2}{21.1 (d_2 - d_1)}$$

$$\frac{dp_f}{dL} = \frac{Kv^n \left(\frac{2+1/n}{0.0208} \right)^n}{144,000 (d_2 - d_1)^{1+n}}$$

$$\frac{dp_f}{dL} = \frac{f_p v^2}{25.8 d}$$

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Pressure drop: power law



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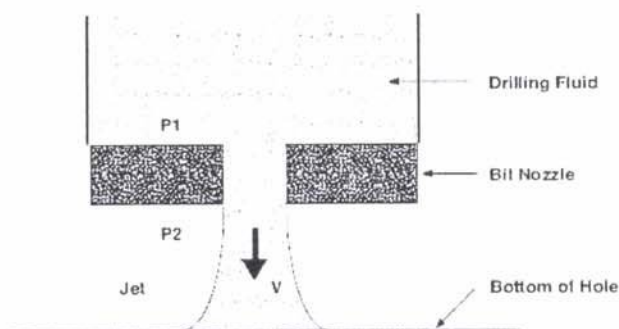
Summary

TABLE 4.6—SUMMARY OF FRICTIONAL PRESSURE LOSS EQUATIONS*

	Newtonian Model	Bingham Plastic Model	Power-Law Model
Mean Velocity, v	Pipe $v = \frac{Q}{2.448 d^2}$ Annulus $v = \frac{Q}{2.448 (d_2^2 - d_1^2)}$	Pipe $v = \frac{Q}{2.448 d^2}$ Annulus $v = \frac{Q}{2.448 (d_2^2 - d_1^2)}$	Pipe $v = \frac{Q}{2.448 d^2}$ Annulus $v = \frac{Q}{2.448 (d_2^2 - d_1^2)}$
Flow Behavior Parameters	$n = 1$	$n = 1$	$n = 0.7$ $K = 510 \frac{\text{lb}_m}{\text{ft}^2 \cdot \text{s}}$
Laminar Flow Frictional Pressure Loss	Pipe $\frac{dp_f}{dL} = \frac{16 \mu v}{d^2}$ Annulus $\frac{dp_f}{dL} = \frac{16 \mu v}{(d_2^2 - d_1^2)}$	Pipe $\frac{dp_f}{dL} = \frac{16 \mu v}{d^2}$ Annulus $\frac{dp_f}{dL} = \frac{16 \mu v}{(d_2^2 - d_1^2)}$	Pipe $\frac{dp_f}{dL} = \frac{16 \mu v}{d^2}$ Annulus $\frac{dp_f}{dL} = \frac{16 \mu v}{(d_2^2 - d_1^2)}$
Turbulent Flow Frictional Pressure Loss	Pipe $\frac{dp_f}{dL} = \frac{f v^2}{25.8 d}$ Annulus $\frac{dp_f}{dL} = \frac{f v^2}{25.8 (d_2^2 - d_1^2)}$	Pipe $\frac{dp_f}{dL} = \frac{f v^2}{25.8 d}$ Annulus $\frac{dp_f}{dL} = \frac{f v^2}{25.8 (d_2^2 - d_1^2)}$	Pipe $\frac{dp_f}{dL} = \frac{f v^2}{25.8 d}$ Annulus $\frac{dp_f}{dL} = \frac{f v^2}{25.8 (d_2^2 - d_1^2)}$

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Pressure drop across the bit



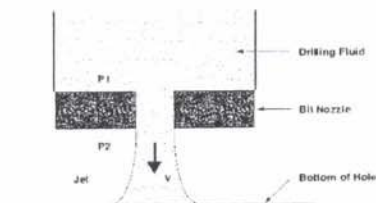
Assumptions:

1. the change in pressure due to a change in elevation is negligible.
2. the velocity v_0 upstream of the nozzle is negligible, compared with the nozzle velocity v_n
3. the frictional pressure loss across the nozzle is negligible.

افت فشار ناشی از friction صرفاً نظری کنیم

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Pressure drop across the bit



where,

ΔP_b = Pressure Loss across the nozzle (psi)

ρ = Density of the Fluid (ppg)

v_d = velocity of discharge (feet per second)

q = gpm

A_t = in²

$$v_n = \sqrt{\frac{\Delta p_b}{8.074 \times 10^{-4} \rho}} \quad (4.30)$$

$$\Delta p_b = \frac{8.311 \times 10^{-5} \rho q^2}{C_d^2 A_t^2}$$

jet velocity

$$v_n = C_d \sqrt{\frac{\Delta p_b}{8.074 \times 10^{-4} \rho}}$$

$C_d = 0.95$

The actual velocity is always smaller than the velocity computed using Eq. 4.30 primarily because the assumption of frictionless flow is not strictly true. To compensate for this difference, a correction factor or discharge coefficient C_d usually is introduced so that the modified equation,

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$$P_1 - 8.074 \times 10^{-4} \rho v_n^2 = P_2$$

Pressure drop across the bit

Example 4.13. A 12.0-lbm/gal drilling fluid is flowing through a bit containing three $1\frac{1}{32}$ -in. nozzles at a rate of 400 gal/min. Calculate the pressure drop across the bit.

Solution. The total area of the three nozzles is given by

$$\begin{aligned} A_t &= \frac{\pi}{4(32)^2} (13^2 + 13^2 + 13^2) \\ &= 7.67 \times 10^{-4} (169 + 169 + 169) \\ &= 0.3889 \text{ sq in.} \end{aligned}$$

Using Eq. 4.34, the pressure drop across the bit is given by

$$\begin{aligned} \Delta p_b &= \frac{8.311 \times 10^{-5} (12)(400)^2}{(0.95)^2 (0.3889)^2} \\ &= 1,169 \text{ psi.} \end{aligned}$$

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Nozzle size

NOZZLE SIZE	NOZZLE AREA (in. ²)	NOZZLE SIZE	NOZZLE AREA (in. ²)
18-18-18	0.75	14-13-13	0.41
18-19-17	0.72	13-13-13	0.39
18-17-17	0.69	13-13-12	0.37
17-17-17	0.67	13-12-12	0.35
17-17-16	0.64	12-12-12	0.33
17-16-16	0.61	12-12-11	0.31
16-16-16	0.59	12-11-11	0.30
16-16-15	0.57	11-11-11	0.28
16-15-15	0.54	11-11-10	0.26
15-15-15	0.52	11-10-10	0.25
15-15-14	0.50	10-10-10	0.23
15-14-14	0.47	10-10-9	0.22
14-14-14	0.45	10-9-9	0.20
14-14-13	0.43	9-9-9	0.19
14-13-13	0.41	9-9-8	0.17
		9-8-8	0.16

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یعنی سه jet در nozzle است که
 14 یعنی 14 in و 13 یعنی 13 in
 32 که مایل 32 صرف نظری کنیم.

✓ Pressure loss calculations

1. Calculate surface pressure losses → این مورد صورت گرفته شده و ما تا حالا افت فشار در bit و drill collar و drill pipe گفته ایم.
2. Decide on which model to use: Bingham Plastic or Power Law
3. Calculate pressure losses inside the Dps first then inside DCs as follows:
 - Calculate critical velocity of flow
 - Calculate actual average velocity of flow
 - Determine whether flow is laminar or turbulent by comparing average velocity with critical velocity. If average velocity is less than critical velocity the flow is laminar. If average velocity is greater than critical velocity the flow is turbulent.
 - Use appropriate equation to calculate pressure drop
4. Divide the annulus into an open and cased section

مانند annulus چندی section داریم
 که بیشتر این قسمت در بالای bit بوده که مربوط
 به drill collar است و ما باید سرعت جریان را برای هر section
 جداگانه محاسبه کرده و تسلط و آرام بودن را مشخص داده و
 محاسبات را انجام دهیم.

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Pressure loss calculations

5. Calculate annular flow around drillcollars (or BHA) as follows:

- Calculate critical velocity of annular flow
- Calculate actual average velocity of flow in the annulus
- Determine whether flow is laminar or turbulent by comparing average velocity
- with critical velocity. If average velocity is less than critical velocity the flow is laminar. If average velocity is greater than critical velocity the flow is turbulent.
- Use appropriate equation to calculate annular pressure drop

6. Repeat step 4 for flow around drillpipe in the open and cased hole sections.

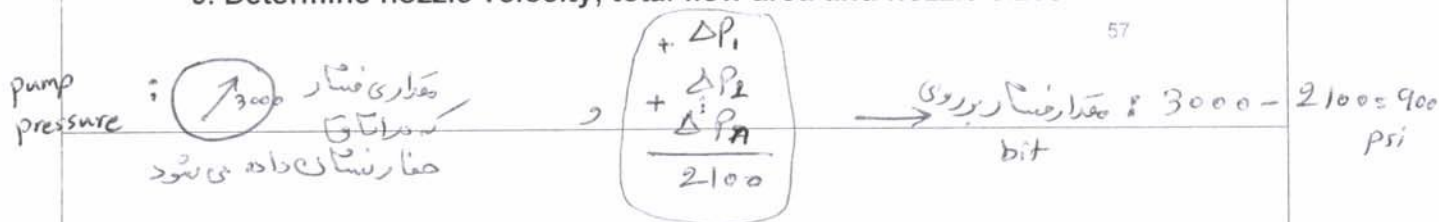
7. Add the values from step 1 to 5, call this system losses

8. Determine the pressure drop available for the bit

$$\Delta P_b = \text{pump pressure} - \Delta P_s$$

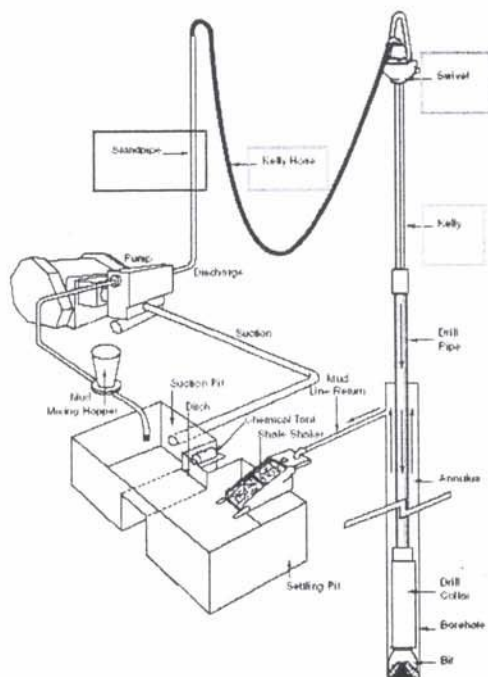
9. Determine nozzle velocity, total flow area and nozzle sizes

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Surface Equipments

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کاهش گpm در پیپ دریل سوراخ ایجاد شده و گpm کاهش
 در پیپ دریل stand pipe یافته یا در پیپ دریل سوراخ ایجاد شده و گpm کاهش
 پیدا کرده است.

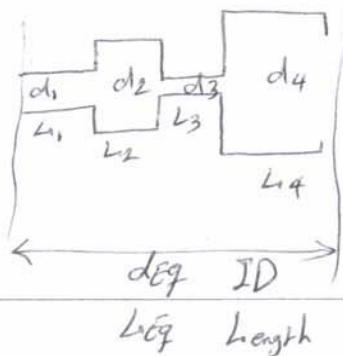
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Surface equipments- method 1

دکل های متصل به یکدیگر است ← مابقی محاسب افت فشار در سطح باید در stand pipe، Kelly have

Surface Connections	No.1		No.2		No.3		No.4	
	ID (In)	Length (ft)	ID (In)	Length (ft)	ID (In)	Length (ft)	ID (In)	Length (ft)
Stand Pipe	3	40	3 1/2	40	4	45	4	45
Drilling Hose	2	45	2 1/2	55	3	55	3	55
Swivel(washpipe & Gooseneck)	2	4	2 1/2	5	2 1/2	5	3	6
Kelly	2 1/4	40	3 1/4	40	3 1/4	40	4	40
DP								
OD (in)		Equivalent Length for Surface connections (ft of DP)						
3 1/2		13.3	437		161			
4 1/2		16.6			761		479	
5		19.5					816	
							340	
							579	



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Surface equipments- method 2

دکل های متصل در سطح محاسبی

Surface Connections	Combinations							
	No.1		No.2		No.3		No.4	
	ID (In)	Length (ft)	ID (In)	Length (ft)	ID (In)	Length (ft)	ID (In)	Length (ft)
Stand Pipe	3	40	3 1/2	40	4	45	4	45
Drilling Hose	2	45	2 1/2	55	3	55	3	55
Swivel(washpipe & Gooseneck)	2	4	2 1/2	5	2 1/2	5	3	6
Kelly	2 1/4	40	3 1/4	40	3 1/4	40	4	40
Equivalent Length 3.826 in ID	2600		946		610		424	
Value of E	2.5 x 10-4		9.6 x 10-5		5.3 x 10-5		4.2 x 10-5	

$$\checkmark P_i = E \times \rho^{0.8} \times Q^{1.8} \times PV^{0.2} \text{ psi}$$

where

ρ = mud weight (lbm/gal)

Q = volume rate (gpm)

E = a constant depending on type of surface equipment used

PV = plastic viscosity (cP)

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Example 1 نمونه سوال امتحانی

فرض کردیم Bingham

- Depth : 10,000'
- Bit size: 9 7/8"
- Dps: 9600', 5" OD, 4.276" ID, 19.5#/ft
- Dcs: 400', 7 3/4" OD, 3 1/2" ID,
- Av= 135 FPM
- Mw= 12 ppg
- Pv=43 cps
- Yp= 20 lb_f/100 ft²
- Bit nozzles: 3 × 12 → $\frac{12}{32} = \frac{3}{8}$
- Surface Connections: Type 4
- Calculate:
 - ① • Pressure drop in different segments (surface connections, Inside DP, Inside DC, in bit, in annulus) → lb_m
 - ② • Jet velocity in FPS → $\frac{\text{ft}}{\text{s}}$
 - ③ • BHCP, ECD
 - ④ • Discharge Pressure → ΔP_{total}
 - ⑤ • Pump Hydraulic power

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Homework

- Chapter 4: 4, 7, 24, 25, 26, 28, 31, 21, 20, 19, 17, 36, 35, 37, 39
- Chapter 6: 20 (b, c, d, g), 2, 3, 4, 5, ⑥, 7, 8, 9, 31

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sol of Example 1:

$$V_c = 1.08 \frac{PV + \sqrt{PV^2 + 12.34 d^2 (MW)(PV)}}{MW(d)} = 5.87 \frac{ft}{s} \quad (D/p)$$

$$V_c = 6.34 \frac{ft}{s} \quad (FPS)$$

$$V_c = \frac{1.08 PV + \sqrt{PV^2 + 9.256 (D-d)^2 (MW)(Y_p)}}{MW(D-d)}$$

$$D/C \text{ در اطراف } V_c = 6.42 \text{ FPS}$$

$$D/p \text{ در اطراف } V_c = 5.10 \text{ FPS}$$

$$AV = \frac{24.51 \text{ pump output (gpm)}}{\frac{D^2 - d^2}{4}} \rightarrow 135 = \frac{24.51 \times Q}{(9.75^2 - 5^2)} \rightarrow Q = 400 \text{ gpm}$$

slide 12 $\frac{D^2 - d^2}{4}$ hole diameter or bit size

$$V = 0.4085 \frac{Q}{d^2} \quad V = 0.4085 \frac{400}{(4.276)^2} = 8.93 \text{ FPS}$$

$$V = 0.4085 \frac{400}{3.34^2} = 18.15 \text{ FPS}$$

$$V = 0.4085 \frac{Q}{D^2 - d^2} \rightarrow \left\{ \begin{array}{l} D/p \text{ در داخل } V = 2.25 \text{ FPS} \\ D/C \text{ در داخل } V = 4.36 \text{ FPS} \end{array} \right.$$

(بنا بر این معیار با یکدیگر)

inside drill pipe	Turbulent
inside drill collar	Turbulent
Annulus drill collar	laminar
Annulus drill pipe	laminar

① surface connection ΔP ?

- pressure drop inside D/p :

$$Re = 928 \frac{MW \times V \times d}{PV} = 928 \frac{12 \times 8.93 \times 4.276}{43} = 9889$$

$$\Delta P = \frac{f \cdot L \cdot V^2 \cdot MW}{25.8 \times d} = \frac{0.0077 \times 9600 \times (8.93)^2 \times 2}{25.8 \times 4.276} = 641.2 \text{ psi}$$

$f = 0.0077$ friction factor

$$\left. \begin{array}{l} \text{From previous table} \\ 9600 \text{ ft} \\ 579 \text{ ft} \end{array} \right\} \rightarrow \Delta P @ \text{ surface connection} = 38.7 \text{ psi}$$

$$\Delta P \text{ inside } D_c = ? \rightarrow Re = 928 \frac{12 \times 18.15 \times 3}{43} = 14101 \rightarrow f = 0.0072$$

$$\Delta P = \frac{f \cdot L \cdot V^2 \cdot MW}{25.8 \times d} = \frac{0.0072 \times 400 \times (18.15)^2 \times 2}{25.8 \times 3} = 147.1 \text{ psi}$$

$$\Delta P @ \text{ Bit} : \Delta P = \frac{MW \times Q^2}{6698.3 n^2 d^2} \quad \text{that: } n: \text{ Nozzle size } d: \text{ Nozzle size}$$

$$= \frac{12 \times 400^2}{6698.3 \times (3)^2 \times (\frac{3}{8})^2} = 1610 \text{ psi}$$

بنابراین: معادلات فوق را در مورد هر یک از مقاطع در نظر بگیرید. ابتدا افت فشار را در هر یک از مقاطع حساب کنید، که ابتدا افت فشار را در هر یک از مقاطع حساب کنید. 3000 psi

① $\Delta P @ \text{ Annulus (P)}$

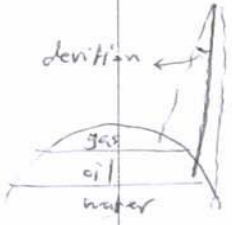
$$= \frac{L \cdot V \cdot PV}{1000(D-d)^2} + \frac{L \cdot YP}{200(D-d)} = \frac{400 \times (4.36) \times 43}{1000(9.75 - 7.375)^2} + \frac{400 \times 20}{200(9.75 - 7.375)} = 16.6 + 18.8 = 35.4 \text{ psi}$$

hole size $d = 7.375$

Flow rate
WOB → بار متوسطی که
RPM → سرعت چغاری (برای تقسیم سرعت چغاری)

Rate of penetration

- Drilling Knowledge and experience of the drilling crew → دانشی افراد و تجربه
- Efficiency of the drilling rigs (mud pump pressure & flow rate limits), depth
- Strength and specification of formation → مقاومت سنگ را بدانیم
 - Rock strength and compaction
 - Porosity, permeability and formation fluid types
 - Pore pressure → جابجایی که pore pressure بیشتر است ← مقدار porosity زیاد است
- Mud Properties
 - Mud weight → صاف میزان mud weight بیشتر شود، سرعت چغاری کم می شود
 - Solid percent → درصد وزن گل بیشتر شود ← مقدار solid و viscosity بیشتر است
 - Viscosity, etc → مقدار GPM یا flow rate زیاد شده ← سرعت چغاری کم می شود
- Mechanical Parameters
 - Bit type
 - Weight on bit
 - RPM
- Hydraulic power of the system
 - Annular velocity → میزان از Min Annular velocity داریم که بتوان چاه را تمیز کرد
 - Jet velocity



میزان افت فشاری که در مته خواهیم داشت.
انحراف از مسیر مستقیم باعث ایجاد horizontal displace می شود. باعث تغییر در برنامه برداشت می شود و اثر منفی دارد.
خواسته شد برداشت کنیم - Cas cap یا water aquifer برخورد کنیم: ← مایک Max. HP را در برنامه ریزی می بینیم چغاری داریم.

Mechanical parameters: WOB

اگر WOB زیاد بریم باعث wear می شود. با افزایش WOB → ROP افزایش می یابد تا جایی که بعد از آن مشکل hole cleaning پیدا می کند و ROP شروع به کاهش می کند.

Soft Formation
Hard Formation
* Poor cleaning

WOB WOB برای افزایش باید لوله های وزن بیشتری شده و اضافه ساز را زیاد می شود.

WOB نیاز داریم تا چغاری و سرعت آن بعد از این حداقل به صورت خطی افزایش یابد و با توجه به مشکل hole cleaning بعد از حدی افزایش نخواهیم داشت.

① differential sticking
② cementing در مته می شود.

spiral
دو مشکل خواهیم دید و به صورت محسوس چغاری نشود.

twist off
بستگی زیاد به وزن و طول دارد. اگر چاه را به صورت spiral چغاری کنیم دو مشکل خواهیم دید و به صورت محسوس چغاری نشود.

Risk of hole deviation → عریضی WOB بیشتر شود.
-Bit balling → احتمال انقباض چاه بیشتر شود.
-Bit wear → افزایش WOB باعث فرسایش بیشتر می شود.
-longer BHA: increase in round trips → مته در سازه اندیشه و باعث خوردگی می شود.
-Torque → افزایش WOB باعث خوردگی می شود.
-Drilling cost!!

پکته شده برای زمانی که بیش تر از حد باشد stabilizer داشته باشیم ← packed hole Assembly
استفاده می کنیم.

① continue sol of previous example :

$$\Delta P|_{\text{Annulus}} = \frac{9600 (2.25) (43)}{1000 (9.75 - 5)^2} + \frac{9600 \times 20}{200 (9.75 - 5)^2} = 39 + 197 = 236 \text{ psi}$$

$$\rightarrow \Delta P @ \text{ Annulus total } = 35.4 + 236 = 271.4 \text{ psi}$$

② سرعت خروجی از نازل های : $0.4085 \frac{Q}{nd^2} = 0.4085 \frac{400}{3(0.375)^2} = 387.3 \text{ Fps}$

③ BHCP + ECD = ?

BHCP = hydrostatic Head pressure + ΔP in Annu .
 → Bottom hole circulate pressure HP

$$HP = 0.052 \times MW \times TD (ft) = 0.052 \times 12 \times 10,000 = 6240 \text{ psi}$$

$$BHCP = 6240 \text{ psi} + 271.4 \text{ psi} = 6511.4 \text{ psi}$$

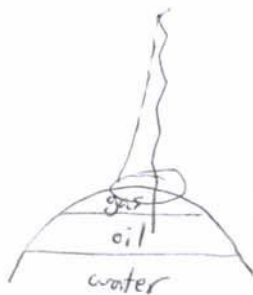
$$ECD = 19.25 \frac{BHCP}{TD} = 19.25 \frac{6511.4}{10,000} = 12.53 \text{ PPG}$$

equivalent
circulate
density

$$\Sigma \Delta P = \Delta P|_{\text{surface}} + \Delta P|_{\text{inside DP}} + \Delta P|_{\text{inside DC}} + \Delta P|_{\text{Bit}} + \Delta P|_{\text{Ann DC}} + \Delta P|_{\text{Ann DP}}$$

$$= 2708 \text{ psi} \rightarrow \text{Discharge pressure}$$

⑤ Hydraulic horse power = $\frac{Q \times P}{1714} = \frac{400 \times 2708}{1714} = 632 \text{ hp}$



ای data را داریم

depth	Angle
200	0
500	0.5
1000	1
1500	2
2000	3

در چاه های گازی مقدار deviation اهمیت دارد.

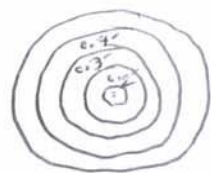
در چاه های گازی باید چاه را plug pack کرد

و در چاه های نفتی حفاری کنیم (آفری حد)

✓ برای تعیین جهت انحراف برای چاه های گازی چاه های حفاری نمی شود

چاه های offshore قبل از راندن casing باید از نمودار CDR/GR استفاده کرد.

برای تعیین زاویه انحراف از یک دستگاه به نام single-shot استفاده می کنیم.



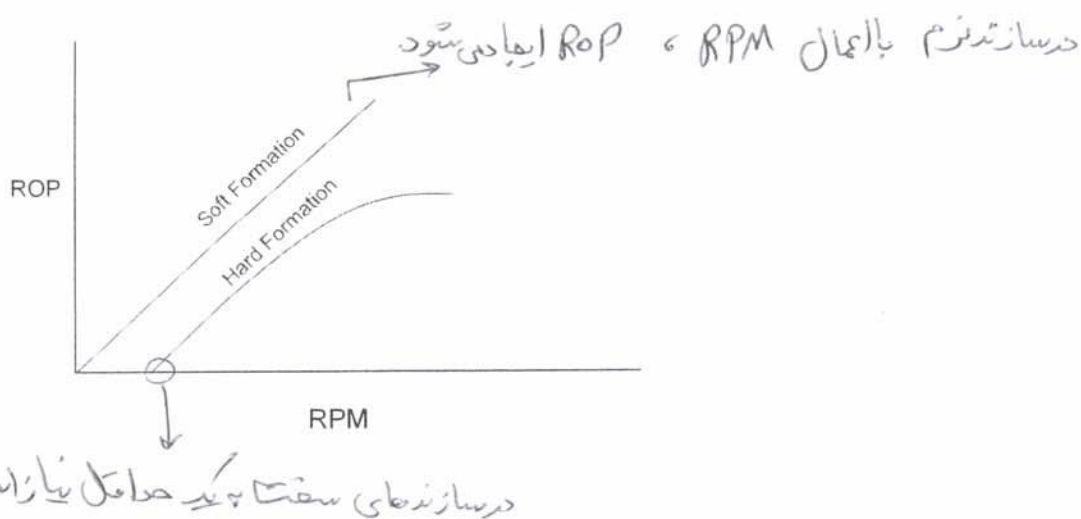
دست اندرایی سمور تعیین جهت حفاری می باشد؛ به کمک این دستگاه اطلاعاتی

فوران رخ داده و آستی سوزی رخ دهد؛ ما باید موقعیت حفاری چاه که به سبب رخ داده است

بدانیم تا relief well (چاه آستی سوزی) را به درستی حفاری کنیم.

برای تعیین جهت انحراف از یک دستگاه به نام Multi-shot استفاده می کنیم. (روشی دیگر)

Mechanical parameters: RPM



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ظرفیت حمل
حمل ها

Carrying capacity of mud

- fluid density → عریض سنگینی تر باشد، ظرفیت حمل زیاد است
- viscosity
- flow regime
- annulus size
- annular speed → از یک حداقل سرعت نمی توان پایین تر آمد.
- particle density → عریض میزان density ذره و کنده بیشتر شود
- particle shape → عریض درست تر باشد، بهتر بالایی آید
- pipe rotation → وقتی لوله های چرخد، ذرات اطراف لوله ها حفاری
- pipe eccentricity → به اطراف پرتاب شده و حیات کمتر می شود
- Hole angle

← نوع قرار گرفت لوله ها
در چاه در چاه های
deviation (جهت دار)
یک مقدار سرعت Min, Max
داریم و سرعت دلخواه
بکنواختی نخواهیم داشت.

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Hydraulic optimization

The two major aims of an optimum hydraulics program:

- To clean the hole effectively → تمیز کردن بهتر چاه
 - the hydraulics must be designed so that the annular velocity never falls below a pre-determined minimum for lifting cuttings.

تأثیر مایه بر حداقل سرعت دالیزی و gpm داشته باشیم.

- To make best use of power available to drill the hole.

- ensuring that the optimum pressure drop occurs across the bit.

با optimal از میزان افت فشار و میزان flow rate برنامه ریزی کنیم.

Since this pressure drop will depend on circulation rate some careful designing is required to satisfy both objectives.

توانی که داریم که حداقل کار را انجام دهد.

Hydraulic optimization

حوظ بگیرید مهم در Max کردن hydraulic داریم.

- Max HHP at the bit
- Max hydraulic impact at the bit (jet impact force)
- Combination of Max HHP & Max jet impact

$\left. \begin{array}{l} \text{Min gpm} = \checkmark \\ \text{power available} = \checkmark \\ \text{Max press} = \checkmark \\ \text{Max flow rate} = \checkmark \end{array} \right\} \begin{array}{l} \text{این چهار مورد} \\ \text{محقق است} \end{array} \rightarrow \begin{array}{l} \text{ما باید مقداری از هر کدام} \\ \text{بیدار کنیم که optimize} \\ \text{رایج است آوریم.} \end{array}$

Max HHP at the bit → حداکثر توان هیدرولیک در نوک

Assumes that the best method of cleaning the hole is to concentrate as much fluid energy as possible at the bit.

- زمانی بهترین روش تمیز کردن چاه این است که حداکثر انرژی مایع را در نوک چاه متمرکز کنیم.

- Speer (1958): The penetration rate would increase with hydraulic horse power until the cuttings were removed as fast as they were generated.

- After this perfect cleaning level was achieved, there should be no further increase in penetration with hydraulic.

➤ Due to the frictional loss in the drilling string and annulus, the horse power developed at the bottom of the hole is different from the hydraulic power developed by the pump.

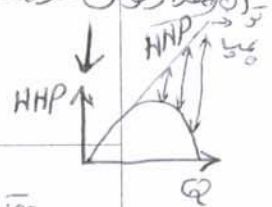
➤ (Bit HHP is not maximised by operating the pump at the max possible horsepower.)

$$HHP_t = HHP_s + HHP_{bit}$$

$$\frac{P_t \times Q}{1714} = \frac{P_s \times Q}{1714} + \frac{P_{bit} \times Q}{1714}$$

توان مایع در نوک چاه با توان هیدرولیک پمپ و در سیستم هیدرولیک چاه با توان هیدرولیک پمپ و توان هیدرولیک در نوک چاه (HHP_{bit}) تفاوت دارد. این مقدار هیدرولیک در نوک چاه با تغییر سرعت چاه (Q) تغییر می‌کند. سرعت حفاری زمانی افزایش می‌یابد که cutting زمانی که با سرعت کند شود با همان سرعت خارج شود. اگر بیشتر از آن شود، نیروی اضافی وارد می‌کنیم.

مثال: سرعت چاه 3 m/hr
Q₁ = 100 gpm → 5 m/hr
Q₂ = 200 gpm → 5 m/hr
Q₃ = 500 gpm → 5 m/hr



Max HHP at the bit

$$HHP_t = \text{input HP} \times E_m$$

E_m = mechanical efficiency

$$HHP_b = HHP_t - HHP_s \rightarrow \text{system (excluding the bit)}$$

HHP_t = total hydraulic horsepower available from the pump

HHP_s = hydraulic horsepower expended in the circulation system (excluding the bit)

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Maximum hydraulic horsepower

$$P_{\text{pump}} = P_{\text{bit}} + P_c$$

$$P_c = P_{\text{circulating}} = P_{\text{surface}} + P_{\text{DP}} + P_{\text{DC}} + P_{\text{AnnDC}} + P_{\text{AnnDP}}$$

$$P_c = kQ^n \quad n = 1.86 \text{ (empirically)}$$

اینجا k : depends on mud properties and wellbore geometry.
کده ای.

$$P_c = kQ^{1.86}$$

$$HHP_{\text{bit}} = HHP_p - HHP_c$$

$$\frac{P_{\text{bit}}Q}{1714} = \frac{P_pQ}{1714} - \frac{P_cQ}{1714} = \frac{P_pQ}{1714} - \frac{kQ^{2.86}}{1714}$$

$$\frac{dP_{\text{bit}}}{dQ} = 0$$

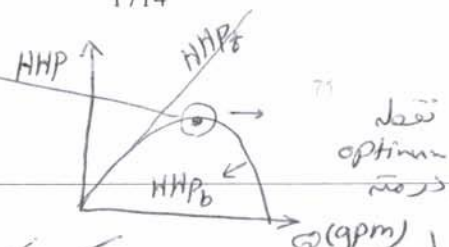
میزان حداکثر توان در bit
نسبت به flow rate است.

$$P_{\text{bit}} = 0.65P_p$$

$$HHP_{\text{bit}} = 0.65HHP_p$$

Continue

$$\begin{aligned} \frac{dP_{\text{bit}}}{dQ} &= \frac{P_p}{1714} - \frac{2.86kQ^{1.86}}{1714} \\ &= \frac{P_p}{1714} - \frac{2.86P_c}{1714} \\ &= \frac{P_p}{1714} - \frac{2.86}{1714}(P_p - P_{\text{bit}}) \\ &= \frac{P_p}{1714} - \frac{2.86P_p}{1714} + \frac{2.86P_{\text{bit}}}{1714} \\ &= P_p \left(\frac{1}{1714} - \frac{2.86}{1714} \right) + P_{\text{bit}} \left(\frac{2.86}{1714} \right) = 0 \\ P_{\text{bit}} &= \frac{P_p \left(\frac{1.86}{1714} \right)}{\frac{2.86}{1714}} = \frac{1.86}{2.86} P_p \end{aligned}$$



ex:

اگر بیش از این اعمال کنیم HHP کاهش می یابد.

Maximum hydraulic horsepower

حداکثر فشار ریمپ با آفونا بجا است.

$$P_c = 0.01Q^{1.86}$$

GPM	P_{pump}	P_c	P_{bit}	HHP_{bit}	HHP_{pump}
300	2800	405	2395	419	490
400	2800	691	2109	492	658
484	2800	980	1820	514	791
500	2800	1047	1753	511	817
600	2800	1470	1330	465	980
700	2800	1958	842	344	1143

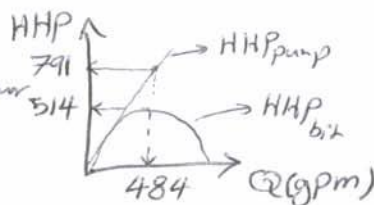
یعنی اگر افت فشار pump را
در صورت قرار دهیم optimum می شود
مقدار optimum درجه

$$P_{\text{bit}} = 0.65P_{\text{pump}}$$

$$P_c = 0.35 \times 2800 = 980 \text{ psi}$$

$$P_c = kQ^{1.86}$$

$$980 = 0.01 \times Q^{1.86} \rightarrow Q = 484 \text{ gpm}$$



Maximum hydraulic impact

Laboratory and field studies have shown that cross flow beneath the face of the bit is the most effective parameter in hole cleaning. Cross flow is maximum when impact force is maximum.

The Jet of fluid exert a force at the bottom of the hole called jet impact force. It is due to the change in the jet momentum as it hits the bottom.

This assumes that the most effective method is to maximise the force with which the fluid hits the bottom of the hole.

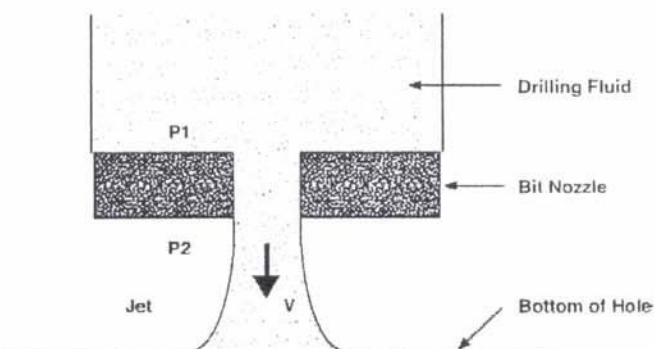
$$F_j = 0.01823 C_d q \sqrt{\rho \Delta p_b}$$

F_j = Jet impact lb

Mw = Mud weight, ppg

Q = flow rate, GPM

P_b : bit pressure drop, psi



or
$$F_j = \frac{Mw \times Q^2}{6040 \times A_n}$$

A: Nozzle Area, in²

Max hydraulic
پتانسیل
در این حالت
پتانسیل
در این حالت

✓ Now: Show that in Max Hydraulic impact theory the following relationships are applied.

Maximum hydraulic impact

Using calculus to determine the flow rate at which the bit impact force is a maximum gives

$$\frac{dF_j}{dq} = \{0.009115 C_d [2\rho \Delta p_p q - (m+2) \cdot \rho c q^{m+1}]\}$$

$$/[(\rho \Delta p_p q^2 - \rho c q^{m+2})^{0.5}] = 0.$$

Solving for the root of this equation yields

$$2\rho \Delta p_p q - (m+2) \rho c q^{m+1} = 0,$$

$$\rho q [2\Delta p_p - (m+2) \Delta p_d] = 0,$$

or

$$\Delta p_d = \frac{2\Delta p_p}{(m+2)} \quad (4.84)$$

$$P_c = 0.51 P_p$$

$$P_b = 0.49 P_p$$

$$\boxed{P_c = 0.51 P_p}$$

$$\boxed{P_b = 0.49 P_p}$$

این 0.51 را سیستم
و 0.49 را در
بیشترین
Max jet impact force داریم.

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(بالای روشی ex: قبلی)

Maximum hydraulic impact

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jet
Max impact force

$0.01 Q^{1.86}$

GPM	P _{pump}	P _c	P _{bit}	HHP _{bit}	HHP _{pump}	I _j	A _n (in ²)
300	2800	405	2395	419	490	895	0.2
400	2800	691	2109	492	658	1098	0.29
484	2800	980	1820	514	791	1246	0.37
500	2800	1047	1753	511	817	1247	0.4
593	2800	1428	1372	475	970	1315	0.53
600	2800	1470	1330	465	980	1302	0.55

روشن قبلی انتخاب شده

در این روشی انتخاب شده Max

$$P_c = 0.51 P_p = 0.51 \times 2800 = 1428 \text{ psi}$$

$$P_c = 0.01 Q^{1.86} \Rightarrow Q = 593 \text{ gpm}$$

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در HHP (نظریه اول) بهترین چون در نظریه اول تقریباً کمتری نیاز دارد و شرکت معمولاً نظریه اول را انتخاب می کند

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Comparison

- max. HHP, takes less power from pumps →
- While taking less power from pumps, it takes about 100 gpm less, so we would have less repairs
- In max HHP account for about 95% of Impact force

در HHP توان پمپ ها کمتر بوده و زور کمتری زمین به پمپ ها کمتر تقریباً نیاز دارد

95٪ را نسبت به impact force تأمین می کند

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V5

نظریه سوم

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Optimum flow rate

$$Q_{opt} = \left[\frac{F \cdot P_i}{k(F + N)} \right]^{1/N}$$

$$k = \frac{Mw}{z} \left[T(c) + 0.56 \sum \frac{L}{d^{4.86}} + \sum \frac{L}{(D_H - D_p)(D_H^2 - D_p^2)^{1.86}} \right]$$

جاری geometry بستنی

For Max. HHP $F=1$

For Max. Impact $F=2$

$N=1.86$

$$P_b = \frac{Mw \times Q^2}{10858 A_n^2}$$

$$P_c = k Q^{1.86}$$

$$v_j = \frac{0.32086 \times Q}{A_n}$$

$$I_j = 0.00516 \times Mw \times Q \times v_j$$

Q_{opt} : Optimum flow rate, GPM

P_i : Desired surface pump pressure, psi \rightarrow Max, Allowable

$Z=9090$

Surface pressure

$T=1.73$

C = Constant for surface Equipment

L = Length of DPs or Dc, ft

A_n = Area of Nozzle, in²

D = Inside diameter of DPs or DCs, in

D_H = Hole diameter, in

D_p = Outside diameter of DPs or DCs

v_j = Jet velocity, ft/sec

I_j = Jet impact, lb

Mw = Mud weight, ppg

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Example 2

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$Mw=71$ pcf= 9.5 ppg

$P_v=4$ cp \rightarrow قطر داخلی

$D_c: 11" \times 3"$, 28 m \rightarrow طول لوله

$9 \frac{1}{4}" \times 3"$, 55m \rightarrow قطر بیرونی

$8 \frac{1}{2}" \times 3"$, 27 m

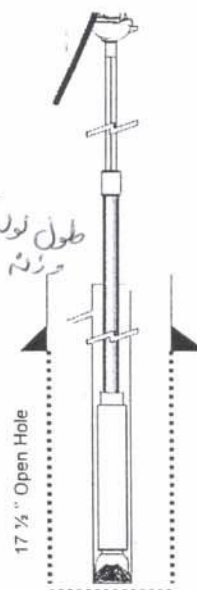
$D_p: 5" \times 4.276"$ \rightarrow قطر داخلی

Max. Allowable surface pressure: 2800 psi

Calculate the Optimum flow rate and Nozzle size using:

1) Max HHP

2) Impact force



1500 meter

meter drilling depth (BH)

متر عمق

Example 2

Max. HHP

در این مورد ۶۵٪ P_t را در نظر می‌گیریم
در نتیجه باید ما $Nozzle$ با قطر گندم در نظر بگیریم
تا P_t کمتر و HHP بیشتر داشته باشیم.

$$k = \frac{Mw}{z} \left[T(c) + 0.56 \sum \frac{L}{d^{4.86}} + \sum \frac{L}{(D_H - D_p)(D_H^2 - D_p^2)^{1.86}} \right] = 0.0037$$

$$Q_{opt} = \left[\frac{F \cdot P_t}{k(F + N)} \right]^{1/N} = \left[\frac{2800}{2.86 \times 0.0037} \right]^{1/1.86} = 820 \text{ gpm}$$

$$P_b = \underbrace{P_t}_{P_c} - \underbrace{0.0037 \times 820^{1.86}}_{P_c} = 1827 \text{ psi} \quad \text{that } P_c = KQ^{1.86} \rightarrow P_b = \frac{MW Q^2}{10858 A_n^2}$$

$$A_n = \left(\frac{820^2 \times 9.5}{1827 \times 10858} \right)^{1/2} = 0.5674 \text{ in}^2$$

Nozzle: 2×16 -15

$$V_f = 0.32086 \times 820 / 0.5674 = 460 \text{ fp/s}$$

$$I_f = 0.00516 \times 9.5 \times 820 \times 463 = 1864 \text{ lbs}$$

به دو عدد ۱۶" و ۱۵" نیاز داریم

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Example 2

Max. Impact

$$k = 0.0037$$

در این مورد ۴۹٪ P_t را در نظر می‌گیریم
در نتیجه باید ما $Nozzle$ با قطر گندم در نظر بگیریم
تا P_t کمتر و HHP بیشتر داشته باشیم.

$$Q_{opt} = \left[\frac{F \cdot P_t}{k(F + N)} \right]^{1/N} = \left[\frac{2 \times 2800}{3.86 \times 0.0037} \right]^{0.5376} = 1010 \text{ gpm}$$

$$P_b = 2800 - 0.0037 \times 1010^{1.86} = 1376 \text{ psi}$$

$$A_n = \left(\frac{1010^2 \times 9.5}{1376 \times 10858} \right)^{1/2} = 0.80 \text{ in}^2$$

Nozzle: 2×18 -20

$$V_f = 0.32086 \times 1010 / 0.8 = 401 \text{ fp/s}$$

$$I_f = 0.00516 \times 9.5 \times 1010 \times 401 = 1985 \text{ lbs}$$

نسبت به قبلی کم شده است.

80

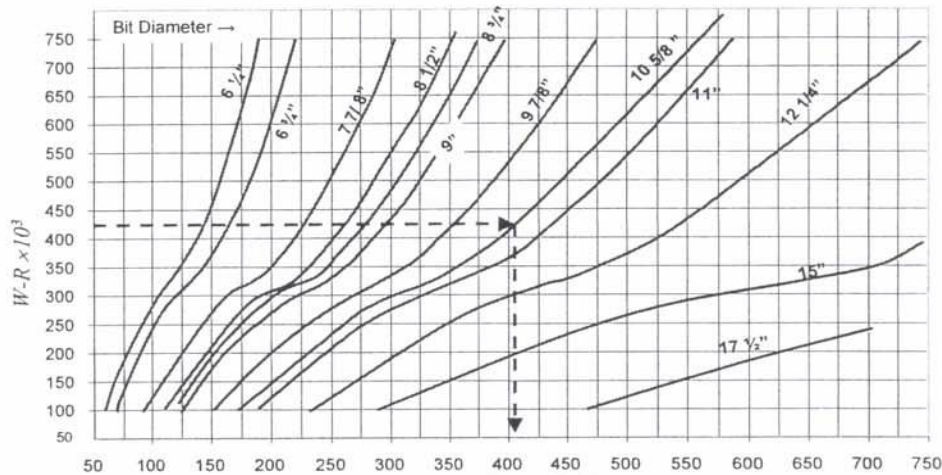
$$RPM = R$$

$$WOB = W$$

$$W \times R = f(\text{Min HHP})$$

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Minimum Bit Hydraulic Horsepower vs. W-R to Prevent Hydraulic Flounder



$$\text{Bit Hydraulic Horsepower} = \frac{GPM \times \Delta P \text{ at Bit}}{1714}$$

Example: Bit Size 10.625"

Bit Weight: 50,000# (4700#/inch)

Rotary Speed: 90 RPM

$$RPM \times WOB \leftarrow W-R = (4700)(90) = 423 \times 10^3$$

Required BHHP=410 hp

$$\rightarrow WOB = \frac{\text{Bit weight}}{\text{Bit size}} = \frac{1 \text{ lb}_f}{\text{in}}$$

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$$P_c = K Q^n$$

The actual value of n can be determined in the field by running the mud pump at several speeds and reading the resulting pressures. A graph of $P_c (=P_p - P_{bit})$ against Q is then drawn.

The slope of this graph is taken as the index n .

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Example: Bit size: $8\frac{1}{2}"$ T.D = 8000' ROP = $5\frac{m}{hr}$
 MW = 10 PPG PV = 12 $\gamma_p = 5$ Max pump press = 2600 psi
 GPM = 400 Nozzle = 3x12 RPM = 50 WOB = 42-44000 lbs

الف) با استفاده از Flunder chart، اگر با افزایش عمق، به دلیل محدودیت فشار دی پمپ ران به $gpm = 350$ کاهش می دهد، چه تغییری در سرعت حفاری به وجود خواهد آمد؟

ب) در عمق 12000' به دلیل افزایش عمق و محدودیت فشار، دی ران به $gpm = 310$ کاهش می دهد، چه تغییری در سرعت حفاری به وجود آمده و برای حل آن چه پیشنهادی دارید؟

Sol: $WR = \frac{RPM \times WOB}{Bit Size}$

$W = 42000$ $RPM = 50$ $\rightarrow WR = \frac{42000 \times 50}{8.5} = 247 \times 10^3$ From Flunder chart Min (HHP)_{bit} = 175 hp

$$\Delta P_{bit} = \frac{8.311 \times 10^{-5} MW q^2}{C_d^2 A_n^2} \text{ or } \Delta P_{bit} = \frac{MW \times q^2}{6698.3 n^2 d^2}$$

$$\Delta P_b = 1340 \text{ psi}$$

$$(HHP)_{bit} = \frac{PQ}{1714} = \frac{1340 \times 400}{1714} = 313 \text{ hp}$$

$$\begin{cases} GPM = 350 \\ \Delta P_b = 1040 \text{ psi} \\ (HHP)_{bit} = 212 \text{ hp} \end{cases}$$

$$\begin{cases} GPM = 310 \\ \Delta P_{bit} = 806 \text{ psi} \\ (HHP)_{bit} = 146 \text{ hp} \end{cases}$$

افزایش داد γ_p کم کنیم
 دو حالت را می توان انجام داد \leftarrow به ران عرض کرد یا gpm را تغییر داد یا WR را تغییر داد.
 مثلاً در این حالت به جای نازل 12 می توان نازل 14 یا کوچکتر انتخاب کرد.

اگر در این حالت به علت HHP کم نخواهیم Nozzle را عوض کنیم
 با توجه به حداقل توان مورد نیاز ΔP_{bit} را حساب می کنیم و با توجه به آن می توانیم Nozzle Area را حساب کنیم.

✓A

Surge and swab pressure

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When running tubulars in a hole filled with drilling mud so called "surge pressures" and "swab pressures" are created. The surge pressure is an increase of the pressure in front of the tubulars

when run into the well, the swab pressure is a pressure reduction behind the tubular when pulled out of the well.

Excessive surge or swab pressures have to be avoided since they can lead to problems like:

1. Pressure reduction due to swab can cause a kick,
2. Pressure increase due to surge pressure can fracture weaker formation and cause lost circulation which in turn can cause a kick,

WOB RPM ROP : Drill off test

۱- ابتدا در RPM ثابت، WOB را تغییر می‌دهیم و حداقل ROP را بدست می‌آوریم.

۲- در هر دو WOB و RPM ثابت، تغییر می‌دهیم و حداقل ROP را بدست می‌آوریم.

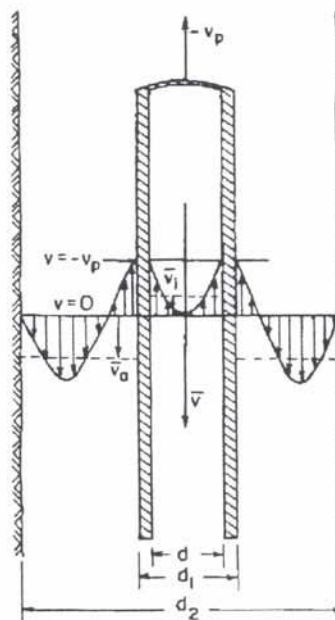
۳- با استفاده از هر دو حداقل ROP مناسب را بدست می‌آوریم

Depth	Bit size	Bit type	Nozzle size	MW	Pv	γp	GPM	Nozzle Velocity	Annular Velocity	pump pressure
100m	17 1/2"	111	3x16	آب	-	-	950			
1000m	"	121	3x16							
1500m	"	131	2x16-18							
2000m	"	131	3x18							

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Surge and swab pressure

$$\bar{v}_a = v_p \frac{3d^4 - 4d_1^2(d_2 - d_1)^2}{6d^4 - 4(d_2 - d_1)^2(d_2^2 - d_1^2)}$$



ex: Bit size: $10 \frac{5}{8}$ " WOB = 50000 RPM = 90 gpm = 420
 what is the min (HHP)_{Bit} = ? & calculate Nozzle Area?

sol: $WR = \frac{50000 \times 90}{10 \frac{5}{8}} = 423 \times 10^3 \rightarrow (HHP)_{bit} = 410$

$\frac{P_b Q}{1714} = 410 \rightarrow \frac{P_b \times 420}{1714} = 410 \rightarrow P_b = \checkmark \rightarrow A_n \rightarrow \checkmark$

$P_b = \frac{MW \times q^2 \times 8.311 \times 10^{-5}}{C_d^2 A_n^2}$

Bit size = $8 \frac{1}{2}$ " : data

Drill pipe = $4 \frac{1}{2}$ " , $16.6 \frac{\text{lb}}{\text{ft}}$

Drill collar = 600 , $6 \frac{1}{2}$ " , $2 \frac{1}{2}$ "
 OD ID

MW = 10.5 ppg

sol:

$\Delta P_b = 1000 \text{ psi} \rightarrow (HHP)_{method}$
 $(HHP)_{bit} = 175 \text{ hp}$
 $WR = 282 \times 10^3 \rightarrow \text{Flounder chart}$
 $(HHP)_{bit} = 200 \text{ hp}$

Interval 4000 - 5000' : Nozzle = $2 \times 11 + 12$

gpm = 300
 max

P.P = 1350 psi

WOB = 40100 #

RPM = 66

ROP = 10' / hr

$A_n = 2 \times 11 + 12$ بجای $A_n = 3 \times 11$

HW: Due: 20/9/87

Hole size = $17 \frac{1}{2}$ "

Depth = 2100 m

MW = 82 pcf

$P_r = 15$ $\gamma_p = 3$

BHA = Bit + Bit sub + 3 jts 11" (27 m, 3" ID)
 + 6 jts $9 \frac{3}{4}$ " (54 m, 3" ID)
 + DP : 5" x 4.276"

Mishan Formation:

Bit type: R₃ (Hughes)

surface connection: type 2

Max pump press = 3000 psi

max gpm = 800 gpm

Nozzle = 3 x 16

calculate:

- 1- The min gpm
- 2- The optimum gpm (HHP & Jet impact Force)
- 3- $\Delta P_{surface} + \Delta P_{pp} + \Delta P_{DC} + \Delta P_{bit} + \Delta P_{Ann}$
- 4- For max HHP & Jet impact Design new Nozzle Area P
- 5- if WOB = 5500 # , RPM = 79 & Flunder chart compare the actual (HHP)_{bit} in Stage 4 with min (HHP) required P



Petroleum University of Technology
Ahwaz Faculty of Petroleum Engineering

In the name of God

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Casing Design

A. Hashemi, PhD

Casing

Objectives:

- To prevent unstable formations from caving in
- To prevent contamination of near-surface fresh water zones.
- To protect weak formations from the high mud weights that may be required in subsequent hole sections. These high Mw may fracture the weaker zones;
- To isolate zones with abnormally high pore pressure from deeper zones which may be normally pressured;
- To seal off lost circulation zones;
- When set across the production interval: to allow selective access for production / injection/control the flow of fluids from, or into, the reservoir (s).
- To provide structural support for the wellhead and BOps.

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CP 30" @ 60

C 20" @ 779 m

C 13 3/8" @ 938.5 m

Tubing 7" @ 41/2

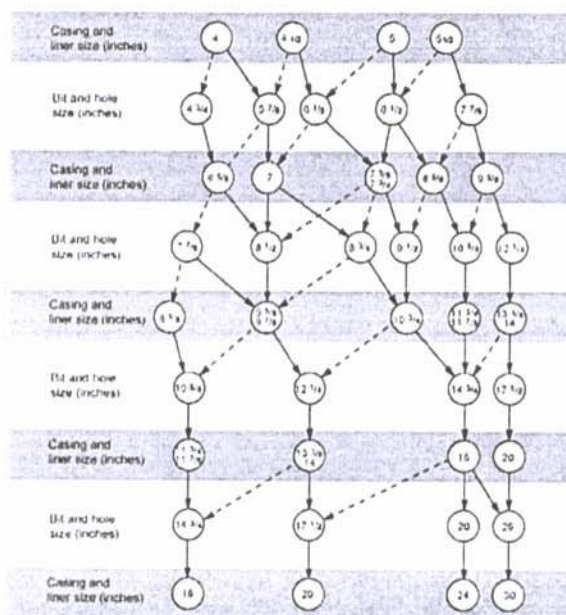
Packer 7" MIIR @ 2408 m

C 9-5/8" @ 2350 m

L 7" @ 2684-2217 m

3

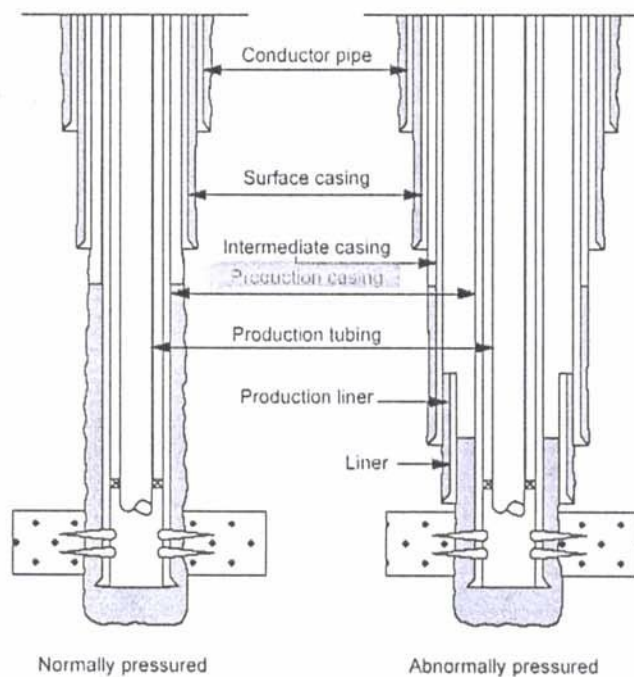
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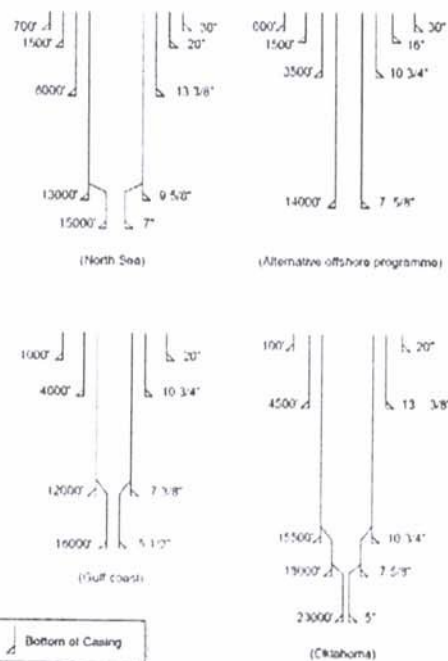
Casing string terminology

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5

Casing string configurations



6

API

The API Committee responsible for the standardisation of tubular goods is **Committee number 5**. This committee publishes, and continually updates, a series of Specifications, Standards, Bulletins and Recommended Practices covering the manufacture, performance and handling of tubular goods. The documents, published by Committee 5, of particular relevance to casing design and specification are :

API SPEC 5CT, "Specification for casing a tubing": Covers seamless and welded casing and tubing, couplings, pup joints and connectors in all grades. processes of manufacture, chemical and mechanical property requirements, methods of test and dimensions are included.

API STD 5B, "Specification for threading, gauging, and thread inspection for casing, tubing, and line pipe threads": Covers dimensional requirements on threads and thread gauges, stipulations on gauging practice, gauge specifications and certifications, as well as instruments and methods for the inspection of threads of round-thread casing and tubing, buttress thread casing, and extreme-line casing and drill pipe.

API RP 5A5, "Recommended practice for filed inspection of new casing, tubing and plain-end drill pipe": Provides a uniform method of inspecting tubular goods.

API RP 5B1, "Recommended practice for thread inspection on casing, tubing and line pipe": The purpose of this recommended practice is to provide guidance and instructions on the correct use of thread inspection techniques and equipment.

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API

API RP 5C1, "Recommended practice for care and use of casing and tubing": Covers use, transportation, storage, handling, and reconditioning of casing and tubing.

API RP5C5, "Recommended practice for evaluation procedures for casing and tubing connections": Describes tests to be performed to determine the galling tendency, sealing performance and structural integrity of tubular connections.

API BULL 5A2, "Bulletin on thread compounds": Provides material requirements and performance tests for two grades of thread compound for use on oil-field tubular goods.

API BULL 5C2, "Bulletin on performance properties of casing and tubing": Covers collapsing pressures, internal yield pressures and joint strengths of casing and tubing and minimum yield load for drill pipe.

API BULL 5C3, "Bulletin on formulas and calculations for casing, tubing, drillpipe and line pipe properties": Provides formulas used in the calculations of various pipe properties, also background information regarding their development and use.

API BULL 5C4, "Bulletin on round thread casing joint strength with combined internal pressure and bending.": Provides joint strength of round thread casing when subject to combined bending and internal pressure.

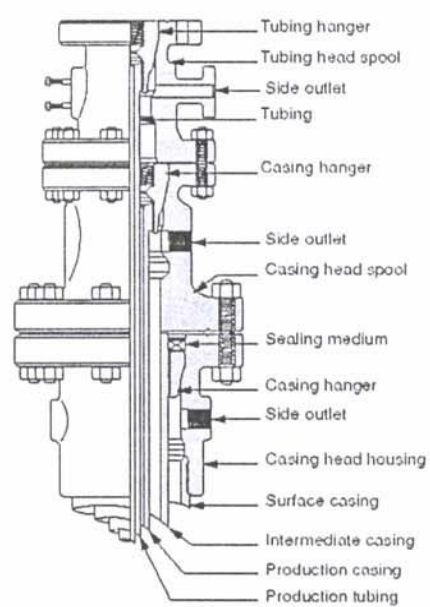
8

casing head spool : بعد از سطحی شدن از عدم فوران BOP رابری داریم و این ch.S رابری روی فلنج پایه قرار می دهیم. (از داخل shoe مانع بالا آمدن سیان و از بیرون slip مانع بیرون آمدن سیان می شود)

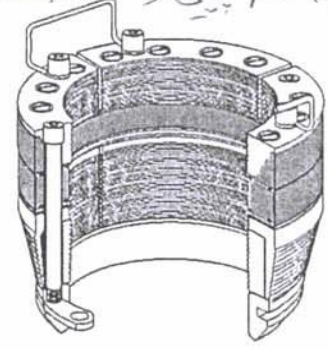
۸۳

- برای هر casing ابتدا یک slip می گذاریم تا کلی وزن را تحمل کند درون فلنج (سپی BOP رابری داریم و یک فلنج روی فلنج قبلی می گذاریم) © A.Hashemi, 2008

API wellhead



- casing اولی روی زمین و با استفاده از سیان محکم می شود.
- در لوله های حفاری همیشه pin پائینی و Box بالایی است.



Slip type casing hanger →

- ۱- جلوگیری از بالا آمدن سیان (sealing)
- ۲- نگه داشتن casing

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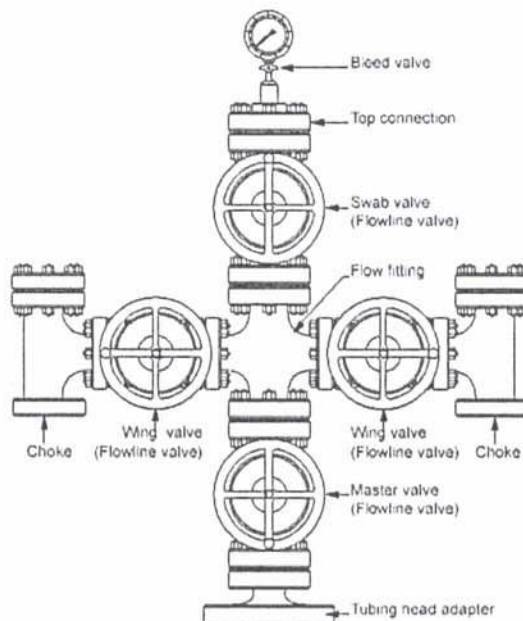
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Surface wellhead spools

- To suspend the weight of the casing string;
- To seal off the annulus between successive casing strings at the surface;
- To allow access to the annulus between casing strings;
- To act as an interface between the casing string and BOP stack.

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X-Mass tree



11

Types of casing

• Conductor pipe : لوله راهنما

is run from the surface to a shallow depth to protect near surface unconsolidated formations, seal off shallow-water zones, provide protection against shallow gas flows, provide a conduit for the drilling mud and to protect the foundation of the platform in offshore operations.

always cemented to surface. It is used to support subsequent casing strings and wellhead equipment or alternatively the pipe is cut off at the surface after setting the surface casing.

می شود /
 - مهمترین وظیفه conductor pipe این است که مانع شستن شدن لایه های نزدیک به زمین
 - مانع از آلوده شدن آب های زیرزمینی می شود.
 - گاهی اوقات به کمک نفوذ گاز به سطح زمین نیاز به BOP است که برای این کار حتماً باید از casing برانیم.
 - مسیری برای حرکت لایه حفاری است.

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Types of casing

Surface Casing

- to prevent caving of weak formations that are encountered at shallow depths
- should be set in competent rocks such as hard limestone.
- serves to provide protection against shallow blowouts,
- A typical size of this casing is 13 3/8 in. (240 mm) in the Middle East and 18 5/8 in. or 20 in. in North Sea

Types of casing

Intermediate casing

- is usually set in the transition zone below or above an over-pressured zone,
- to seal off a severe-loss zone or to protect against problem formations such as mobile salt zones or caving shales.

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- بعد از تمیز کردن بالا و درون liner نیاز به تست کردن آن می باشد. ضعیف ترین قسمت liner، overlap آن است.

برای آن باید در چاه را به بیم و به پامی کنیم و فشار را افزایش می دهیم. افت فشار نشانه دهنده وجود loss است.

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Types of casing

روش دوم استفاده از ابزار DST است.

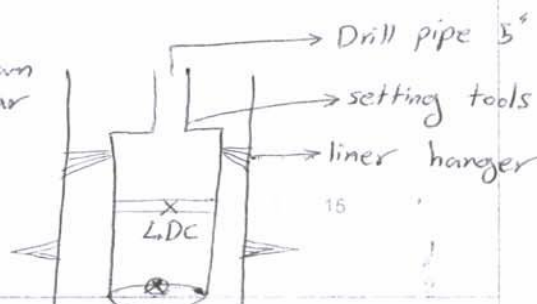
Production casing

- is the last casing string.
- To isolate producing zones,
- to provide reservoir fluid control
- to permit selective production in multizone production

← overlap ← گاز پر فشار ۱۲۰ m
نفت ۶۰ m

- حجم سیان لازم برای سیان کاری liner برابر است با حجم بین LDC و شیر یک طرفه و فضای overlap و فضای openhole. برای مطمئن شدن از سیان کاری مناسب، حجم بیشتری سیان به کار می بریم.

LDC: Latch down collar



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Types of casing

Liner

- is a string of casing that does not reach the surface.
- are hung on the *liner* by use of a liner-hanger
- In liner completions both the liner and the intermediate casing act as the production string.

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- tie-back: باید طوری راند شود که بالای آن در سطح و پائینی بروی لبه قبلی قرار گیرد که مشکل این روش این است که باید well head را عوض کنیم.

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Types of liner

- **tie-back:** after the liner has been run and cemented it may be necessary to run a casing string of the same diameter as the liner and connect onto the top of the liner hanger, effectively extending the liner back to surface.
- **drilling liner:** liners may also be used as an intermediate string to case off problem zones before reaching the production zone. In this case the liner would be known as a drilling liner.
- **stub liner:** Liners may also be used as a patch over existing casing for repairing damaged casing or for extra protection against corrosion. In this case the liner is known as a stub liner.

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tie-back است بالینی تفاوت که تا سطح نمی آید. Tie-back sleeve: سیم

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Aadvantages of a liner

- Total costs of the production string are reduced (running and cementing times)
- Complete wells with less weight landed on wellheads and surface pipe
وزن کمتر روی wellhead و surface pipe
- A scab liner tie-back provides heavy wall cemented section through salt sections.
- Permits drilling with tapered drillstring. → tubing ها با توجه به عمق تغییر می کند. انشان
- Where rig capacity cannot handle full string; when running heavy 9 5/8" casing.
- Improved completion flexibility.
- The liner can be rotated during cementing operations. This will significantly improve the mud displacement process and the quality of the cement job.

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Disadvantages of a liner

- Possible leak across a liner hanger
- Difficulty in obtaining a good primary cementation due to the narrow annulus between the liner and the hole

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Casing design

- Objectives: The primary purpose of designing casing strings is to control well conditions safely and economically.

کنترل به خوبی شرایط برای حیات اتمام دهد

از لحاظ اقتصادی

- The casing size to be run determines the maximum bit size for subsequent drilling, and the bit size limits the next size of casing

طوری casing باید طراحی شود که بتوان Max size متر را برای حفاری راند

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حجم وزن سنگی تر باشد ID کمتر است، چون گوشه ضخامت بیشتر است.
(OD همیشه ثابت است.)

$$489.5 \frac{lb}{ft} = E_{steel} \leftarrow \text{جمع وزن فولاد} \leftarrow \text{حفظ کنیم}$$

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Properties of casing

Casing Size (Outside Diameter **O.D.**)

4.5"-36" → OD بستری

Drift diameter
 $OD \leq 27 \frac{1}{8}" \Rightarrow DD = ID - 0.094$
 $31 \frac{1}{2}" \leq OD \leq 85 \frac{1}{8}" \Rightarrow DD = ID - 0.125$
 $95 \frac{1}{8}" \leq OD \leq 133 \frac{1}{8}" \Rightarrow DD = ID - 0.156$
 $16" \leq OD \Rightarrow DD = ID - 0.188$

Drift diameter: The drift diameter refers to the guaranteed minimum I.D. of the casing.

باید قبل از casing با این توبه max rubber بطور انفرادی گرفته شود.
که ممکن است در کارخانه قطر max
max می توان از درون casing عبور داد که معمولاً این عمل در سطح توبه از رانندگی casing انجام شده و Drift اندازه گیری می شود.

Length of Joint

The length of a joint of casing has been standardised and classified by the API as follows:

معمولاً در ایران لیست داده می شود

Range	Length (ft.)	Average Length (ft.)
1	16-25	22
2	25-34	31
3	34+	42

درست ریخت نشده باشد
ممکن است در حین جابجایی
ضربه دیده و قطران
تفکیک و این عمل را
Drift گویند

معمولاً در casing گذاشتن یک لوله ی سنگی بالا گذاشته (ID کمتر دارد) و سپس لوله های سبک و سبکی لوله های سنگی را قرار می دهند. این یک سازه لوله با هم می شود که اگر استیاسی در casing گذاری شده، می تواند از تمامی مشکلات جلوگیری کند.

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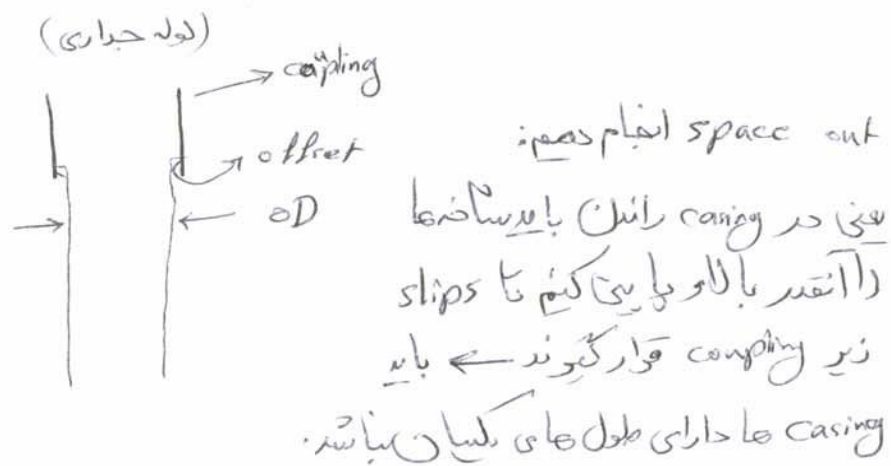
Properties of casing

Casing Weight is the weight per foot of the casing and is a representation of the wall thickness of the pipe. There are for instance four different weights of 9 5/8" casing:

OD: لیست است

Weight lb/ft	OD in.	ID in.	Wall Thickness in.	Drift Diameter in.
				$8 \frac{3}{4}$
53.5	9.625	8.535	0.545	8.379
47	9.625	8.681	0.472	8.525
43.5	9.625	8.755	0.435	8.599
40	9.625	8.835	0.395	8.679

سایز Max
منته که قرار است از آن
لوله جاری رد شود.
که معمولاً کمتر از ID
است تا مانده گیر نکند.



Casing Grade

The letter refers to the chemical composition of the material and the number refers to the minimum yield strength of the material e.g. N-80 casing has a minimum yield strength of 80000 psi and K-55 has a minimum yield strength of 55000 psi.

Hence the grade of the casing provides an indication of the strength of the casing. The higher the grade, the higher the strength of the casing.

N-80
L-80
C-75
P-110
V-150

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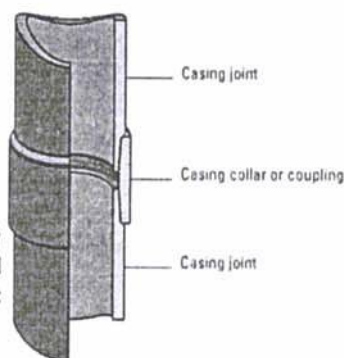
Properties of casing contd.

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Couplings are short pieces of casing used to connect the individual joints. They are normally made of the same grade of steel as the casing.

The API has specifications for four types of couplings.

- Short round threads and couplings (CSG)
- Long round threads and couplings (LCSG)
- Butress threads and couplings (BCSG)
- Extremeline threads (XCSG)



e, with
erence
or the

The CSG and LCSG have the same basic thread design. They have eight threads per inch. These threads are generally referred to as 8 x 11 threads. The difference between the two is that the LCSG has a longer thread run-in distance. LCSG are very common couplings.

← Buttruss (BCSG) threads are more square, with five threads per inch. They are also longer couplings, with corresponding longer thread run-out.

The XCSG (Extremeline) couplings are different from the other three connectors in that they are integral connectors, meaning the coupling has both box and pin ends.

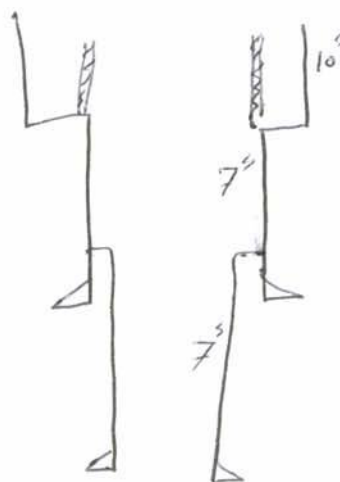
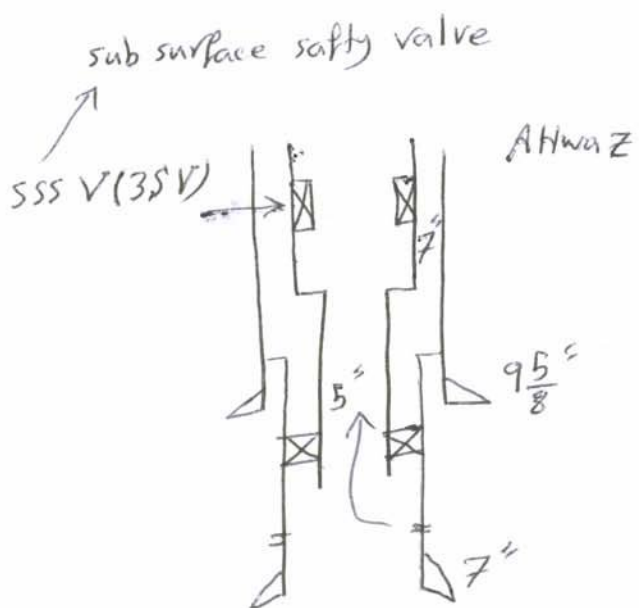
→ تَرَدَدَ treads
 واحد طَرْدٍ طَرْدًا
 ← يَتَرَدَّدُ

در معادری خاص از چید لود casing با grade های مختلف استفاده می شود:

(چید سبانه بالای ۱۰.۵ است) $10.5 \rightarrow 9.5$

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تنها موردی که از ترکیب چند لوله جاری با سایزها مختلف استفاده می کنند



Properties of casing contd.

- Coupling threads are cut on a taper, causing stress to build up as the threads are made up. A loose connection can result in a leaking joint. An over-tight connection will result in galling, which again, will cause leaking. Proper make-up is monitored using torque make-up tables and the number of required turns.
- A special thread compound (pipe dope) is used on casing couplings, each type of coupling having its own special compound.

باید این threads را طوری بزنند که جلوله یابی و بازا کاملاً به هم متصل شده که کار بتواند وارد شود

Properties of casing

- The body yield strength is the tensional force required to cause the pipe body to exceeds its elastic limit.
- The yield strength, is defined as by API as the tensile stress required to produce a total elongation per unit length of 0.005 on a standard test specimen.
- Min Yield Strength, σ_{yield} , # 80% of the average yield strength observed.
- Tensile strength: Is the greatest longitudinal stress that a metal can bear without tearing apart.

چنانچه تنش کششی کم تر از طول اعمال شده و ۰.۰۰۵ تغییر طول دهد
Max yield

بسیاری نیرو به سطح بالایی اعمال می شود

اگر به یک لوله نیروی اعمال شود و باعث می شود که لوله آبراز یک حالتی زیاده تر شود و در حالت پلاستیک می شود

Properties of casing

API Grade	Yield Strength (min), psi	Tensile Strength (min), psi
H-40	40,000	60,000
J-55	55,000	75,000
K-55	55,000	95,000
C-75	75,000	95,000
L-80	80,000	100,000
N-80	80,000	100,000
C-90	90,000	105,000
C-95	95,000	105,000
P-110	110,000	125,000

مقاومت بیشتری دارد ←

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API casing performance properties

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✓ **Axial Tension:** Axial tension loading results primarily from the weight of the casing string suspended below the joint of interest.

- **Body yield strength** is the tensional force required to cause the pipe body to exceed its elastic limit.

- **Joint strength** is the min. tensional force required to cause the joint failure.

✓ **Burst Pressure rating:** is the calculated min. internal pressure that will cause the casing to rupture in the absence of external pressure and axial loading.

✓ **Collapse Pressure rating:** is the min. external pressure that will cause the casing walls to collapse in the absence of internal pressure and axial loading.

(در مقابل حلال شدن)

Tension

load که اضافه وارد می کنیم به براساس وزن string تا لوله های کبر کرده آزاد شود

➤ Tension design is based on the load imposed from the weight of pipe hanging from below with each section of the string having to support the entire weight of the casing below.

→ landing joint (لنگر)

➤ Tension loads are maximum at the surface and zero at some point within the string.

➤ Usually casing strings are run in fluid and a neutral point exists in the string due to buoyancy.

حنی

توقه ای که نه نیروی کششی و نه نیروی فشاری دارند

➤ Every string run in fluid has a neutral point above which the pipe is in tension and below the pipe is in compression.

ترکشی بیشتر می شود

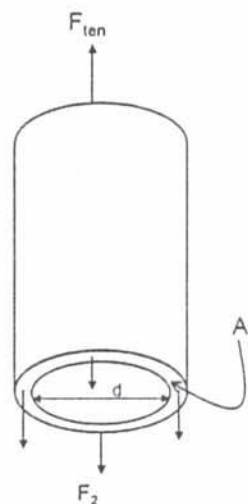
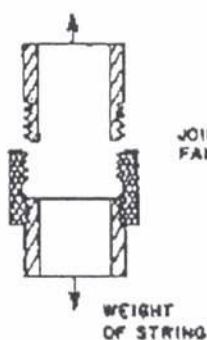
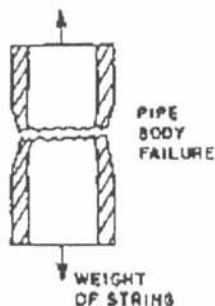
وقتی نیروی tension بیشتر شود ← مقاومت بیشتری کمتر و مقاومت

Tension

The force F_{ten} tending to pull apart the pipe is resisted by the strength of pipe wall, which exert a counterforce, F_2 :

$$F_2 = \sigma_{yield} A_s$$

The pipe body strength computed by this equation is the minimum force that would be expected to cause permanent deformation of pipe.



Example

yield strength min $\leftarrow 55000$

Compute the body-yield strength for 20-in., K-55 casing with a nominal wall thickness of 0.635 in. and a nominal weight per foot of 133 lbf/ft.

فقط وزن body

Solution:

This pipe has a minimum yield strength of 55,000 psi and an ID of:

$$d = 20.00 - 2(0.635) = 18.730 \text{ in.}$$

Thus, the cross-sectional area of steel is

فقط در تبدیل واحد ها
دقت شود

$$A_s = \frac{\pi}{4} (20^2 - 18.73^2) = 38.63 \text{ sq.in.}$$

$$F_{ten} = \sigma_{yield} * A_s$$

$$F_{ten} = 55,000 (38.63) = 2,125,000 \text{ lb}_f$$

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می توان بهلول نیروی وارد کرد
رناسی از وزن لوله ها و یا وزن لوله ها
+ اضافه کششی فاسی از لوله ها

Burst

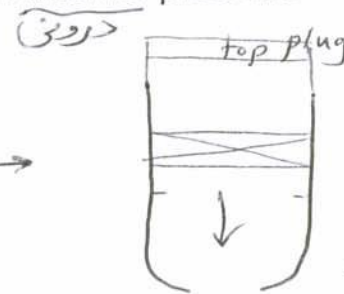
مثلاً می توان مقدار حداکثر کششی برای آزاد کردن
لوله های گیر کرده حساب کرد با در نظر گرفتن
safety factor

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Burst loads in casing design result from the internal pressure encountered.

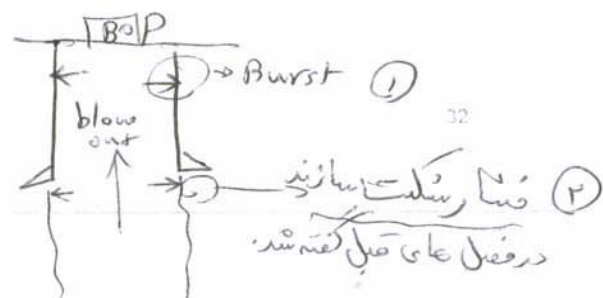
Burst loads result from:

- pressures during cementing
- acidizing,
- hydraulic fracturing,
- tubing leaks,
- closing in drilling wells after kicks



در حین سیان کاری
ممکن است مسیر
خروج سیان
به داخل بسته شود
و این باعث Burst می شود

وقتی در حین حفاری Kick برخورد کنیم
چاه را می بندیم و فشار درون چاه
افزایش می یابد و ما ممکن است
Burst رخ دهیم



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Burst

Barlow's law

$$P = 1.75 \frac{y_m}{D/t}$$

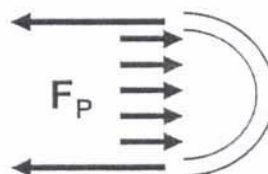
P = internal yield pressure, psi

y_m = minimum yield strength, psi

t = nominal wall thickness, in

D = O.D. of pipe, in

d = ID of pipe, in



$$t = \frac{D - d}{2}$$

Therefore

BP: is proportional to pipe grade

is proportional to pipe thickness

is proportional to $1/t$

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اگر ID را نداشته باشیم، می توان آن را با استفاده از OD و grade بدست می آوریم.

Example

For 8 5/8", 24 #, k55, ID 8.097" compute the burst resistance.

$$P_b = 1.75 \times \frac{55000}{85/8 \left(\frac{85/8 - 8.097}{2} \right)} = 2946 \text{ psi}$$

این مقاومت در صافی باشد در جابجایی

به جای استفاده از این روابط می توان از جدول موجود استفاده کرد. (312 - 323 pages)

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Collapse

- Collapse is the first condition considered in casing design.
- The maximum collapse load occurs at the bottom of the string.

This dictates that casing is designed from the bottom to the top.

- Collapse loads are applied to the casing string from the drilling fluid or formation fluid on the outside of the casing.
- The maximum collapse load occurs when the inside of the pipe is empty and the drilling fluid exerts a hydrostatic pressure on the outside.

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* وقتی یک لوله در برابر تنش کششی قرار دهیم مقاومت collapse آن کم می شود و مقاومت Burst آن زیاد می شود.

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Collapse : $P_{ext} - P_{int}$ مقاومت لوله در مقابل معیاله شدن ناشی

- Parameters affecting CR
 - y_m
 - D/t
 - S_a : axial stress
- The combination of stresses due to the weight of the casing and external pressures are referred to as 'biaxial stresses'. Biaxial stresses reduce the collapse resistance of the casing and must be accounted for in designing for deep wells or combination strings.

Biaxial stress: وقتی یک لوله در چاه قرار می گیرد یک تنش ناشی از فشارهای بیرونی به آن وارد می شود و یک تنش عم به خاطر وزن آن به لوله وارد می شود.

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برای محاسبه collapse resistance باید D و t و y_m را داشته باشیم

Calculation of collapse resistance of pipes

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1000 psi

Y_m (ksi)	α	β	γ	A	B	C	F	G
40	16.40	27.01	42.84	2.950	0.0465	754	2.063	0.0325
50	15.24	25.83	38.83	2.979	0.0515	1056	2.003	0.0347
55	14.81	25.01	37.21	2.991	0.0541	1206	1.989	0.0360
60	14.44	24.42	35.73	3.005	0.0566	1356	1.983	0.0373
70	13.65	23.38	33.17	3.037	0.0617	1656	1.984	0.0403
75	13.60	22.91	32.05	3.054	0.0642	1806	1.990	0.4180
80	13.38	22.47	31.02	3.071	0.0667	1955	1.996	0.4340
90	13.01	21.69	29.18	3.105	0.0716	2254	2.017	0.4660
95	12.85	21.33	28.36	3.124	0.0743	2404	2.029	0.4820
100	12.70	21.00	27.60	3.143	0.0768	2553	2.040	0.4990
105	12.57	20.70	26.89	3.162	0.0797	2702	2.053	0.0515
110	12.44	20.41	26.22	3.181	0.0819	2852	2.066	0.0532
120	12.21	19.88	25.01	3.219	0.0870	3151	2.092	0.0565
125	12.11	19.63	24.46	3.239	0.0895	3301	2.106	0.5820
130	12.02	19.40	23.94	3.258	0.0920	3451	2.119	0.0599
135	11.92	19.18	23.44	3.278	0.0946	3601	2.133	0.0615
140	11.84	18.97	22.96	3.297	0.0971	3751	2.146	0.0632
150	11.67	18.57	22.11	3.339	0.1021	4053	2.174	0.0666
155	11.59	18.37	21.70	3.358	0.1047	4204	2.188	0.0693
160	11.52	18.19	21.32	3.375	0.1072	4356	2.202	0.0700
170	11.37	17.82	20.60	3.412	0.1123	4660	2.231	0.0734
180	11.23	17.47	19.93	3.449	0.1173	4966	2.261	0.0769

برای شرایط آزمایشگاه که لوله فقط تحت تنش فشاری قرار می گیرد و تنش کششی وجود ندارد.
فشار داخلی در این حالت صفر است.

$$\begin{aligned} \text{If } D/t \leq \alpha &\rightarrow CR = 2Y_m \times \frac{(D/t) - 1}{(D/t)^2} \\ \text{If } \alpha < D/t \leq \beta &\rightarrow CR = Y_m \left[\frac{A}{(D/t)} - B \right] - C \\ \text{If } \beta < D/t \leq \gamma &\rightarrow CR = Y_m \left[\frac{F}{(D/t)} - G \right] \\ \text{If } \gamma < D/t &\rightarrow CR = \frac{46.95 \times 10^6}{(D/t)(D/t - 1)^2} \end{aligned}$$

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Example 1: Calculation of collapse resistance of pipes

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Csg 13 3/8" N-80, 72#, ID= 12.347"

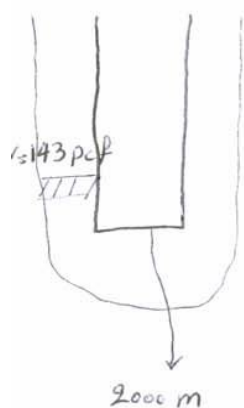
$$D/t = \frac{D}{(D-d)/2} = \frac{13.375}{(13.375 - 12.347)/2} = 26.0214$$

$$\beta < D/t \leq \gamma \rightarrow CR = Y_m \left[\frac{F}{(D/t)} - G \right]$$

$$CR = 80000 \left[\frac{1.998}{26.0214} - 0.0434 \right] = 2670 \text{ psi}$$

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bridge، یعنی جایی از دیواره ریزشی کرده و چاه plug شده و گودشگی قطع می شود. در این حالت به علت پمپ کردن گل فضا را افزایش می یابد و گل بر اثر شکست شدن سازند صوری رود و باعث به وجود آمدن حالت ① می شود.



① دالیز پر است - داخل لوله عا خالی است.

می خواهیم ببینیم ته چاه CL چه مقدار است!

چون داخل لوله عا خالی پس $P_i = 0$ است و P_e ناشی از وزن گل است.

$$CL = P_e - P_i^{\text{ته چاه}} = \frac{MW}{144} \times 3.281 \times h = 6000 \text{ psi}$$

$$CL = 0 \text{ در سطح}$$

② دالیز خالی و داخل لوله هم خالی است: (total lost circulation) $CL = 0$ ته چاه

- در بعضی موارد ممکن است اتفاق بیافتد ولی در حالت کلی level off می شود.

③ داخل لوله عا پر - دالیز خالی

- یک جسم خارجی مثل دستکش یا لوله بیافتد و این حالت باعث خالی ماندن دالیز می شود.

$CL = \text{collapse load} = P_e - P_i$

$BL = \text{Burst load} = P_i - P_e$

$\begin{cases} CR \geq CL \rightarrow \text{مسئله پیش نمی آید} \\ CR < CL \rightarrow \text{لوله میچاله می شود} \end{cases}$

$\begin{cases} BR \geq BL \rightarrow \text{مسئله پیش نمی آید} \\ BR < BL \rightarrow \text{لوله می ترکد} \end{cases}$

Example 2: Calculation of collapse resistance of pipes

Dp 5" D-55, ID= 4.276"

$$D/t = \frac{D}{(D-d)/2} = \frac{5}{(5-4.276)/2} = 13.81$$

$$D/t \leq \alpha \quad \longrightarrow \quad CR = 2Y_m \times \frac{(D/t) - 1}{(D/t)^2}$$

$$13.81 \leq \alpha \quad CR = 2 \times 55000 \frac{13.81 - 1}{(13.81)^2} = 7390 \text{ psi}$$

$$\begin{cases} P_e = \frac{MW \cdot h}{144} \times 3.281 \\ P_i = \end{cases}$$

* اگر مقدار گلی که در درون لوله وجود دارد برای با مقدار گلی پستالوله

باشد مقدار BL صفر است.

اگر درون لوله plug شود و یک فشار 2000 psi به درون لوله وارد کنیم: $P_i = \frac{MW \cdot h}{144} \times 3.281 + 2000$

$$P_e = \frac{MW \cdot h}{144} \times 3.281$$

Example 3: Calculation of collapse resistance of pipes

7" P110, ID= 6.174"

$$D/t = \frac{D}{(D-d)/2} = \frac{7}{(7-6.174)/2} = 17.1569$$

$$\alpha < D/t \leq \beta \quad CR = Y_m \left[\frac{A}{(D/t)} - B \right] - C$$

$$CR = 110000 \left[\frac{3.181}{17.1569} - 0.0819 \right] - 2852 = 8530 \text{ psi}$$

Differential Fill-up : به گونه ای طراحی می شود که مقدار ۶ درصد لوله های حفاری پر شوند
shoe-collar

مقاومت بدون اعمال axial tension } Tabulated collapse resistance (TCR)
 (label) ~ (از جدول) } = Burst = :
 = Tension = :

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مقاومت تصحیح شده و تension پول دارد شود: corrected collapse resistance (CCR)

CCR همان تراز TCR است. (در حالتیکه لوله تحت Tension قرار می گیرد).
 Axial tension stress

$$T_a = \frac{T_b}{A} - W_o D_x K$$

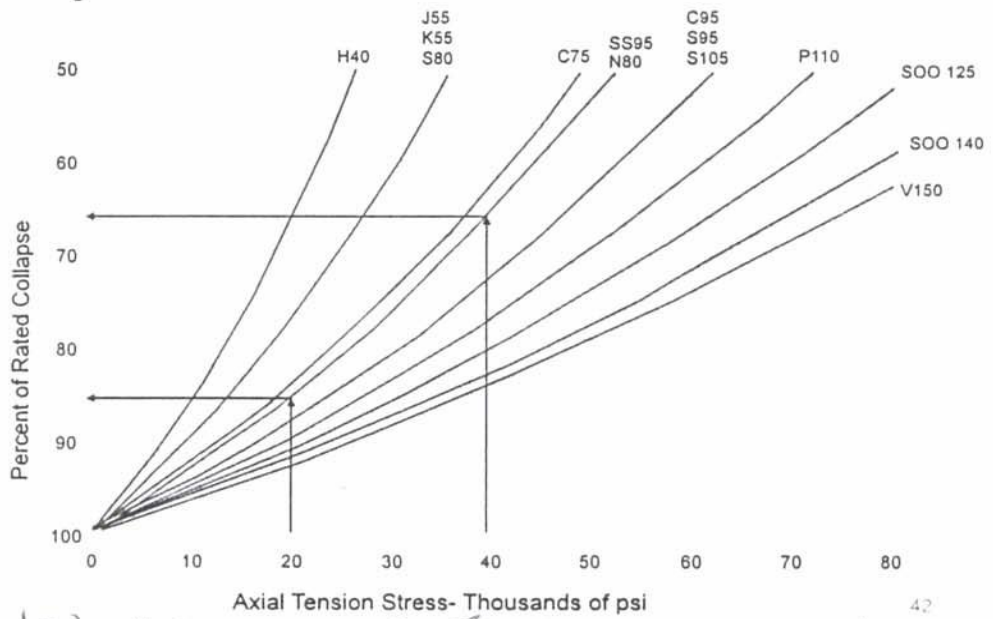
T_a = Axial tension stress at any depth with inside of casing empty, lb → بدترین حالت لوله وقتی خالی است
 T_b = buoyed tension load, lb → Tension در حالتیکه لوله در سیال شناور است.
 A = Pipe body cross sectional area
 D_x = variable depth, ft → به دلایل امتحانهای لوله در اعراض نقاط تقوین لوله
 D = pipe outside diameter, in
 d = pipe inside diameter, in
 W_o = mud density outside pipe, ppg
 K = Dimensionless factor for determining axial tension stress

$$K = 0.052 \left[1 + \frac{0.3}{\left(\frac{D}{d}\right)^2 - 1} \right]$$

چاه مقاومترین لوله را از نظر مقاومت collapse و در سطح لوله با کمترین مقاومت collapse به کار

change over point grade: نقطه ای که در آن grade لوله عوض می شود یا در grade ثابت وزن لوله عوض شود (هر چه وزن بیشتر باشد، مقاومتشان بیشتر است - در grade ثابت).

Effect of tensile loading on casing collapse



- با توجه جدول سرچ axial tension کمتر شود collapse resistance بیشتر است.
 - وقتی لوله تحت tension قرار می گیرد، مقاومت collapse کمتر است.

میکد لوله با مقاومت 2670 psi (مقاومت collapse) با گلی $MW=120 pcf$ راجع به عمق می توان استفاده کرد
 بندری شرایین
 $C_L = P_e - P_i = P_e \rightarrow 2670 = \frac{120}{144} \times 3.281 \times D \rightarrow D_x = 976 \text{ m}$
 اگر لوله تحت هیچ tension نباشد $TCR=2670$

collapse Factor
 $CSF = \frac{TCR}{C_L} = \frac{2670}{2670} = 1$

Example

چون $CSF = \frac{TCR}{C_L} < 1 \Rightarrow$ احتمال collapse شدن وجود دارد. اگر لوله 2500 psi داشته باشد چنانچه اتفاقی افتد

Compute the CCR (corrected collapse resistance) for a 13-3/8" N-80, 72# Csg $TCR=2670 \text{ psi}$, when the following tensile stresses are applied: 20,000 psi, 40000 psi
 با توجه به این فشار و grade از جدول صفحه قبل ضریب را می خوانیم

From fig. 85% $\rightarrow CCR=0.85 \times TCR=0.85 \times 2670=2270 \text{ psi}$ for 20000 lbs $\rightarrow D=830 \rightarrow$ برای مثال بالا وقتی لوله تحت tension قرار می گیرد.

From fig. 65% $\rightarrow CCR=0.65 \times TCR=0.65 \times 2670=1740 \text{ psi}$ for 40000 lbs

casing 13 $\frac{3}{8} \Rightarrow$ $\begin{cases} P110, 72\#, BTS: TCR=2890 \text{ psi} \\ N80, 72\#, BTS: TCR=2670 \text{ psi} \end{cases}$ جدول 43

$C_L = 2500 \times 3.281 \times \frac{80}{144} = 4557 \Rightarrow CSF = \frac{2670}{4557} = 0.6$

چون لوله ای از این به قیاس تر نداریم، جبریم از همین لوله استفاده کنیم. باید مایک عمق از مشخص از عمق لوله و برای اطمینان از اینکه لوله ضعیف تر استفاده می کنیم تا از لحاظ اقتصادی به صرفه تر باشد.

Example

MW=80 pcf/10.7 ppg
 Calculate the CCR and change over point for 13 3/8" csg N80, 72#, BTS.
 A) Ignore the axial tension effects
 B) Account for axial tension effects
 For both cases assume CSF=1
 Buoyancy factor = $1 - MW(ppg)/489.5 = 0.84$

Solution:

A) $CCR=TCR=2670 \text{ psi}$

$D(m) = \frac{CR \times 144}{MW(pcf) \times 3.281 \times CSF} \quad D = (2670 \times 144) / (80 \times 3.281) = 1465 \text{ m}$

B) T_a = Axial tension stress at any depth with inside of casing empty, lb
 T_b = buoyed tension load, lb = $(2500 - 1465) \times 72 \times 3.281 \times 0.84 = 205380 \text{ lbs}$
 A = Pipe body cross sectional area = 24.386 sqin
 D_x = variable depth = $(1465 \text{ m} \times 3.281) = 4808 \text{ ft}$
 D = pipe outside diameter, in (13.375 in)
 d = pipe inside diameter, in (12.6)
 W_o = mud density outside pipe, ppg = 10.7
 K = Dimensionless factor for determining axial tension stress = 0.177

$T_x = \frac{T_b}{A} - W_o D_x K = \frac{205380}{24.386} - (10.7)(4808)(0.177) = 4137 \text{ psi}$

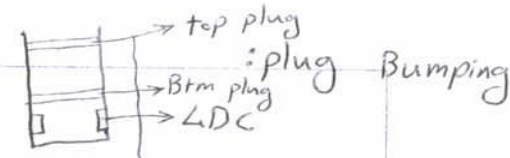
From fig. 97% $\rightarrow CCR=0.97 \times TCR=0.97 \times 2670=2590 \text{ psi}$ for $d=1420 \text{ m}$



از این نقطه D_x حساب می کنیم اگر منفی یا صفر شود لوله تحت compression است یا اصلاً نقطه Neutral است و نیازی به تضعیف نداریم.

Dog-leg severity (سد دگ): $\frac{10^\circ}{100}$ ← تغییر در زاویه در واحد ft ← هر چه بیشتر باشد، نیروی خمشی وارده بر طول بیشتر است.

یکی از خطرات از پایان سیمان کاری، باید فشار را بزرگتر از top plug افزایش داد. افزایش فشار در سطح نشان دهنده رسیدن top plug به Btm plug است.



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Casing design considerations

- 1) Collapse Loading scenario (always worst cases): the casing is fully evacuated due to lost circulation, the pore pressure is acting on the outside
- Maximum collapse load occurs at the bottom of the string

Collapse load: $P_c = P_o - P_i$

- 2) Burst Loading scenario: the maximum burst load is experienced if the well is closed in after a gas kick has been experienced. The pressure inside casing is due to formation pore pressure at the bottom of the well and a column of gas which extends from the bottom of the well to surface.

Burst load: $P_b = P_i - P_o$

External loads:

- 1) The pore pressure
- 2) Maximum Mw
- 3) The pressure due to column of cement slurry

Internal loads:

- 1) Pressure due to influx
- 2) Full evacuation
- 3) Production tubing leak
- 4) Fracture pressure of open formations

- 3) Axial Loading: Dry Weight of casing, Buoyed weight, DLS, Plug Bumping, Temperature changes, Overpull etc.

- 4) Compression: this type of loading could occur when an inner string transfers its weight to an outer string in which it is landed off or cemented

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Sources of data for casing design

Data	Source
1. Formation pressure, psi	Offset wells well logs, log analyst
2. Casing setting depths, ft	Offset wells, kick tolerance calculations
3. Fracture gradient (psi ft) or fracture pressure (ppg or psi) at casing seat	Offset wells, well logs, calculation of fracture gradient
4. Mud density, ppg	As above
5. Mean sea water level, ft	
6. Available casing grades and weights	Stock status report
7. Strength properties (burst, collapse, yield)	API or manufacturer's catalogues
8. Geothermal temperatures	Offset wells

توسعه زمین سایشی می شود ←

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Collapse design

- Maximum collapse load occurs at the bottom of the string.
- This dictate that casing is designed from the bottom to the top.
- Collapse loads are applied to the casing string from the drilling fluid or formation fluid on the outside of the casing
- The collapse design factor is the ratio of the rated collapse pressure divided by the external hydrostatic pressure at the setting depth.

$$\text{Min } c d = 1$$

$$\text{Collapse surface Factor} = C S F = \frac{C R}{C L}$$

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hydrostatic head - فشار در تپه = فشار در تپه = well head P_i در سطح که جریان پیدا کرده است.

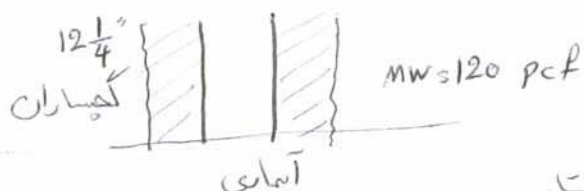
Burst design

- بدترین شرایط صاف است که لوله طاقالی باشد و گاز خود را به سطح برساند.
- بدترین شرایط در سطح (چون P_e در سطح صفر است) است.

- Burst load in casing design result from the internal pressure encountered.
- The most sever condition in burst occurs during a blowout when the casing string is completely empty and the well is closed in with only dry gas in the hole.
- The maximum burst design load at the top of the string is determined by the pressure at setting depth less the pressure of a column of gas to the surface.

$$\text{min Burst safety Factor} = 1.125 = \frac{B R}{B L}$$

در تپه چاه موهلاً منفی است. چون موهلاً چاه یا سیان شده است یا به اندازه ی وزن کل چاه آن برابر



فشار داخل لوله کمتر از فشار بیرون لوله است.
چون فشار آسانی کمتر از فشار کپساران است.

- بدترین شرایط مربوط به سرچاه است چون لوله بالایی تحت وزن لوله های

پایینی قرار میگیرند
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Tension design

- Tension design is based on the load imposed from the weight of pipe hanging from below with each section of the string having to support the entire weight of the casing below.
- Tension loads are maximum at the surface and zero at bottom.

$$\text{Tension surface factor} = T S F = \frac{T R}{T L}$$

$$\text{Min } T S F \geq 1.8$$

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Special casing designs

- Hydrogen sulfide
- Earth tectonics
- Massive salt sections
- Abnormal pressures
- Lost circulation
- corrosion

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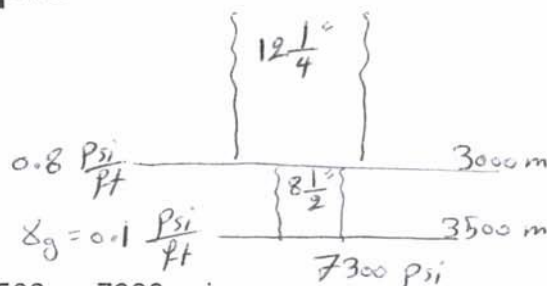
- مشکل این طراحی این است که ۶ نوع مختلف لوله را نیاز داریم. در واقع نباید لوله های کمتر از ۳۰۰۰ m را سرچاه بفروشیم.

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Casing design example

- 12 1/4" Hole
- MW=135 pcf
- 9 5/8" @3000 m
- Next Section 3000-3500 mdd
- 8 1/2" Hole
- Maximum bottom hole pressure @ 3500 m: 7300 psi
- Formation fracture gradient= 0.8 psi/ft
- Gas gradient: 0.1 psi/ft
- Design factor
 - Collapse: 1 $\rightarrow CL = CR$
 - Burst: 1.1
 - Tension 1.8

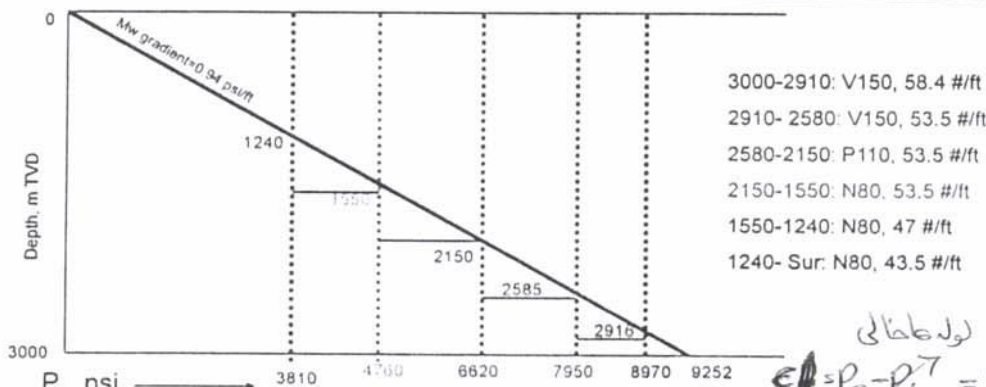


اگر گفته باشند $SCR = 2$ یا مقاومت لوله ها را نصف می کنیم یا سیاحت را عوض می کنیم (وزن لوله ها را دو برابر کنیم).
 مثلاً اگر عمق ۱۲۴۰ برای casing اول بدست آمده برای این حالت آن را نصف می کنیم یعنی ۶۲۰.
 پس ۱۲۴۰ بر آخرین نوع casing $CL = CR$.

Collapse design

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In Stock Csg	Collapse (psi)	Burst (psi)	Tension (1000lb)
9 5/8", V150, 58.4#/ft, BTS (id=7)	11570	16230	2532
9 5/8", V150, 53.5#/ft, BTS (id=8.536 in)	8970	14860	2323
9 5/8", P110, 53.5#/ft, BTS (id=8.536 in)	7950	10900	1710
9 5/8", N80, 53.5#/ft, BTS (id=8.536 in)	6620	7930	1244
9 5/8", N80, 47#/ft, BTS (id=8.681 in)	4760	6870	1086
9 5/8", N80, 43.5#/ft, BTS (id=8.755 in)	3810	6240	1005



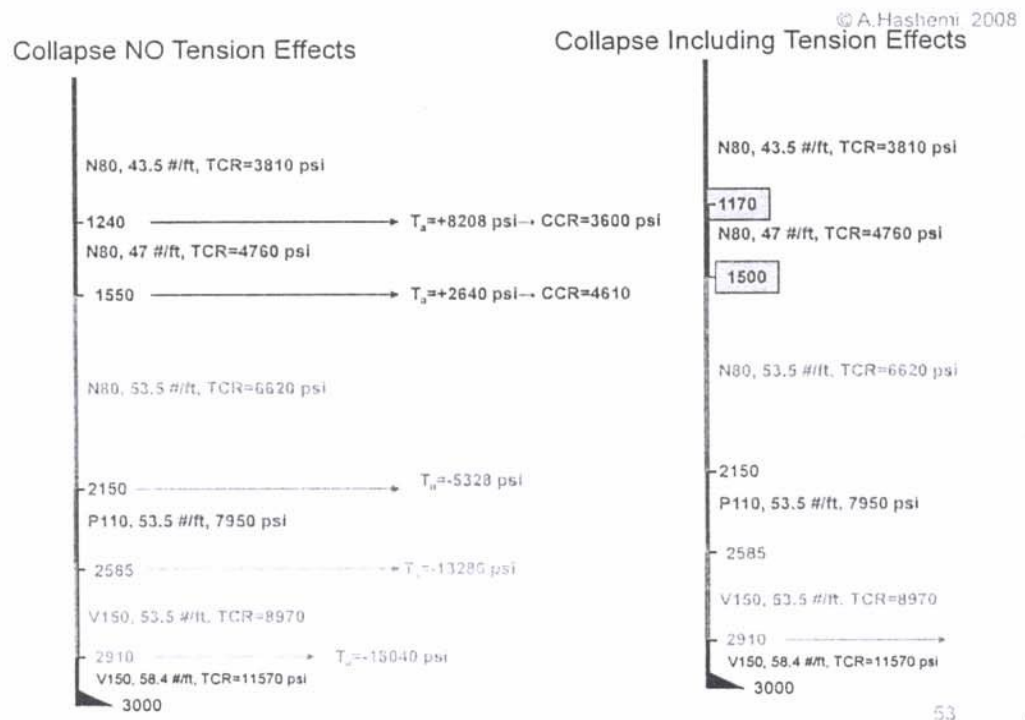
۱۲۴۰ جواب می دهد

مقاومت لوله چون ثابت است به صورت یک خط راست در می آید.

$$CL = \frac{P_e - P_i}{P_t} = P_e \rightarrow \text{مثلاً}$$

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تension بدترین حالت را در نقاط تقوین در نظر می گیریم. - برای وارد کردن اب



BL: یعنی اگر چاه جریان پیدا کند در چاه را ببندیم، اختلاف فشار P_i و P_o چه مقداری شود.

Burst design

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Burst load @ surface:

$$P_i = 7300 - 3500 \times 3.281 \times 0.1 = 6151 \text{ psi}$$

$$\text{Fracture formation pressure below } 9 \frac{5}{8} \text{ shoe: } 3000 \times 0.8 = 7874 \text{ psi}$$

$$\text{Bottomhole pressure in case of gas kick} = 6151 + (3000 \times 3.281 \times 0.1) = 7135 \text{ psi} < 7874$$

$$P_o @ 9 \frac{5}{8} \text{ shoe} = (135/144 \times 3.281 \times 3000) = 9228 \text{ psi}$$

$$P_i @ 9 \frac{5}{8} \text{ shoe} = 7135 \text{ psi}$$

$$BL = 7135 - 9228 = -2100 \text{ psi}$$

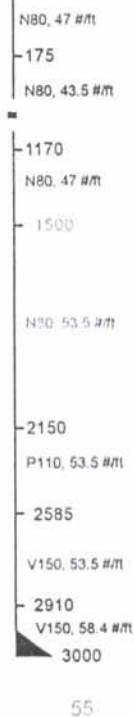
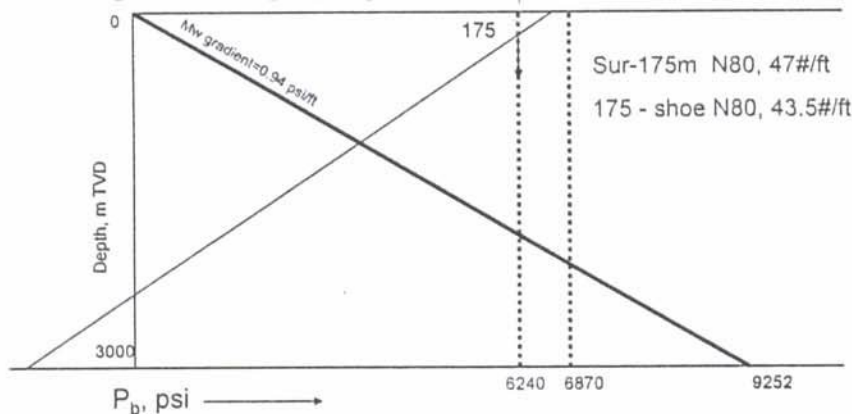
یعنی سازند نمی شکند و محاسبات را براساس 7135 psi انجام می دهیم ولی اگر سازند می شکست محاسبات را براساس Fracture gradient انجام می دهیم.

Burst design

Collapse + Burst 2008

Burst design: $8151 \times 1.1 = 6766$ psi

در عمق 6240 یعنی لوله با مقاومت Burst 175 جواب نمی دهد باید لوله با مقاومت تر انتخاب کنیم.



هرجا safety factor کمتر از مقدار مورد نیاز شد باید لوله قوی تر بخاریم.

Tension design

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Wa=482760 lbs;	TSF=2.25	N80, 47 #/ft
Wa=455774 lbs;	TSF=2.2	175
		N80, 43.5 #/ft
Wa=303774 lbs;	TSF=3.3	1170
		N80, 47 #/ft
Wa=255970 lbs;	TSF=4.24	1500
		N80, 53.5 #/ft
Wa=150850 lbs;	TSF=8.25	2150
		P110, 53.5 #/ft
Wa=74293 lbs;	TSF=23	2585
		V150, 53.5 #/ft
Wa=17245 lbs;	TSF=134	2910
		V150, 58.4 #/ft
		3000

↑ شروع می کنیم